Modelling coupled microbial processes in the subsurface: Model development, verification, evaluation and application

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Abstract

To study subsurface microbial processes, a coupled model which has been developed within a Thermal-Hydraulic-Chemical-Mechanical (THCM) framework is presented. The work presented here, focuses on microbial transport, growth and decay mechanisms under the influence of multiphase flow and bio-geochemical reactions. In this paper, theoretical formulations and numerical implementations of the microbial model are presented. The model has been verified and also evaluated against relevant experimental results. Simulated results show that the microbial processes have been accurately implemented and their impacts on porous media properties can be predicted either qualitatively or quantitatively or both. The model has been applied to investigate biofilm growth in a sandstone core that is subjected to a two-phase flow and variable pH conditions. The results indicate that biofilm growth (if not limited by substrates) in a multiphase system largely depends on the hydraulic properties of the medium. When the change in porewater pH which occurred due to dissolution of carbon dioxide gas is considered, growth processes are affected. For the given parameter regime, it has been shown that the net biofilm growth is favoured by higher pH; whilst the processes are considerably retarded at lower pH values. The capabilities of the model to predict microbial respiration in a fully coupled multiphase flow condition and microbial fermentation leading to production of a gas phase are also demonstrated.

Keywords Microbial; Coupled; Transport; Reaction; Model development; Applications.

1. Introduction

Microbial biomass in subsurface porous media consists of both suspended cells and attached biofilms. Microorganisms, such as bacteria under suitable conditions grow and occupy the free spaces in porous media by forming bacterial biofilms. Biofilms are microbial populations, encapsulated in their self-produced extracellular polymeric substances (EPS), attached on solid surfaces submerged in a liquid phase (Bakke, 1986; Mitchell et al., 2009). The presence of microbes and their activities significantly influences the physical and chemical properties of subsurface soils and rocks. In natural subsurface these activities are often complex and coupled with multiple flow and geochemical reactions. For example, microbes alter the chemical compositions and states of soil-water (Murphy and Ginn, 2000), biofilms obstruct fluid flows by sealing inter-particle pore spaces (Rosenzweig et al., 2014) and these processes consequently affect the supply of nutrients and hinders microbial growth.

Microbial activities have adverse or unwanted impacts on public health, ground engineering works etc., but they can be adopted to a wide range useful applications. For example, biofilms are used as bio-barriers. They can also be used for bioremediation of pollutant plumes or to enhance oil recovery (Chen-Charpentier, 1999). They facilitate biotransformation, a process by which toxic pollutants are transformed into non-toxic substances (Cunningham et al., 1991; Chen-Charpentier, 1999). With regard to Carbon Capture and Sequestration (CCS) technologies, subsurface biofilms have been found effective in enhancing CO2 trapping mechanisms and limiting the leakage of sequestered supercritical carbon dioxide through geologic cap-rocks, formation fractures and near the injection wells (Mitchell et al., 2009). Therefore, to ensure their effective usages, understanding of the fundamental processes in porous media is essential.

In saturated porous media, microbial processes and their impacts on physical properties of the media have been studied extensively via laboratory experiments (Trulear and Characklis, 1980; Bakke, 1986; Taylor and Jaffe, 1990a; Cunningham et al., 1991; Vandevivere and Baveye, 1992a, b; Baveye et al., 1992; Seki et al., 1998; Ginn et al., 2002; Mitchell et al., 2009 and others) and by using theoretical and numerical methods (Rittmann and McCarty, 1980; Corapcioglu and Haridas, 1984, 1985; Bakke, 1986; Taylor et al., 1990; Taylor and Jaffe, 1990b, c; Rittmann, 1993; Chen-Charpentier, 1999; Murphy and Ginn, 2000; Seki and Miyazaki, 2001; Thullner and Baveye, 2008 and others). In contrast, limited attempts have been made to explore the processes in unsaturated conditions (Schaefer et al., 1998; Rockhold et al., 2004; Yarwood et al., 2006; Maggie and Porporato, 2007; Mostafa and van Geel, 2007; Gargiulo et al., 2007; Ebigbo et al., 2010; Rosenzweig et al., 2013, 2014).

Microbial cells in the suspended or planktonic state, in saturated or nearly-saturated porous media, are transported via physicochemical processes such as convection, dispersion, diffusion, straining and filtration (Murphy and Ginn, 2000; Ginn et al., 2002). However, in unsaturated conditions, the concept of planktonic free movement is unlikely and microbes predominantly exist as biofilms at the solid surfaces (Or et al., 2007). In saturated conditions, the dominant microbial life is also in biofilms. To assess the impacts of microbial activities in such conditions, it is important to understand the factors influencing the transport and reaction mechanisms as well as the quantity of biomass in the medium. Net accumulation of biofilms and suspended cells depends on growth and decay rates controlled by various physical and chemical processes. Cunningham et al. (1991) reported from Escher (1986) that under constant supply of growth nutrients, sorption related processes are controlled by suspended cell concentrations and growth processes at solid surfaces are regulated by the concentrations of attached microbes on those surfaces. In deep subsurface environments or in absence of a suitable external electron acceptor, bacteria reproduce primarily by metabolising growth substrates or fermentation; however in presence of electron acceptors they grow by respiration (Bethke, 2008). Microbial population reduces due to cell death as well as in presence of biocides. Biocide, such as supercritical

CO2, reduces the number of living cells in the liquid phase (Zhang et al., 2006). The movement of microbes between the planktonic state and sessile state also affects biomass quantity in individual phases. For example, biofilm mass loss due to high liquid shear force at the biofilm-liquid interface (Trulear and Characklis, 1980; Rittmann, 1982; Bakke, 1986) or due to changes in physiochemical conditions (Bakke, 1986); results in an increase of suspended microbes in the liquid phase. In addition, attachment and detachment of cells may take place to and from biofilm phase (Cunningham et al., 1991), until a steady-state is reached between suspended cell and biofilm concentrations. Microbial processes are also affected by the chemical constituents of the medium (Or et al., 2007). Reactive transport and supply of growth nutrients might be affected by the presence of various chemicals and minerals. Conversely microbes promote certain reactions that alter the local geochemical condition of the native media. Microbial growth kinetics are influenced by pH of the system (Ibragimova et al., 1969; Tan et al., 1998; Hoštacká et al., 2010; Rousk et al., 2009). In their experiments, Hoštacká et al. (2010) observed significant growth at pH 8.5 than in pH less than 6.0. As the pH of a system changes, ionization states of the components in the system also changes (Dixon and Webb, 1979). The active components of microbial cells are usually the cell-enzymes (Tan et al., 1998). Enzymes contain ionizable groups which need to be in appropriate ionic states to bind substrates, catalyzes reactions, and to produce biomass (Segel, 1975).The study of such complex coupled interactions in variably saturated porous media is challenging and rarely available in literatures.

In the scope of this study, a microbial model has been developed at the macroscale of a porous medium within a coupled thermal-hydraulic-chemical-mechanical (THCM) framework. The aim of the research is to analyse the impacts of microbial processes on physical and chemical behaviours of the medium which subjected to simultaneous flow, reaction and deformation conditions. The THCM model, COMPASS (Thomas and He, 1998; Seetharam et al., 2007; Masum, 2012; Sedighi et al., 2015), is based on a mechanistic approach in which the mechanisms to explain relevant behaviours are included in an additive manner with inter-related couplings as required. COMPASS is linked with the geochemical model PHREEQC version 2.0 (Parkhurst and Appelo, 1999) which estimates both thermodynamically equilibrium and kinetically controlled chemical reactions. The advanced modelling capabilities have been exploited to investigate the aforementioned complex microbial processes in the subsurface soils.

In this paper, theoretical and numerical developments of the microbial model including the couplings between transport module and reaction module are presented. Verifications of the model and evaluations against experimental results have been conducted. The model has been applied to predict biofilm growth in a variably saturated sandstone core and under changing pH condition. The model is then used to investigate microbial respiration in a coupled two-phase flow condition. Finally, a simulation of microbial growth via fermentation has been demonstrated. Since microbes in unsaturated condition mainly exist by forming biofilms, model simulations and applications presented here are

focused on the biofilm processes only. The feedback of net biomass accumulation on media porosity, permeability is estimated through a mass-volume relationship. In this article, biofilms are assumed to be impermeable and water inside the biofilm is immobile and concentration of substrate in the biofilm is the same as in the liquid phase. In the simulations, it has been considered that the biofilm reached to mature state (Bakke, 1986) during the settlement period and its density remains constant throughout the simulation. That means that although the biofilm mass grows (or reduces) during the simulation, the ratio between bacterial cell mass and biofilm (cell+EPS) mass remains unchanged (at the early stages of biofilm development the ratio varies with time). The model is presented here for isothermal conditions and mechanical stress/ strain is ignored. Microbial processes including suspended cells, thermal gradients and mechanical deformation will be addressed in future publications.

2. The Model

The nomenclature is presented in Table A of Appendix A.

2.1 Theoretical formulation

In an unsaturated porous medium that contains microbial biofilm, the total porosity (n_0) can be divided into liquid phase, gas phase and biofilm phase as,

$$\theta_l + \theta_g + \theta_b = n_0 \tag{1}$$

where θ_l, θ_g, θ_b are the volumetric liquid, gas and biofilm contents, respectively. Growing biofilms occupy inter-particle spaces and restrict the overall flow processes in the medium. Therefore, porosity is affected by the volume of biofilm phase and,

$$\theta_l + \theta_g = n_0 - \theta_b = n. \tag{2}$$

Here n is the active porosity that is unaffected by the biofilm phase and where flow of fluids primarily takes place. By expressing the volumetric liquid content $\theta_l = nS_l$ and the volumetric gas content $\theta_g = nS_g$; the relationship between liquid saturation(S_l) and gas saturation (S_g) yields, $S_g + S_l = 1$. It has been considered that the gas phase is unsuitable for the survival of microbes, as a result, the spread of attached biomass in the solid phases should be encapsulated within the liquid phase volume of the media. Following Effendiev (2013), it has been assumed that growing biofilm assimilates the liquid phase rather than pushing it out of the system.

2.1.1 Conservation of microbial biomass

The mass conservation equation of a suspended cell in the liquid phase is expressed as,

$$\frac{\partial}{\partial t}\left(\theta_l c_b^l\right) = \nabla\left(\theta_l D_b^* \nabla c_b^l\right) + \nabla\left(\theta_l v_l c_b^l\right) + s_b^l \tag{3}$$

where $c_b^l$is the concentration of the suspended microbe and $D_b^*$is the hydrodynamic dispersion coefficient in the liquid phase. Details of hydrodynamic dispersion in the model is presented in Section 2.1.5. v_l represents velocity of the liquid phase and s_b^lrepresents the sinks or sources.

