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A Kinetic Modelling Study for Estimating Residual NH₃ Speciation at the Combustion Outlet in 70/30 vol% NH₃/H₂ Flames

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Topic: Reaction Modelling

Introduction

The development of new combustion systems for energy conversion is crucial due to recent constraints [1]. Global warming has highlighted the need for decarbonized fuels with zero carbon emissions. Hydrogen (H₂) and ammonia (NH₃) have emerged as promising alternatives, but their combustion characteristics, such as laminar flame speed, ignition delay times, and pollutant formation (e.g. NOx) must be understood. Kinetic reaction mechanisms are essential to comprehensively study the combustion chemistry of these fuels, including the breakdown of fuel molecules, formation of intermediate species, and production of combustion products like nitrogen and water when NH₃ is used as fuel.

Accurate speciation measurements of NH₃ and H₂ in the combustion system are of great importance as they directly impact combustion performance by providing crucial radicals that either accelerate or decelerate the combustion process. Ensuring a low level of residual NH₃ at the combustion exit is a crucial requirement to consider in the development of new combustion systems. A study conducted by Hayakawa et al. [2] determined that the optimal equivalence ratio for achieving a simultaneous reduction in unburned ammonia and NOx at the combustor exit is 1.2. Furthermore, when dealing with the fuel blend 70/30 vol% NH₃/H₂ in air, the ratio of final to initial mole fractions of NH₃ is high, but this ratio decreases with increasing H₂ concentration [3]. Consequently, the primary objective of the present study is to analyse the performance of 70 different kinetic reaction mechanisms in estimating the mole fraction of unburned NH₃ at the combustion exit. Moreover, the study aims to identify the most accurate and reliable model by employing the symmetric mean absolute percentage error (SMAPE) formula as a quantitative metric. This evaluation will be conducted across various equivalence ratios (ϕ) to encompass a comprehensive range of operating conditions.

Kinetic modelling

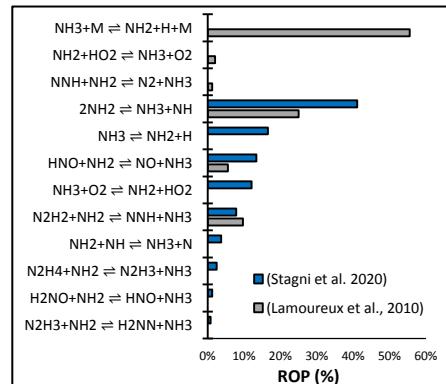
In this study, 70 kinetic reaction mechanisms sourced from the literature were analyzed under atmospheric conditions to assess their performance in predicting the mole fraction of unburned NH₃ for a volumetric fuel mixture consisting of 70% NH₃ and 30% H₂ (Table 1). To conduct these analyses, a burner-stabilized stagnation flame model provided by ANSYS Chemkin-PRO 2022 R2 software was utilized. All numerical simulations were implemented in a one-dimensional computational model with a length of 2 cm, which closely mimicked the experimental setup used in previous studies (specifically, the distance between the nozzle burner and the top plate). Experimental measurements for validation purposes were obtained from [2], where identical fuel mixtures and operating conditions were employed. A stagnation flame configuration was chosen in the experimental setup to ensure accurate measurements and avoid issues with flame stabilization. To quantitatively determine the most accurate model that could faithfully reproduce the experimental measurements, a symmetric mean absolute percentage error (SMAPE) formula was employed as a metric. This formula allowed for a comprehensive evaluation of the models' performance and facilitated the identification of the model with the highest accuracy in predicting the mole fraction of unburned NH₃.

Table 1: Kinetic reaction mechanisms adopted in the present study.

NO.	Kinetic mechanism	No. of Reactions	No. of species	Ref	NO.	Kinetic mechanism	No. of Reactions	No. of species	Ref
1	(Bertolino et al., 2021)	264	38	[4]	36	(Dagaut et al., 2008)	250	41	[5]
2	(Mei, Ma, et al., 2021)	264	38	[6]	37	(Gregory P. Smith et al., 2000)	325	53	[7]
3	(Han et al., 2021)	298	36	[8]	38	(Coda Zabetta & Hupa, 2008)	371	60	[9]
4	(Mei, Zhang, et al., 2021)	257	40	[10]	39	(Alzueta MU, 2016)	654	131	[11]
5	(Gotama et al., 2022)	119	26	[12]	40	(Shmakov et al., 2010)	1207	127	[13]
6	(Shrestha et al., 2021)	1099	125	[14]	41	(Esarte et al., 2011)	536	79	[15]
7	(Z. Wang et al., 2021)	444	91	[16]	42	(Abian et al., 2015)	201	31	[17]
8	(X. Zhang et al., 2021)	263	38	[18]	43	(T. Wang et al., 2018)	925	81	[19]
9	(Arunthanayothin et al., 2021)	2444	157	[20]	44	(T. Faravelli, 2017)	158	29	[21]
10	(Stagni et al., 2020)	203	31	[22]	45	(POLIMI, 2014)	155	29	[23]
11	(Han et al., 2019)	177	35	[24]	46	(Marques et al., 2013)	318	61	[25]
12	(De Persis et al., 2020)	647	103	[26]	47	(Aranda et al., 2013)	566	95	[27]
13	(Mei et al., 2019)	265	38	[28]	48	(Jiang et al., 2020)	60	19	[29]
14	(Li et al., 2019)	957	128	[30]	49	(Sun et al., 2022)	486	66	[31]
15	(Okafor et al., 2019)	356	59	[32]	50	(Song et al., 2019)	158	29	[33]
16	(Glarborg et al., 2018)	231	39	[34]	51	(Mével et al., 2009)	203	32	[35]
17	(Shrestha et al., 2018)	1081	124	[36]	52	(Da Rocha-Mathieu et al., 2019)	66	22	[37]
18	(Otomo et al., 2018)	213	32	[31]	53	(Da Rocha-Otomoet al., 2019)	51	21	[37]
19	(U. Mechanism, 2018)	41	20	[38]	54	(Da Rocha-Okafor et al., 2019)	70	24	[37]
20	(Klippenstein et al., 2018)	211	33	[39]	55	(Kovaleva et al., 2022)	354	59	[40]
21	(Nakamura et al., 2017)	232	33	[41]	56	(Houshfar et al., 2012) Midd temp	91	26	[42]
22	(Y. Zhang et al., 2017)	251	44	[43]	57	(Houshfar et al., 2012) High temp	430	52	[42]
23	(Lamoureux et al., 2016)	934	123	[44]	58	(Houshfar et al., 2012) Low temp	198	35	[42]
24	(Xiao et al., 2017)	276	55	[45]	59	(Caprioli et al., 2021)	2300	201	[46]
25	(Song et al., 2016)	204	32	[47]	60	(Xu et al., 2023)	389	69	[48]
26	(Nozari & Karabeyolu, 2015)	91	21	[49]	61	(Thomas et al., 2022)	1099	125	[50]
27	(Mathieu & Petersen, 2015)	278	54	[51]	62	(Kovács et al., 2020)	214	34	[52]
28	(Duynslaeger et al., 2012)	80	19	[53]	63	(Kovács et al., 2021)	537	70	[54]
29	(Klippenstein et al., 2011)	202	31	[55]	64	(Saxena & Williams, 2007)	288	59	[56]
30	(K. Zhang et al., 2011)	701	88	[57]	65	(Valkó et al., 2022)	537	70	[58]
31	(Lamoureux et al., 2010)	883	119	[59]	66	(Alzueta et al., 2001)	464	65	[60]
32	(Komov, 2009)	1207	127	[61]	67	(Nakamura & Shindo, 2019)	485	66	[62]
33	(Mendiratta & Glarborg, 2009)	779	79	[63]	68	(Glarborg, 2022)	270	41	[64]
34	(Tian et al., 2009)	703	84	[65]	69	(Tang et al. 2022)	211	35	[66]
35	(Singh et al. 2022)	259	32	[67]	70	(Marshall et al. 2023)	228	34	[68]