The mass balance equation of a biofilm attached to solid surfaces is given by,

$$\frac{\partial}{\partial t}(c_b^s) = s_b^s \tag{4}$$

where c_b^s is the amount of biofilm per unit volume of the porous media and s_b^s represents the sinks or source terms. Biofilm concentration (c_b^s) is related to biofilm volumetric content via $c_b^s = \theta_b \rho_b^s$, where ρ_b^s is the biofilm mass density *i.e.* the amount of dry biomass per unit wet volume of the biofilm.

Microbial sinks/ sources include physical growth (*e.g.* substrate metabolism, attachment) and decay processes (*e.g.* endogenous decay, biocide decay, detachment, shear loss etc.), local geochemical condition (r_{chem}) and the presence of external sinks or sources (r_{ext}). Therefore,

$$S_b^i = r_\alpha - r_\beta \pm r_{chem} \pm r_{ext} \qquad i \in \{l, s\} \tag{5}$$

where α represents the growth rates and β represents the decay rates. Superscript *l* and *s* represents suspended biomass and attached biofilm, respectively.

Subsurface microbes primarily grow by metabolising growth-limiting substrates. If growth is limited by both a substrate and an electron acceptor, then the process is explained by the dual Monod's kinetics as follows:

$$r_{substrate} = k_+ \left(\frac{c_d^s}{K_s' + c_d^s}\right)\left(\frac{c_d^e}{K_e' + c_d^e}\right)\theta_l c_b^l \qquad \text{[suspended biomass]} \tag{6a}$$

$$r_{substrate} = k_+ \left(\frac{c_d^s}{K_s' + c_d^s}\right)\left(\frac{c_d^e}{K_e' + c_d^e}\right)c_b^s \qquad \text{[attached biofilm].} \tag{6b}$$

Here k_+ is the substrate utilisation rate. c_d^s is the substrate concentration and c_d^e is the concentration of electron acceptor in the liquid phase. K_s' and K_e' are Monod half-saturation constants of substrate and electron acceptor, respectively.

Biomass decay is expressed using a first-order rate as follows:

$$r_{decay} = k_- \theta_l c_b^l \qquad \text{[suspended biomass]} \tag{7a}$$

$$r_{decay} = k_- c_b^s \qquad \text{[attached biofilm].} \tag{7b}$$

Here k_- is a combined decay rate that includes both endogenous and biocide-induced death.

$$k_- = k_-^e + k_-^b \tag{8a}$$

where k_-^e is the endogenous death rate and k_-^b is the biocide mediated reduction rate, which accounts microbial death due to a toxic non-wetting phase such as scCO2, and mass transfer of high

concentrations of CO2 into the aqueous phase. Biocide decay rate as a function of gas phase saturation has been suggested by Ebigbo et al. (2010).

$$k_{-}^{b} = c_{-}^{b}\left(S_g\right)^{c_c} \quad (8b)$$

where c_{-}^{b} and c_c are empirical parameters depending on the bacterial species/ biofilm and on the porous media properties.

Loss of biomass from biofilms might occur due to fluid shear stress. Bakke (1986) observed removal of small particles from biofilms at the biofilm-liquid interface due to the shear stress imposed by the flowing liquid. Following Bakke (1986) biofilm shear loss is written by,

$$r_{shear} = b_s c_b^s \quad (9)$$

where b_s is the detachment rate due to liquid shear stress τ. The relationship between τ and b_s can be expressed as, $b_s = k_\tau \tau$. Here k_τ is a specific shear loss coefficient. For Newtonian liquids, shear stress (τ) can be obtained from dynamic viscosity (μ_l) and velocity gradient. Therefore,

$$\tau = \mu_l \nabla v_l \quad (10)$$

Concentration of suspended cells in the liquid phase is increased by shear loss of biofilms. Meanwhile, attachment of suspended cells from liquid phase to biofilms reduces the amount in suspension. These processes are expressed using a linear first-order relationship.

$$r_{attchment/detachment} = k_a \theta_l c_b^l - k_d c_b^s \quad (11)$$

where $k_a$and k_d are the attachment and detachment rates of cells to and from the biofilms respectively.

Impacts of local geochemical environment on microbial activities are estimated by the r_{chem} term in the model. Concentrations of dissolved chemicals and minerals, redox state, pH etc. are calculated/ updated from bio-geochemical reactions via the geochemical model. The information is then used to predict microbial physical processes implemented in the transport model and vice-versa. For example, dissolution of CO2 in porewater reduces the pH of the system (which is evaluated by the chemical model) and the effect of pH on microbial growth can be estimated from the transport model. Ibragimova et al. (1969) and Tang et al. (1989) proposed a pH dependent growth kinetic,

$$k_{pH} = \frac{k_0^p K_1^p}{K_1^p + [H^+]}. \quad (12)$$

Here k_{pH} is a pH-dependent growth rate. k_0^p is a specific growth rate with respect to pH which determines the shape of the k_{pH}-pH diagram. K_1^p is an empirical constant, known as ionisation constant (Tan et al., 1998) and $[H^+]$ represents the concentration of hydrogen ion (mol/L) in the liquid solution. Figure B1 (Appendix B) shows the behaviour of k_{pH} as a function pH for different values of k_0^p and K_1^p. The pH-dependent microbial growth can be expressed as,

$$r_{chem} = k_{pH} \theta_l c_b^l \quad \text{[suspended biomass]} \quad (13a)$$

$$r_{chem} = k_{pH} c_b^s \quad \text{[attached biofilm].} \tag{13b}$$

Since solution pH influences substrate binding with microbial cells, pH-dependent growth rate is linked with that of the substrate utilisation, *i.e.* Equation (6). In absence of a growth substrate, solution pH alone does not influence microbial growth. In a similar manner, the effects of other chemical processes on the net microbial growths can be included. Implementations of the microbial processes within the THCM model and the linkage with the geochemical model are described in section 2.2.

2.1.2 Conservation of dissolved chemicals

The governing equation of multicomponent chemical flow in a liquid phase is given by,

$$\frac{\partial(\theta_l c_d^i)}{\partial t} = \nabla\left(\theta_l D_d^* \nabla c_d^i\right) + \nabla\left(\theta_l c_d^i v_l\right) + s_d^i \tag{14}$$

where c_d^i represents the concentration and D_d^* is the hydrodynamic dispersion coefficient (Section 2.1.5) of the i^{th} component in the liquid phase. S_d^i represents the total sink/ source for the i^{th} component including geochemical reactions, microbial interactions and any external source or sink. Microbial growth reduces the amount of substrate and electron acceptor (*i.e.* dissolved oxygen) and their respective sinks s_d^s, s_d^e can be expressed as,

$$s_d^s = -r_{substrate}/Y \tag{15a}$$

$$s_d^e = -F\, r_{substrate}/Y \tag{15b}$$

where Y is the growth yield *i.e.* the amount of biomass created per unit mole of substrate (Bethke, 2008) and F is the oxidiser yield which represents the amount of oxygen consumed per unit mass of substrate (Murphy and Ginn, 2000). Please note in Equation (6) $i = s$ denotes the presence of a single growth substrate.

2.1.3 Conservation of liquid and gas

The mass conservation equation for the liquid phase flow is expressed as,

$$\frac{\partial(\theta_l \rho_l)}{\partial t} = \nabla(\rho_l v_l) + S_s \tag{16}$$

where, ρ_l is the liquid density which is constant in this study and S_s represents the liquid phase sink/ source. Liquid velocity (v_l) is calculated using the Darcy's law,

$$v_l = -\frac{K_{int} k_{rl}}{\mu_l} \nabla u_l. \tag{17}$$

Here u_l denotes the porewater pressure, k_{int} is the in-situ intrinsic permeability, k_{rl} is the liquid phase relative permeability.

The multicomponent gas transport equation is given by,

$$\frac{\partial(\theta_g c_g^i)}{\partial t} = \nabla\left(\theta_g D_g^i \nabla c_g^i\right) + \nabla\left(\theta_g c_g^i v_g\right) + s_g^i. \tag{18}$$

Here c_g^i is the concentration and D_g^i is the effective diffusion coefficient of the i^{th} gas species. Since, gas phase molecular diffusion often dominates mechanical dispersion (Costanza-Robinson and Brusseau, 2006), effective diffusion coefficient of i^{th} species is calculated as,

$$D_g^i = \tau_g D_g^0. \tag{19a}$$

Here D_g^0 is the molecular diffusion coefficient of gas in free flow condition. In a mixture of gases diffusion of one component may be affected by the others. Estimation of multicomponent molecular diffusion coefficients in the model is based on the method (Generalized Multicomponent Fick's Law) proposed by Taylor and Krishna (1993) and has been presented elsewhere (Masum et al., 2012; Masum, 2012). However, multi-nary interactions among gas components have been ignored in this paper and only self-molecular-diffusion of components has been considered. τ_g in Equation (19a) is the gas phase tortuosity factor, which is obtained from the Millington and Quirk (1961) model as,

$$\tau_g = n^{1/3} S_g^{7/3}. \tag{19b}$$

The sink/ source term s_g^i includes gas phase reactions, dissolution (or formation) in the liquid phase and external sinks or sources of the i^{th} gas species. Partitioning of components between gas phase and liquid phase is considered to be in equilibrium following Henry's law. Gas components, which dissolve in liquid phase, are treated as dissolved chemicals (Equation 14) and therefore, the i^{th}component of s_g^i is linked with that of s_d^i via $c_d^i = H_c c_g^i$. Here, H_c is Henry's constant.

The gas phase velocity,

$$v_g = -\frac{K_{int} k_{rg}}{\mu_g} \nabla u_g \tag{20}$$

where k_{rg} is the gas phase relative permeability and μ_g is the dynamic viscosity of the gas phase. The total gas pressure (u_g) is obtained by using the ideal gas law.

$$u_g = \sum_{i=1}^{N_g} c_g^i RT \tag{21}$$

Here $N_g$is the total number of gas components, R is the universal gas constant and T is the reference temperature.

Original intrinsic permeability ($k_{int,0}$) of porous media, which is a function of material structure only, is affected by biofilm growth. The in-situ intrinsic permeability (k_{int}) is estimated from the original permeability using the expression given by Somerton et al. (1975).

$$\frac{K_{int}}{k_{int,0}} = \left(\frac{n}{n_0}\right)^3 \tag{22}$$

2.1.4 Soil water characteristic behaviour and relative permeability

In a multiphase system, the presence of both gas phase and liquid phase leads to matric suction (s) which is expressed as, $s = u_g - u_l$. Suction often regulates the saturation states of a porous medium and it is measured from water retention behaviours of the medium. In this paper, the water retention behaviour is based on the van Genuchten (1980) model.

$$S_l = S_r + (1 - S_r)\left[\frac{1}{1 + |\alpha h|^{\beta}}\right]^{m} \qquad m = 1 - \frac{1}{\beta} \tag{23}$$

where α, m, β are curve fitting parameters, S_r is the residual degree of saturation and h is suction head ($= s/\gamma_l$). Here, γ_l is the unit weight of water.

The liquid phase relative permeability is defined by (van Genuchten, 1980),

$$k_{rl} = S_e^{1/2}\left(1 - (1 - S_e^{1/m})^{m}\right)^{2} \tag{24}$$

Parker et al. (1987) presented the gas phase relative permeability,

$$k_{rg} = (1 - S_e)^{1/2}(1 - S_e^{1/m})^{2m}. \tag{25}$$

Here $S_e$denotes the effective saturation.

$$S_e = \frac{S_l - S_r}{1 - S_r} \tag{26}$$

2.1.5 Hydrodynamic dispersion

Hydrodynamic dispersion coefficient (Equation 3 & 14) includes both mechanical dispersion coefficient and effective molecular diffusion coefficient. Bear and Verruijt (1987) proposed hydrodynamic dispersion coefficient as,

$$D_d^* = D_d^h + D_d^i. \tag{27a}$$

Here D_d^h is the coefficient of mechanical dispersion and it is considered to be a function of the average fluid velocity (Pickens and Gillham, 1980). Hydrodynamic dispersion affects the spread of dissolved chemicals or suspended microbes both in parallel (longitudinal) and in perpendicular (transverse) directions to flow. In this paper, only longitudinal dispersion is considered. Therefore,

$$D_d^h = \alpha_L |v_l| \tag{27b}$$

where, α_L is the coefficient of longitudinal dispersivity and $|v_l|$ is the absolute average velocity of liquid phase.

The effective molecular diffusion coefficient of i^{th} chemical component is calculated as,

$$D_d^i = \tau_l D_d^0. \tag{28a}$$

Here D_d^0 is the molecular diffusion coefficient of chemical in free flow and τ_l is the porous media tortuosity factor in the liquid phase, which is obtained from the Millington and Quirk (1961) model as,

$$\tau_l = \theta_l^{7/3}/n^2. \quad (28b)$$

275

276 *2.2 Numerical formulation*

277 The microbial model has been developed within the THCM model, COMPASS (COde of Modelling
278 PArtially Saturated Soils). The detailed developments of COMPASS including theoretical and
279 numerical formulations, verifications, validations and numerous applications have been presented
280 elsewhere (Thomas and He, 1998; Seetharam, 2003; Seetharam et al., 2007; Masum, 2012; Sedighi et
281 al., 2015). In the model, the governing transport equations are expressed in terms of the primary
282 variables, *i.e.* porewater pressure (u_l), poregas concentration ($\boldsymbol{c_g}$), dissolved chemical concentration
283 ($\boldsymbol{c_d}$), suspended biomass concentration ($\boldsymbol{c_b^l}$), biofilm concentration ($\boldsymbol{c_b^s}$), temperature (T) and
284 displacement ($\boldsymbol{u}$). For example, Equation (3) can be expressed in terms of primary variables as follows:

$$C_{c_b l}\frac{\partial u_l}{\partial t} + C_{c_b c_g}\frac{\partial c_g}{\partial t} + C_{c_b c_b}\frac{\partial c_b^l}{\partial t} + C_{c_b u}\frac{\partial \boldsymbol{u}}{\partial t} = \nabla\left(K_{c_b c_b}\nabla c_b^l\right) + \nabla\left(K_{c_b l}\nabla u_l\right) + s_b^l \quad (29)$$

285 where,

286 $$C_{c_b l} = -nc_b^l\frac{\partial S_l}{\partial s}, C_{c_b c_g} = -nRTc_b^l\frac{\partial S_l}{\partial s}, C_{c_b c_b} = nS_l, C_{c_b u} = S_l c_b^l W^{\mathrm{T}}\mathrm{P}, K_{c_b c_b} = \theta_l D_b^*,\ K_{c_b l} = \frac{K_{int}k_{rl}}{\mu_l}$$

287 Here P is the strain matrix and $\boldsymbol{W}$ is a vector of differential operators. Following that, the equations are
288 spatially discretised using Galerkin Finite Element Method (GFEM). Please note that the 7th term (or
289 microbial sinks/ sources) in Equation (29) is implemented in the model following a sequential non-
290 iterative approach (SNIA). As per this approach, the sink/source is calculated only once in each time
291 step after the convergence of the transport equations are achieved. Therefore, dropping this term, the
292 approximated form of Equation (29) yields,

$$-C_{c_b l}\frac{\partial \hat{u}_l}{\partial t} - C_{c_b c_g}\frac{\partial \hat{c}_g}{\partial t} - C_{c_b c_b}\frac{\partial \hat{c}_b^l}{\partial t} - C_{c_b u}\frac{\partial \hat{\boldsymbol{u}}}{\partial t} + \nabla\left(K_{c_b c_b}\nabla \hat{c}_b^l\right) + \nabla\left(K_{c_b l}\nabla \hat{u}_l\right) = R_\Omega \quad (30)$$

293 Here R_Ω is the residual error imposed due to the approximation over the domain, Ω and (^) indicates
294 the approximated primary variables. The aim of the Galerkin weighted residual method is to reduce the
295 residual error to zero in some average sense over the domain. The matrix form of the governing
296 equations, following the GFEM, can be expressed as follows:

$$\boldsymbol{A\varphi} + \boldsymbol{B}\frac{d\boldsymbol{\varphi}}{dt} + \boldsymbol{C} = \{\boldsymbol{0}\} \quad (31)$$

297 where $\boldsymbol{A}$, $\boldsymbol{B}$, $\boldsymbol{C}$ are the matrices of coefficients and $\boldsymbol{\varphi}$ is the vector of primary variables *i.e.*, $\varphi =$
298 $\{u_l, T, c_g^i, \ldots\ldots, c_g^{N_g}, c_d^i, \ldots\ldots, c_d^{N_d}, c_{b,i}^l, \ldots\ldots, c_{b,N_b^l}^l, c_{b,i}^s, \ldots\ldots, c_{b,N_b^s}^s, u\}$. Here, N_g, N_d, N_b^l and N_b^s are the total
299 number of gas, dissolved chemicals, suspended biomass and biofilm species in the system respectively.
300 An implicit mid-interval backward difference procedure is used for temporal discretisation of Equation
301 (31). Finally, an iterative solution procedure called the predictor-corrector algorithm (Douglas and
302 Jones, 1963) is applied to solve the set of equations. A schematic diagram (or flowchart) describing the
303 coupled microbial processes in COMPASS and the linkage with PHREEQC is presented in Figure 1.

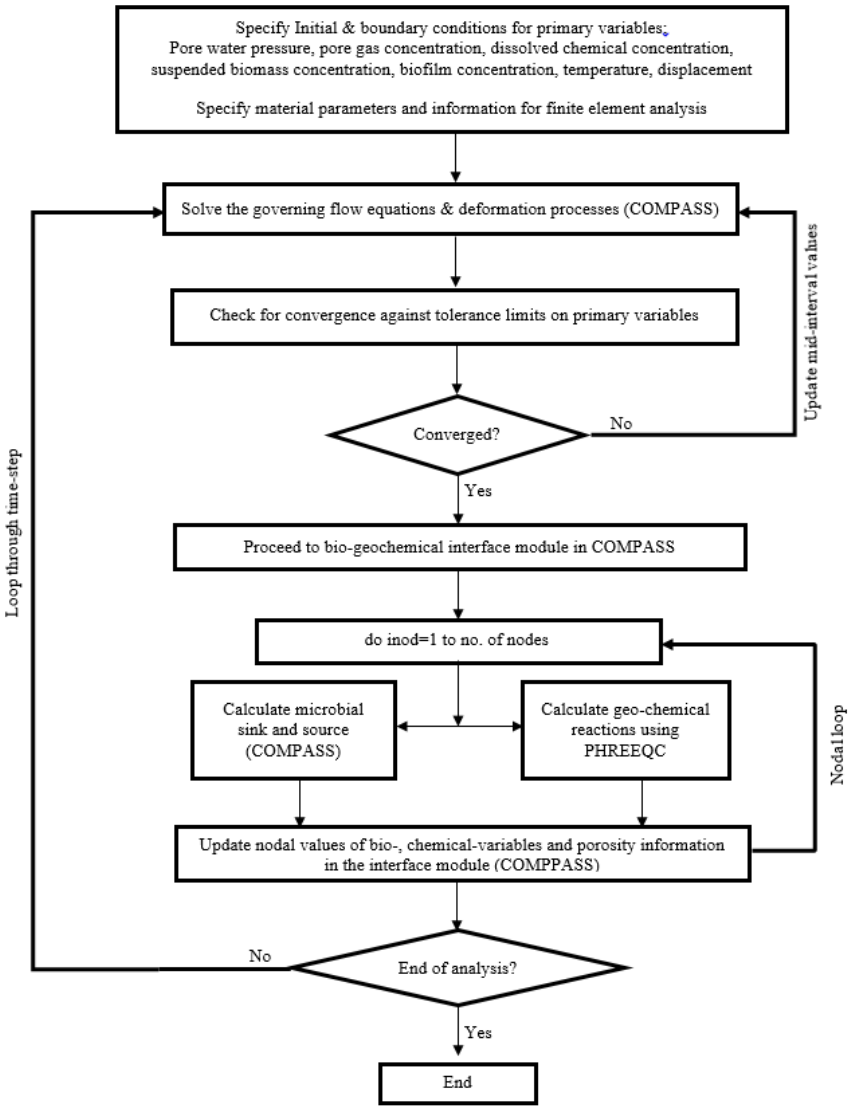

Figure 1 Flowchart diagram of the coupled microbial model. The transport model, COMPASS, is linked with geochemical reaction model, PHREEQC version 2.0. The microbial processes and geochemical reactions are linked via SNIA, since they are handled only once in every time step after the convergence of transport equations occurs.