Results and Discussions

The primary findings of the SMAPE investigations reveal that the performance of the Lamoureux et al. mechanism [59] is satisfactory, displaying an error estimation range of 4% to 7% when considering the ϕ values between 1 and 1.2. However, its accuracy diminishes when estimating the mole fraction of NH_3 at ϕ of 1.4, resulting in underestimation. In contrast, the Stagni et al. mechanism [22] proves to be more precise in predicting the mole fraction of unburned NH_3 under highly rich conditions ($\phi=1.4$).



The conducted sensitivity analysis underscores the significance of specific reaction steps, such as $\text{NH}_3 + \text{O} \rightleftharpoons \text{NO} + \text{H}$, $\text{NH}_3 + \text{M} \rightleftharpoons \text{NH}_2 + \text{H} + \text{M}$, and $\text{NH}_3 + \text{OH} \rightleftharpoons \text{HNO} + \text{H}$, in enhancing the reactivity of the system by facilitating the production of crucial radicals, notably H, which play a vital role in sustaining the reaction process. Moreover, the reaction flow analysis highlights the importance of reactions including $\text{HNO} + \text{NH}_2 \rightleftharpoons \text{NO} + \text{NH}_3$, $2\text{NH}_2 \rightleftharpoons \text{NH}_3 + \text{NH}$, and $\text{NH}_3 + \text{M} \rightleftharpoons \text{NH}_2 + \text{H} + \text{M}$, as they contribute significantly to the formation of NH_3 , Fig.1. Notably, the reactivity of reaction steps $2\text{NH}_2 \rightleftharpoons \text{NH}_3 + \text{N}$ and $\text{NH}_3 + \text{M} \rightleftharpoons \text{NH}_2 + \text{H} + \text{M}$ demonstrates an increase with higher ϕ values, while reaction $\text{HNO} + \text{NH}_2 \rightleftharpoons \text{NO} + \text{NH}_3$ exhibits a decrease. Furthermore, the consumption of NH_3 is predominantly

Fig. 1. Rate of formation of NH_3 at $\phi = 1.4$

governed by reaction steps $\text{NH}_3 + \text{OH} \rightleftharpoons \text{NH}_2 + \text{H}_2\text{O}$, $\text{NH}_3 + \text{H} \rightleftharpoons \text{NH}_2 + \text{H}_2$, and $\text{NH}_3 + \text{O} \rightleftharpoons \text{NH}_2 + \text{OH}$, which are the reactions of NH_3 with the most reactive radicals such as OH, H, and O, Fig.2. These reactions heavily influence the depletion of NH_3 within the system.

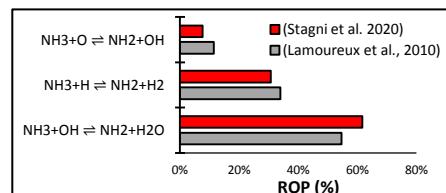


Fig. 2. Rate of consumption of NH_3 at $\phi = 1.4$

Conclusions

This study investigated 70 kinetic reaction models to assess their accuracy in reproducing NH_3 speciation at the combustion exit zone. Differences in reaction steps and rate parameters were observed among the tested mechanisms. The Lamoureux model provided reliable estimates of unburned NH_3 within the ϕ range of 1-1.2, but its accuracy declined near 1.4. NH_3 was primarily converted to NH_2 radicals through OH reactions across all temperatures, with secondary involvement of O radicals at low-intermediate temperatures. NH_3 dehydrogenation also occurred via H radicals through the $\text{NH}_3 + \text{H} \rightleftharpoons \text{NH}_2 + \text{H}_2$ reaction at higher temperatures. Additionally, NH_3 regeneration at the combustion exit was predominantly driven by the $\text{NH}_3 \rightleftharpoons \text{NH}_2 + \text{H}$ reaction at $T=504$ K.

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