COMPASS code has been developed on Fortran F90 while PHREEQC is available in C Programming language. The COMPASS-PHREEQC model runs on a combine Fortran-C platform. Once the convergence of primary variables (solving governing flow and deformation equations) is achieved, the programme proceeds to the bio-geochemical interface (in COMPASS) where microbial and geochemical reaction sink/ sources are estimated at every nodal points. Depending on the problem, either of the sink/ sources can be estimated first. For example, dissolution of CO2 reduces pH of a system, which consequently affect microbial growth. In this case, geochemical reaction (in PHREEQC) is estimated initially and then the updated information is used to calculate microbial sink/ sources.

Concentrations of chemicals, minerals, gases and microbes (for microbial-induced mineral kinetics), from the bio-geochemical module, are passed to PHREEQC as input data. Simultaneously an input file, including relevant thermodynamic and kinetic reactions information, is also provided to proceed PHREEQC calculations. Following the measurements of microbial and geochemical reaction sink/ sources, the primary variables and porosity information at the nodal points are updated and the programme continues to the next time-step.

3. Verification

In this section, two examples of the model verifications are presented. The aim is to demonstrate the implementation accuracy and conceptual testing of the microbial processes in a coupled multiphase system.

3.1 Biofilm growth at a maximum rate

Considering $c_d^s \gg K_s'$ and $c_d^e \gg K_e'$ then $\frac{c_d^s}{K_s'+c_d^s} \cong 1$ and $\frac{c_d^e}{K_e'+c_d^e} \cong 1$, which lead to biofilm growth at a maximum rate (*i.e.* Equation (6b)). If biofilm growth is the only process of interest, Equation (4) yields,

$$\frac{\partial c_b^s}{\partial t} = k_+ c_b^s \tag{32}$$

Here k_+ represents the maximum growth rate and the growth is limited by neither the substrate nor the electron acceptor. The analytical solution of Equation (32) is: $c_b^s(t) = c_b^s(0)e^{k_+ t}$.

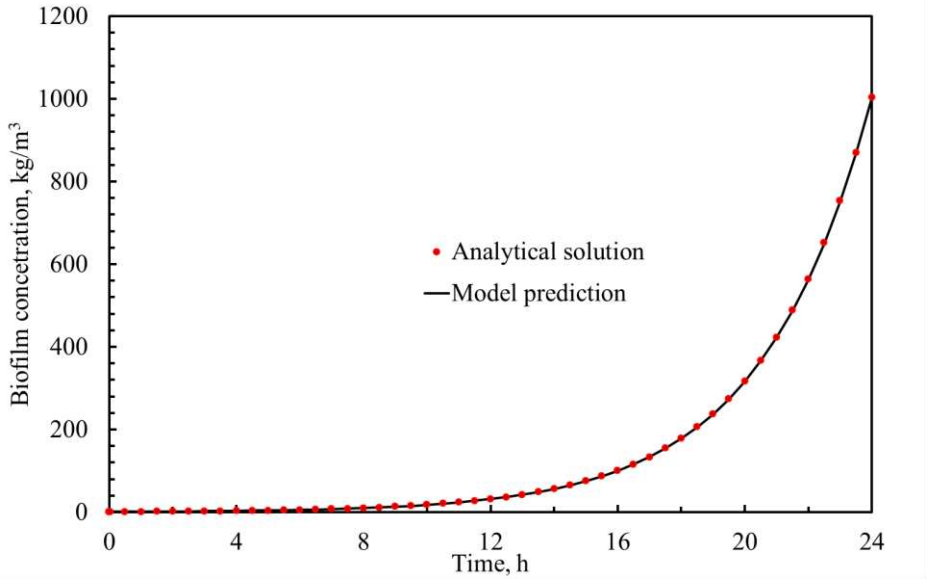

Figure 2 Comparison of the model predicted biofilm growth to the analytical solution.

For an initial biomass concentration, $c_b^s(0)$ = 1.0 kg/m^3 and $k_+ = 8.05\times10^{-5}$ s^{-1}, the results of biofilm growth for 24 h are presented in Figure 2. The results show that the model predicted result is in good agreement with the analytical solution.

3.2 Biofilm growth in a multiphase system

Growing biofilm in a multiphase system affects the flow of other phases. In this exercise, a 0.50 m by 0.05 m unsaturated sandstone sample is used to investigate such behaviour. It is assumed that no biocide exists and the growth nutrient is constantly available to the microbes during the simulation. Therefore, the substrate sink is omitted. It is also assumed that electron acceptors do not limit biofilm growth. The sample domain is discretized into 100 equal-sized quadrilateral elements. The simulation is carried out for 10 d.

3.2.1 Simulation conditions

Initial porewater pressure and poregas concentration are -2×10^3 Pa and 4.036 mol/m^3, respectively. Initial biofilm concentration, $c_b^s = 0.001$ kg/m^3 while the suspended biomass concentration, $c_b^l = 0$. Concentration of the glucose substrate (c_d^s) during the simulation ($t \geq 0$) is 25×10^{-3} kg/m^3.

At the left boundary, *i.e.* x $= 0$, gas is injected at the rate of 1.0×10^{-4} mol/m^2/s. At the right boundary *i.e.* x = 0.50, water pressure is fixed at 1.0×10^6 Pa.

3.2.2 Results

The simulation parameters are presented in Table 1 and the results are in Figure 3. The results show that the volumetric liquid content (θ_l) in the sample (at x = 0.10) increases rapidly from 0.21 to 0.249 by the supplied water from the fixed boundary. The flowing water displaces poregas and θ_g reduces. The system remains nearly water saturated until the poregas pressure is high enough (after 11.52 minutes) to push the waterfront away from the gas injection face. Eventually the gas phase desaturates the sample, resulting in the minimum or residual liquid saturation state (s_r = 0.612 which corresponds to $\theta_l = 0.153$). The flow processes are relatively fast in sandstone due to weak water holding capacity. It is noticeable from the results that the biofilm phase is relatively small during the first 24 h of the simulation to exert any noticeable influence on the system. It grows rapidly after two days and reaches a maximum after 5.8 d. Since the sample has already reached to the residual liquid saturation, biofilm growth mainly occurred in the residual water volume. At this stage, the entire liquid volume disappears into the biofilm phase and the remaining void volume is now occupied by the gas phase only. The active porosity (n) is affected by the growing biofilm following the phase-volume relationships considered in the model, *i.e.* Equations (1) and (2). After 5.8 d the sample porosity reaches to a minimum value of 0.149.

Table 1 Parameter values for the verification of biofilm growth under multiphase flow condition.

Parameters	Values	Comments
Medium and fluid flow parameters:		
Porosity, n_0	0.25	
Intrinsic permeability, $K_{int,0}$	3.98×10^{-14} m^2	Mitchell et al. (2009)
Viscosity of water, μ_l	0.9×10^{-3} Pa s	Fredlund and Rahardjo (1993)
Viscosity of the gas, μ_g	1.5×10^{-5} Pa s	Mitchell et al. (2009)
Diffusion coefficient of the gas in air, D_g^0	1.0×10^{-5} m^2/s	Fredlund and Rahardjo (1993)
Henry's constant, H_c	6.1×10^{-4} mol/L/atm	Sander (2015); for nitrogen gas
Universal gas constant, R	8.3142 J/K/mol	
Absolute temperature, T	298 K	
Biofilm Parameters:		
Substrate utilisation rate, k_+	8.01×10^{-5} s^{-1}	Beyenal et al. (2003)
Yield coefficient, Y	0.628 kg/kg	Beyenal et al. (2003)
Monod half-saturation constant, K_s'	26.9×10^{-3} kg/m^3	Beyenal et al. (2003)
Endogenous death rate, k_-^e	3.18×10^{-7} s^{-1}	Taylor and Jaffe (1990)
Shear loss coefficient, b_s	2.97×10^{-6} s^{-1}	Rittmann (1982)
Biofilm density, ρ_b^s	65 kg/m^3	Peyton (1995)
Water retention parameters:		
α	0.79 m^{-1}	(van Genuchten, 1980)
β	10.4	(van Genuchten, 1980)
s_r	0.612	(van Genuchten, 1980)

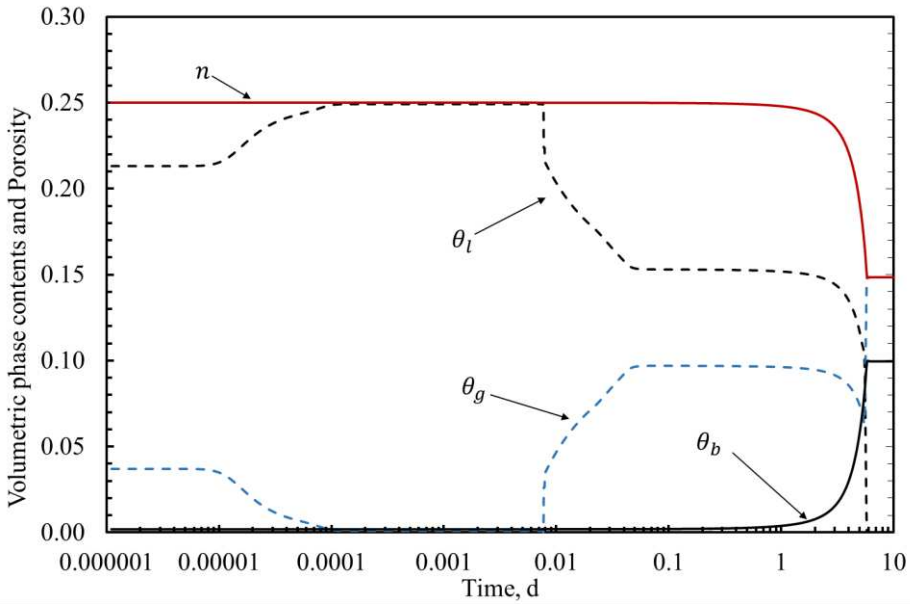

Figure 3 Biofilm growth in a two-phase flow system. Evolution of liquid phase, gas phase, biofilm phase and porosity. Please note, the vertical-axis scales both porosity and volumetric phase contents (θ). The black *dashed line* represents liquid content and the blue *dashed line* for gas content.

Figure 3 results show that, at any time, the corresponding volumetric contents of liquid, gas and biofilm phases accumulate to the initial or unaffected system porosity (n_0). That suggests the coupled two-phase processes are properly implemented in the model.

4. Model Evaluation

In this section, the model is evaluated against the experimental results of relevant interests. A laboratory-based test has been chosen from the literature, which estimated the effects of biofilm growth on physical properties of porous media.

4.1 Model evaluation against experiments of Cunningham et al. (1991)

Cunningham et al. (1991) carried out laboratory-scale experiments to investigate the effects of biofilm growth on porosity and permeability of saturated porous media. 50 mm by 9 mm by 2 mm porous media biofilm reactors were filled with either glass spheres, sand or a mixture of both glass and sand. The experiments were performed under a constant piezometric boundary condition at the inlet and the outlet and the volumetric flow rate was measured at a regular interval for 8 to 12 days. *Pseudomonas aeruginosa* inoculum was used in their experiments. Since the bacteria form uniform biofilms, and the kinetic and stoichiometric coefficients of this microorganism are well documented in literatures. Prior to the tests, 5 mL of the concentrated inoculum was injected into each of the sterile reactors under steady-state conditions to enable initial adsorption of the microbial cells and the formation of biofilms in the solid phase. After 8 hours of settling period and significant sorption, reactors were flushed to remove non-adsorbed cells and steady-state condition was established to begin the experiments. 25×10^{-3} kg/m^3 glucose substrate was continuously supplied in the liquid phase of the porous media during the tests.

4.1.1 Simulation conditions

Initial biofilm concentration in the reactor is calculated by measuring the bacterial cell weight in the 5 mL inoculum, which contained approximately 10^8 cells per mL of the inoculum (Cunningham et al., 1991). Kim et al. (2012) reported that the dry weight of *Pseudomonas aeruginosa* cells varies between 6.4×10^{-11} to 2.8×10^{-12} g/cell. In this case, 1.0×10^{-12} g/cell is chosen to obtain the initial concentration of biofilm, $c_b^s = 0.55$ kg/m^3. Please note that due to lack of sufficient data, almost all of the cells in the inoculum is assumed to be absorbed onto the solid phase. Concentration of suspended biomass in the liquid phase is negligible; therefore, $c_b^l = 0$. Since, continuous supply of substrate was ensured during the tests, its concentration during the simulation ($t \geq 0$) is 25×10^{-3} kg/m^3. At $t = 0$, the saturated porewater pressure $u_l = 100$ Pa.

At the left (x = 0) and right (x = 0.05) boundaries, the applied hydrostatic pressures are 100 Pa and 350 Pa, respectively.

409

410 *4.1.2 Parameters*

411 Peyton (1995) reported volumetric mass density of a number of mono- and mixed-population biofilms.
412 The values range between 5 and 130 kg/m^3. For *Pseudomonas aeruginosa*, Peyton (1995) calculated
413 the average biofilm density of 65.3 kg/m^3. In this simulation, an average density of 85 kg/m^3 is used.
414 Parameters of substrate utilisation kinetics were collected from Beyenal et al. (2003) as, $k_+ = 8.01\times10^{-5}$ s^{-1}
415 and $K_s' = 26.9\times10^{-3}$ kg/m^3. The endogenous death rate, $k_-^e = 3.18\times10^{-7}$ s^{-1} (Taylor and Jaffe, 1990).
416 The shear detachment rate, $b_s = 3.21\times10^{-6}$ s^{-1} (Rittmann, 1982). The porosity and original intrinsic
417 permeabilities ($K_{int,0}$) of the 0.70 mm and 0.54 mm sand are 0.40 and 0.38 and 3.2×10^{-10} m^2 and 2.2×10^{-10} m^2, respectively. The viscosity of liquid water, $\mu_l = 0.895\times10^{-3}$ Pa s (Fredlund and Rahardjo, 1993).
418
419

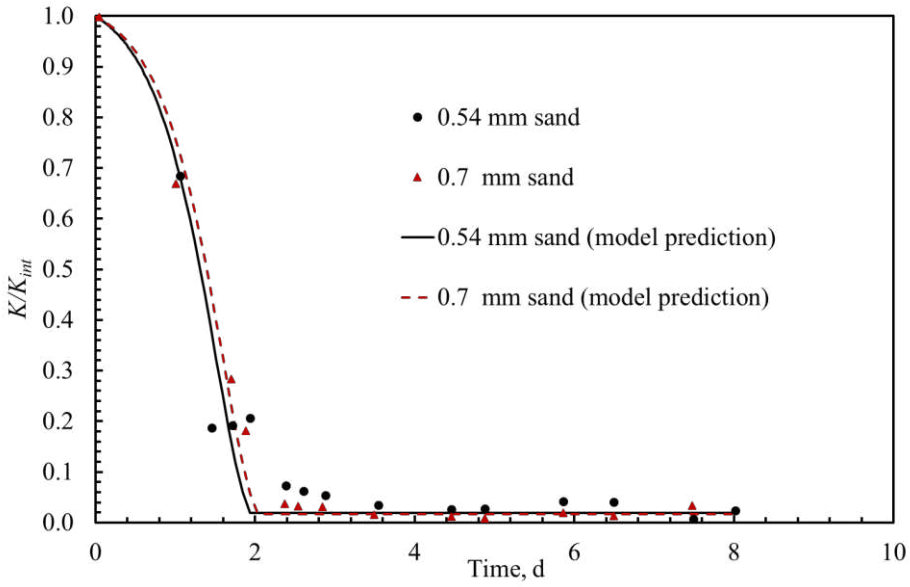

Figure 4 Permeability reduction due to biofilm growth in saturated biofilm reactors. Comparison between model results and the experimental results of Cunningham et al. (1991).

420

421 *4.1.3 Results*

422 The model domain is discretised into 100 equally sized quadrilateral elements. The simulation is carried
423 out for 8 d. Model predicted results for the 0.54 mm and 0.7 mm sand reactors are presented in Figure
424 4. The results are obtained at x = 0.025 m. The simulation results are in good agreement with the results
425 of permeability reduction obtained by Cunningham et al. (1991). Biofilm growth affects the active
426 porosity of the sand reactors, which consequently alter the in-situ intrinsic permeability of the media
427 following Equation (22). Permeability of both reactors drops to the minimum relatively fast (in around
428 2 days) and remains steady until the end of the simulation. The fast growing biofilm undermines the
429 overall impacts of biomass reductions (endogenous death and shear loss in this case). The minimum

permeability predicted in these simulations are approximately 2% of the original value, which is within the range of values (between 1 and 5%) observed by Cunningham et al. (1991).

5. Application

In this section, the model has been applied to investigate subsurface microbial process. Four sets of simulations are presented to observe i) microbial growth at various gas injection rates, ii) effect of pH on the growth, iii) microbial respiration in a fully coupled multiphase condition and, iv) microbial fermentation and gas production. The model domain is a 0.5 m by 0.125 m sandstone core. The domain is discretized into 100 quadrilateral elements with finer spatial discretization at the boundaries, as shown in Figure 5.

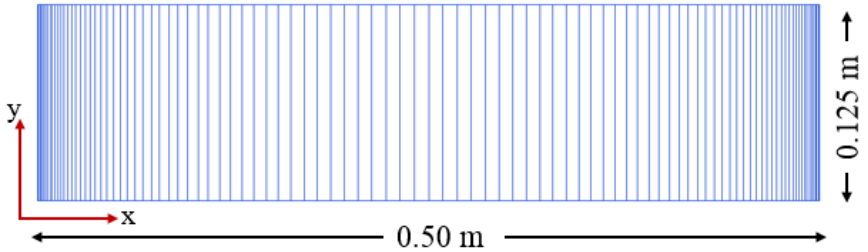

Figure 5 Simulation mesh of the sample domain.

5.1 *Biofilm growth in two-phase condition*

In these simulations, biofilm growth is investigated under simultaneous flow of water and a gas. The objective is to investigate the response of microbial growth and its effect on porous media flow properties at different gas injection rates. Two tests have been carried out, where injection rate in Test I is higher than in Test II. It has been assumed that the substrate is abundantly available to microbes and the growth is not limited by an electron acceptor. The simulations have been carried out for 24 h.

5.1.1 *Initial and boundary conditions*

Initial porewater pressure (u_l) in the core is -2×10^3 Pa, gas concentration, $c_g = 4.04$ mol/m^3, biofilm concentration, $c_b^s = 1.0$ kg/m^3 and the concentration of suspended biomass, $c_b^l = 0$.

At the right boundary, *i.e.* at x = 0.50 gas is injected at the rate of 1.0×10^{-6} mol/m^2/s and 1.0×10^{-7} mol/m^2/s in Test I and Test II, respectively. The left side of the core (*i.e.* at x = 0) is fixed at a water pressure of 100 Pa. The left boundary and the right boundary are impermeable for gas and water, respectively. Concentration of the glucose substrate during the simulation ($t \geq 0$) is 25×10^{-3} kg/m^3.

5.1.2 *Parameters*

The simulation parameters are listed in Table 2.

460 **Table 2** Parameter values for Test I and Test II simulations.

Parameters	Values	Comments
Medium and fluid flow parameters:		From Table 1
Biofilm Parameters:		
Substrate utilisation rate, k_+	8.01×10^{-5} s^{-1}	Beyenal et al. (2003)
Monod half-saturation constant, K_s'	26.9×10^{-3} kg/m^3	Beyenal et al. (2003)
Endogenous death rate, k_-^e	3.18×10^{-7} s^{-1}	Taylor and Jaffe (1990)
Shear loss coefficient, b_s	2.97×10^{-6} s^{-1}	Rittmann (1982)
Biofilm density, ρ_b^s	65 kg/m^3	Peyton (1995)
Water retention parameters:	From Table 1	

461

462 5.1.3 *Results*

463 The simulation results are obtained from the gas injection boundary *i.e.* x = 0.5. The results in Figure 6
464 show that the liquid saturation in the core increases rapidly from 0.85 to 0.87 due to the fixed hydrostatic
465 boundary. The core remains nearly water saturated until the poregas pressures is large enough to drive
466 the waterfront away from the gas injection face. As expected, the core starts to desaturate earlier in Test
467 I than in Test II. The core reaches to the minimum liquid saturation after 4.2 h in Test I but in Test II
468 the liquid saturation reduces to 0.68 after 24 h of simulation. Figure 7 shows the results of biofilm
469 growth and its effects on the core porosity. During the saturation and desaturation period, biofilm phase
470 remains too small to exert any noticeable change on the porosity of the core. The impact escalates with
471 the net growth of the biofilm phase which is limited by the volume of available water in the core.
472 Biofilm concentration and porosity reduction in Test II is larger than in Test I, since the desaturation of
473 the core in Test II is slower which provides more time for the biofilm to grow before liquid phase
474 reaches to the minimum. The results show that the core porosity is reduced to 0.16 and 0.15 in Test I
475 and II which are 64% and 60% of the original unaffected porosity, respectively. Figure 8 shows the
476 evolution of gas pressure (and concentration) for the corresponding gas injection rates. After 24 h the
477 observed gas pressure in Test I is 188.8 kPa while in Test II 14.8 kPa.

478

479 At the early stages of the simulations, when fluid flow processes are dominant, biofilm phase remains
480 considerably small and liquid shear loss is negligible. At the later stages, when biofilm growth is
481 significant, fluid flow is minimum and shear loss is insignificant. For the current parameter values, the
482 results suggest that under constant supply of substrates, growth processes surpass the overall decay rates
483 and promote net accumulation of biofilm in the sandstone core. However it is worthwhile to mention
484 that the water phase in natural soils at residual saturation might be discontinuous and the notion of
485 uninterrupted supply of growth nutrients to the microbes in such condition may lead to an
486 overestimation.

487

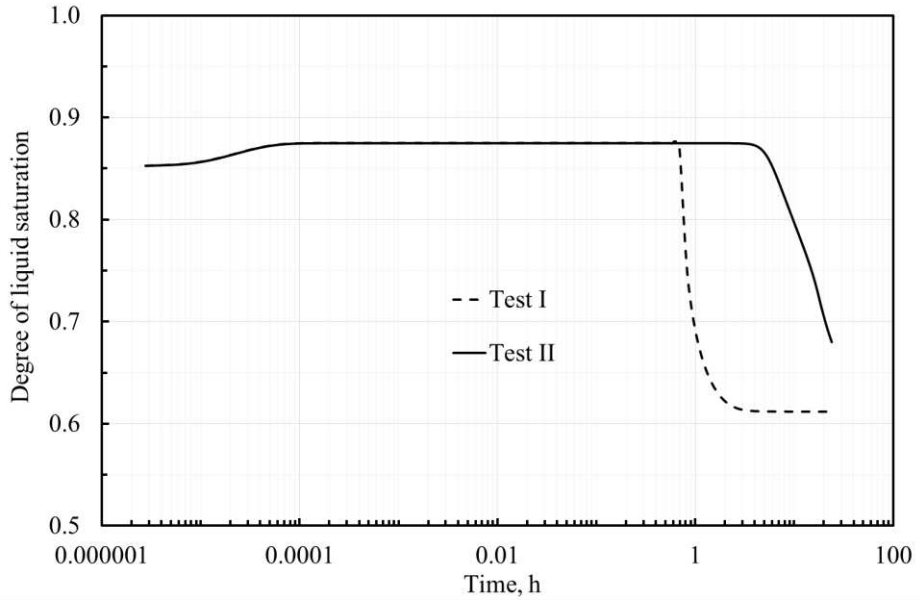

Figure 6 Evolution of water saturation in the sandstone core under simultaneous flow of water and gas. Gas injection rates for Test I and Test II simulations are 1.0×10^{-6} mol/m^2/s and 1.0×10^{-7} mol/m^2/s, respectively.

488

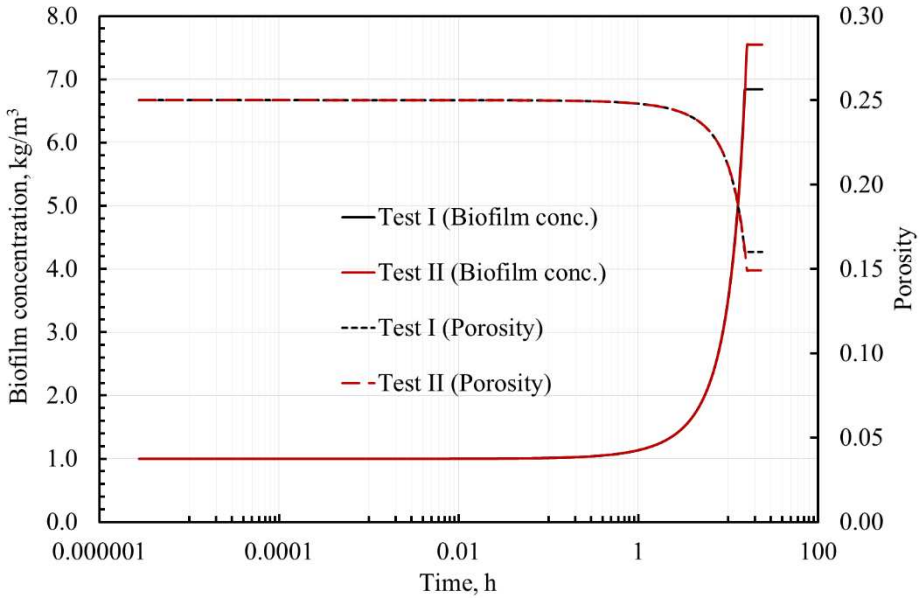

Figure 7 Biofilm concentration and the effect on sandstone porosity for Test I and II. The *solid lines* represent biofilm concentration on the left vertical axis and the *dashed lines* represent porosity on the right vertical axis.

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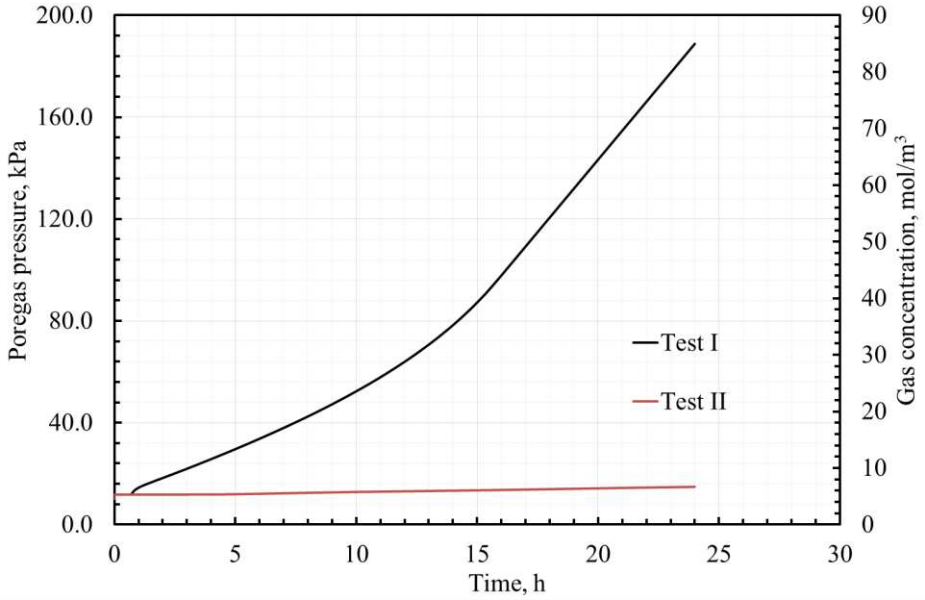

Figure 8. Gas pressure (concentration) evolution during Test I and II simulations.

490

491 5.2 *Effect of pH on biofilm growth*

492 The aim of this section is to observe biofilm growth under variable pH. Two set of simulations have
493 been carried out in that regard. In the first set biofilm growth is predicted under a constant pH. In the
494 second simulation injection and dissolution of CO2 gas in the sandstone water has been considered.
495 Aqueous carbon dioxide, CO2 (aq), reacts with water and forms aqueous carbonic acid, H_2CO_3. The
496 carbonic acid may lose up to two protons to form bicarbonate and carbonate species. The released proton
497 eventually reduces the pH of the system. The overall reaction:

$$CO_2(g) \leftrightarrow CO_2(aq) \quad \text{(R1.1)}$$

$$CO_2(aq) + H_2O \leftrightarrow H_2CO_3 \quad \text{(R1.2)}$$

$$H_2CO_3 \leftrightarrow 2H^+ + CO_3^{2-} \quad \text{(R1.3)}$$

498 The reactions (R1) have been modelled using PHREEQC. To emphasis on the effect of pH on biofilm
499 growth following assumptions have been made at this stage: substrate concentration remains constant
500 throughout the simulation, growth is not limited by electron acceptors, substrate doesn't influence the
501 solution pH and microbial metabolism of this substrate doesn't produce any gas. The simulations have
502 been carried out for 10 h.

503

504 5.2.1 *Initial and boundary condition*

505 In both simulations, initially fully water saturated sandstone core is assumed to contain 1.0 kg/m^3 of
506 biofilm at pH 7.0. Concentration of the substrate during the simulation ($t \geq 0$) is 25×10^{-3} kg/m^3.
507 In simulation 1 (constant pH), fixed hydrostatic pressure of 100 Pa is considered at the left and right
508 boundaries. In simulation 2 (variable pH), fixed hydrostatic pressure of 100 Pa is applied at the left
509 boundary *i.e.* at x = 0 and a constant CO2 gas injection rate of 1.0×10^{-9} mol/m^2/s is applied at the right

boundary (x = 0.50). The left boundary for the gas and right boundary for water are assumed impermeable in simulation 2.

5.2.2 *Parameters*

The parameters are listed in Table 3. PHREEQC database "*Phreeqc.dat*" (wwwbrr.cr.usgs.gov, 2017) is used in Simulation 2. Reaction parameters which are required for the simulation *i.e.* thermodynamic equilibrium constant (log_k) and reaction enthalpy (delta_h) are available in the database. An example of PHREEQC input data file for simulation 2 is presented in Table 4. Please note that the gas dissolution (R1.1) is calculated using PHREEQC and therefore, Henry's constant has not been mentioned explicitly.

Table 3 Parameter values for simulation 1 (constant pH) and 2 (variable pH).

Parameters	**Simulation 1**	**Simulation 2**	**Comments**
Medium and fluid flow parameters:			
Porosity, n_0	0.25		
Intrinsic permeability, $K_{int,0}$	3.98×10^{-14} m^2		Mitchell et al. (2009)
Viscosity of water, μ_l	0.9×10^{-3} Pa s		Fredlund and Rahardjo (1993)
Viscosity of the gas, μ_g	-	1.5×10^{-5} Pa s	Mitchell et al. (2009)
Gas diffusion coefficient, D_g^0	-	1.0×10^{-5} m^2/s	Fredlund and Rahardjo (1993)
Universal gas constant, R	-	8.3142 /mol	
Absolute temperature, T	-	298 K	
Biofilm Parameters:			
Substrate utilisation rate, k_+	8.01×10^{-5} s^{-1}		Beyenal et al. (2003)
Yield coefficient, Y	0.628 kg/kg		Beyenal et al. (2003)
Half-saturation constant, K_s'	26.9×10^{-3} kg/m^3		Beyenal et al. (2003)
Endogenous death rate, k_-^e	3.18×10^{-7} s^{-1}		Taylor and Jaffe (1990)
Shear loss coefficient, b_s	-	2.97×10^{-6} s^{-1}	Rittmann (1982)
Biocide decay constant, c_-^b	-	8.7×10^{-4} s^{-1}	Ebigbo et al. (2010)
Biocide decay constant, c_c	-	3	Ebigbo et al. (2010)
Biofilm density, ρ_b^s	65 kg/m^3		Peyton (1995)
Parameters for pH dependent growth:			
Growth constant, k_0^p	-	5.19×10^{-5} s^{-1}	(Tan et al., 1998)
Ionisation constant, K_1^p	-	9.15×10^{-7} mol/L	(Tan et al., 1998)
Water retention parameters:			
	-	From Table 1	

Table 4 An example of PHREEQC input data file for the simulation 2.

```
TITLE Dissolution of CO2 gas in water and pH change

SOLUTION_SPECIES
CO3-2 + 2 H+ = CO2 + H2O
      log_k          16.681
      delta_h      -5.738  kcal

PHASES
CO2(g)
      CO2 = CO2                    # dissolution of CO2 in water
      log_k          -1.468        # Gas : Liquid partitioning following Henry's law
      delta_h        -4.776 kcal   # reaction enthalpy

SOLUTION 1  Pure water             # solution definition/ composition
      -units   mol/kgw
      pH      **                   # data provided from the transport module
      C       **                   # total carbon; data provided from the transport module

GAS_PHASE 1
 -fixed_volume
CO2(g)      **                     # data provided from the transport module

End
```

5.2.3 *Results*

Development of the biofilm and change in porosity with time at the right boundary (x = 0.5) are presented in Figure 9. The simulation results show significant biofilm growth at constant pH of 7.0 (Simulation 1). In contrast limited biofilm growth is observed at this location under CO2 injection (Simulation 2). The lack of growth in simulation 2 is associated with the reduction of pH. According to Equation (12), at lower pH, ionisation state of the system becomes less suitable for the microbe to bind substrates and therefore, the growth is hindered. Figure 10 shows that injected CO2 reduces pH from initial 7.0 to 5.5 in a short span of time which retards the pH-dependent growth rate from 4.68×10^{-5} to 6.92×10^{-6} s^{-1} (inset diagram), although the substrate is abundantly available. Increasing CO2 pressure also accelerates biocide-induced death. Since CO2 gas is highly soluble in water, the gas phase pressure build up is limited and as a result, the liquid saturation at this location remains relatively high (Figure 11). The modelling capacity of the linked COMPASS-PHREEQC platform has been demonstrated via simulation 2.

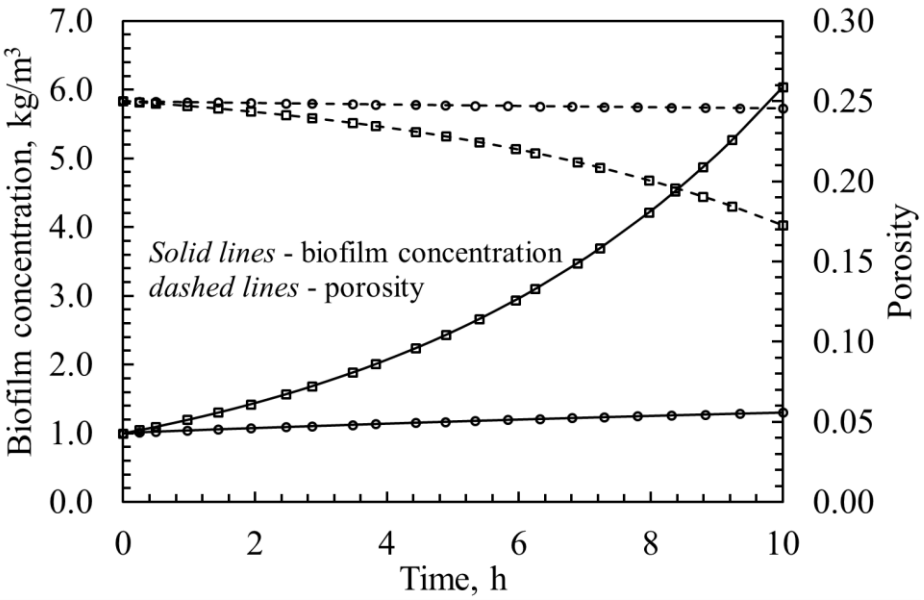

Figure 9 Biofilm growth and porosity evolution at the gas injection boundary, x =0.50. The symbol (□) represents simulation 1 *i.e.* constant pH and (○) for Simulation 2 *i.e.* variable pH. The *solid lines* represents biofilm concentration on the left vertical axis and the *dashed lines* represents porosity on the right vertical axis.

540

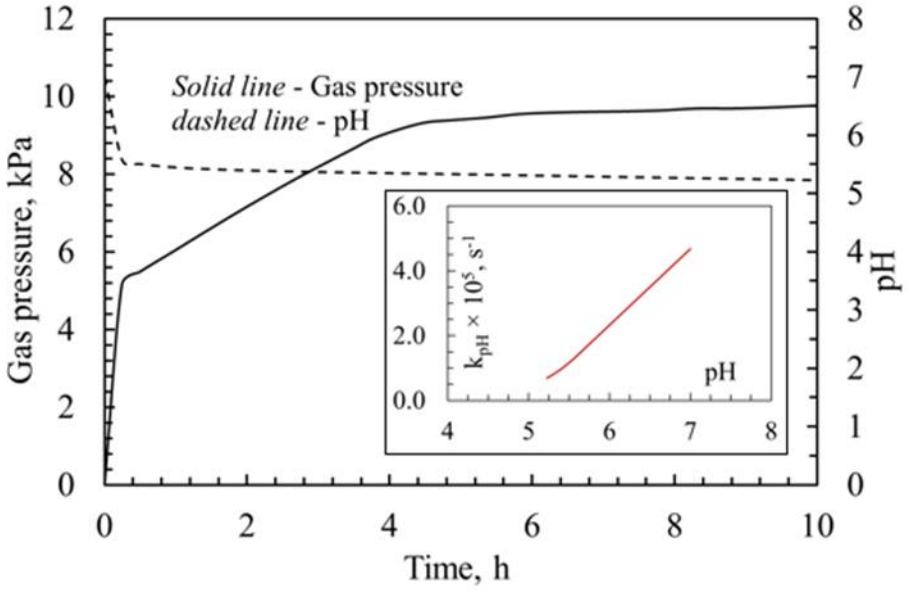

Figure 10 Evolution of CO2 pressure and pH at the gas injection boundary in Simulation 2. The *dashed line* represents pH on the right vertical axis and the *solid line* for gas pressure on the left vertical axis. The diagram inset shows the effect of pH on the growth rate, kpH, during the simulation.

541

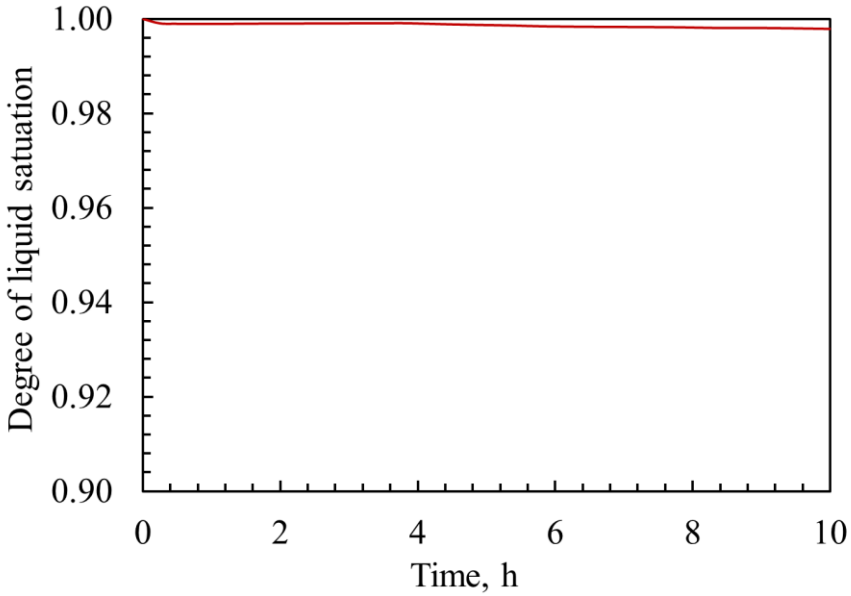

Figure 11 Change in liquid saturation with time at the gas injection boundary during simulation 2. Please note the scale of vertical axis ranges between 0.9 and 1.0.

542

543 5.3 *Microbial respiration in coupled two-phase flow condition*

544 In this simulation, the model has been applied to investigate microbial respiration under a two-phase
545 flow condition. During respiration microbes harness the energy released from a reduced species in the
546 environment to an oxidized species (Bethke, 2008). Therefore the growth is limited by both substrate
547 and an electron acceptor. It has been assumed that the microbial species does not produce any gas during
548 respiration. The simulation has been carried out for 24h.

549

550 5.3.1 *Initial and boundary conditions*

551 Initial conditions for this simulation are: porewater pressure -2.0×10^3 Pa, substrate concentration (c_d^s)
552 1.0 kg/m^3, dissolved oxygen concentration (c_d^e) 1.0 kg/m^3, gas concentration 1.0 mol/m^3, biofilm
553 concentration, 0.1 kg/m^3 and the concentration of suspended biomass, $c_b^l = 0$.
554 At the boundary, x = 0, concentrations of substrate and dissolved oxygen are fixed at 3.0 and 1.0 kg/m^3,
555 respectively. At the right boundary, x = 0.50, gas is injected at the rate of 3.0×10^{-6} mol/m^2/s and the left
556 boundary is considered impermeable for the gas. Fixed hydrostatic pressures of 1.0×10^3 and 2.0×10^2 Pa
557 are maintained at the left and right boundary, respectively.

558

559 5.3.2 *Parameters*

560 The simulation parameters are listed in Table 5.

561

562 **Table 5** Parameter values for the simulation of microbial respiration in a two-phase flow

Parameters	Values	Comments
Medium and fluid flow parameters:		
Porosity, n_0	0.25	
Intrinsic permeability, $K_{int,0}$	3.98×10^{-14} m^2	Mitchell et al. (2009)
Viscosity of water, μ_l	0.9×10^{-3} Pa s	Fredlund and Rahardjo (1993)
Viscosity of the gas, μ_g	1.5×10^{-5} Pa s	Mitchell et al. (2009)
Henry's constant	6.1×10^{-4} mol/L/atm	Sander (2015); for nitrogen gas
Gas diffusion coefficient, D_g^0	1.0×10^{-5} m^{2}s^{-1}	Fredlund and Rahardjo (1993)
Diffusion coefficient of glucose in water, $D_d^{s,0}$	6.70×10^{-10} m^{2}s^{-1}	Cussler (1997)
Diffusion coefficient of dissolved oxygen in water, $D_d^{e,0}$	2.10×10^{-9} m^{2}s^{-1}	Cussler (1997)
Longitudinal dispersion coefficient, α_L	1.0 m	Gelhar et al. (1992)
Universal gas constant, R	8.3142 J/K/mol	
Absolute temperature, T	298 K	
Biofilm Parameters:		
Substrate utilisation rate, k_+	8.05×10^{-5} s^{-1}	Beyenal et al. (2003)
Substrate yield coefficient, Y	0.628 kg/kg	Beyenal et al. (2003)
Substrate half-saturation constant, K_s'	26.9×10^{-3} kg/m^3	Beyenal et al. (2003)
Oxygen yield coefficient, F	0.635 kg/kg	Beyenal et al. (2003)
Oxygen half-saturation constant, K_e'	1.18×10^{-3} kg/m^3	Beyenal et al. (2003)
Endogenous death rate, k_-^e	3.18×10^{-7} s^{-1}	Taylor and Jaffe (1990)
Shear loss coefficient, b_s	2.97×10^{-6} s^{-1}	Rittmann (1982)
Biofilm density, ρ_b^s	65 kg/m^3	Peyton (1995)
Water retention parameters:	From Table 1	

563

564 *5.3.3 Results*

565 Evolution results of the components have been collected from three locations *i.e.* x = 0, 0.15 and 0.45
566 m of the sample (Figure 5). Figure 12a presents biofilm growth and its effects on the medium porosity.
567 The results show maximum growth at the nutrient source and away from the source it is affected by the
568 supply of nutrients as well as liquid saturation, which is influenced by the injected gas. Loss of porosity
569 continues at variable rates with biofilm growth along the sample (*i.e.* at 0.15m, porosity reduces 5.2%
570 to 0.237) but reaches the minimum, at the nutrient source, after 19h approximately. Biofilm
571 concentration and porosity profiles after 24 h are presented in Figure 13a. The results indicate that the
572 biofilm growth and porosity loss are negligible closer to the gas injection boundary. Although, at the
573 early stages of the simulation biofilm grows by utilising the available substrate and oxygen, the growth
574 is very small and un-detectable at the scale used in the y-axis. The growth period is short near this
575 boundary, since the sample de-saturates rapidly by the injected gas and it retards the flow of substrate
576 and oxygen to the microbes.

577

578 Figure 12b shows the evolution of substrate and dissolved oxygen concentrations in the sample. Initial
579 concentrations of both substrate and dissolved oxygen were 1.0 kg/m^3. However, at the boundary,

580 substrate concentration instantly reaches to the applied concentration of 3.0 kg/m^3. Along the sample
581 domain, the convective-dispersive transport of substrate and dissolved oxygen are affected by biofilm
582 growth, porosity and permeability reduction as well as gas pressure evolution. The results show that, at
583 0.15 m from the source, substrate concentration reaches to a maximum of 1.17 kg/m^3 after 1 h and
584 reduces to zero after 9 h. Meanwhile, the dissolved oxygen concentration reduces from 1.0 kg/m^3 to
585 0.18 kg/m^3 after 9 h and remains steady for the rest of the simulation. From the result of biofilm growth
586 at this location, Figure 12a, it can be noticed that after 9 h the growth suspends due to lack of substrate,
587 which consequently ceases the consumption of dissolved oxygen. Concentration profiles of the nutrients
588 (substrate and electron acceptor) are presented in Figure 13b after 5 h and 9 h of simulation. Since, the
589 elevated gas pressure de-saturates the sample, both substrate and dissolved oxygen concentrations are
590 negligible within the vicinity (note the concentration evolution of nutrients at 0.45 m in Figure 12b) of
591 the gas injection boundary. The 'hump shape' near the end of the concentration profiles (Figure 13b)
592 occurs due to simultaneous flow of nutrients driven by hydraulic gradient from one side and gas-
593 pressure driven water flow from the other side. No hump is visible for the substrate after 9 h, since all
594 of it has been used in the microbial respiration.
595
596 Evolution of gas concentration and liquid saturation is presented in Figure 12c. Since, no outflow of
597 gas has been allowed, its concentration across the sandstone sample increases rapidly from initial 1.0
598 mol/m^3 to 2.1 mol/m^3 at the onset of the simulation due to reduction of gas phase volume. The fixed
599 hydrostatic pressures at the boundaries almost saturates (>99%) the sample. However the constant
600 injection of gas increases the concentration close to the boundary and pushes the waterfront away. After
601 approximately 3 h gas pressure at 0.05 m from the injection boundary increases sharply and decreases
602 the liquid saturation (to 0.67 after 5 h). Therefore biofilm growth at this location (Figure 12a), as
603 mentioned earlier, is negligible. The gas concentration and liquid saturation profiles are presented in
604 Figure 13c. The results are plotted after 19 h simulation period when the porosity of the left boundary
605 reduces to zero *i.e.* the face becomes impermeable due to bio-clogging.
606

a)

b)

c)

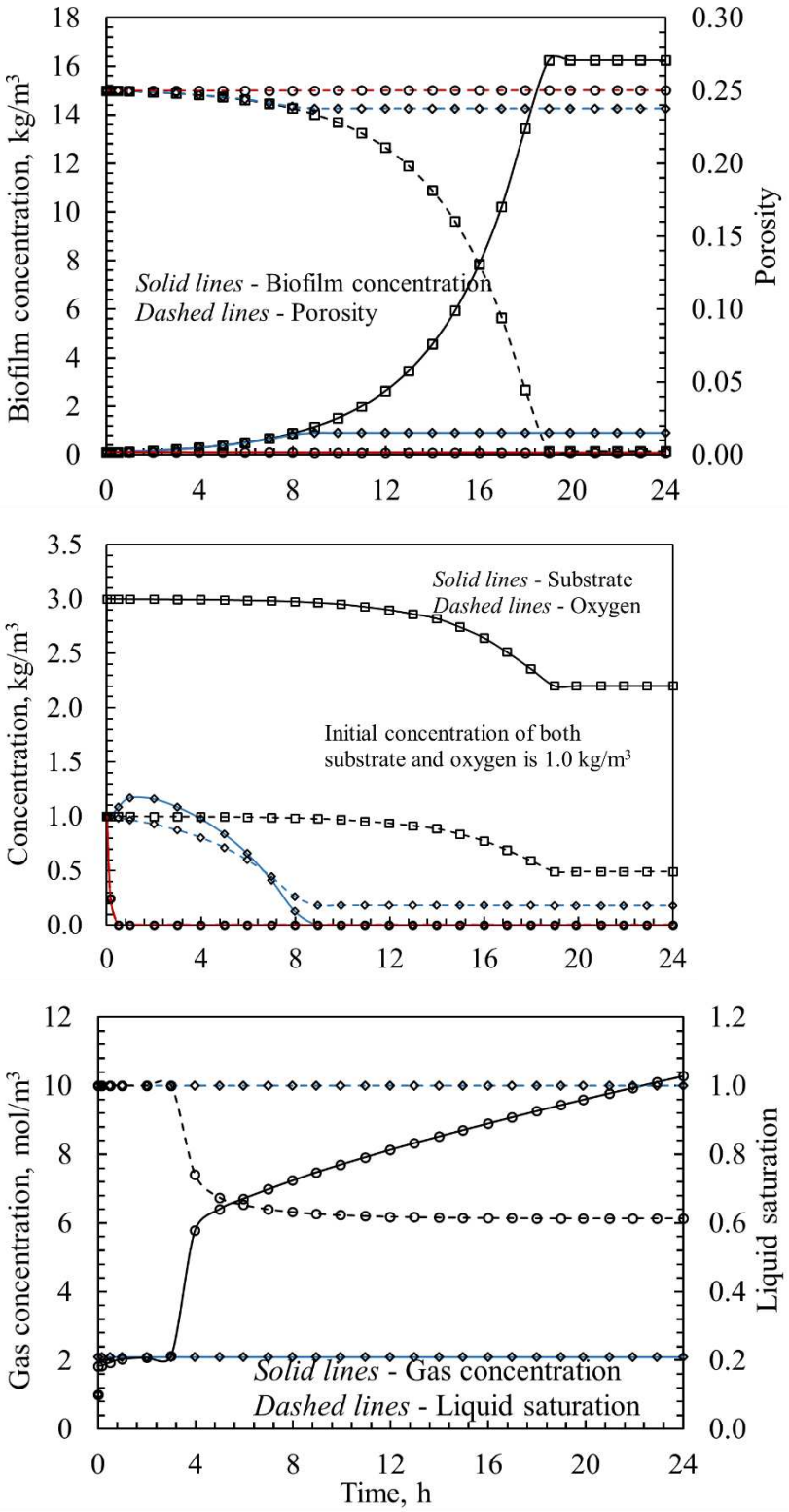

Figure 12 Evolution of a) biofilm and porosity, b) substrate and electron acceptor, c) gas concentration and liquid saturation in the sandstone sample. The symbols (□), (◊), (○) represent the results at x = 0, 0.15 and 0.45m, respectively. Please note that in c) only the results at 0.15 and 0.45m are presented.

607

608

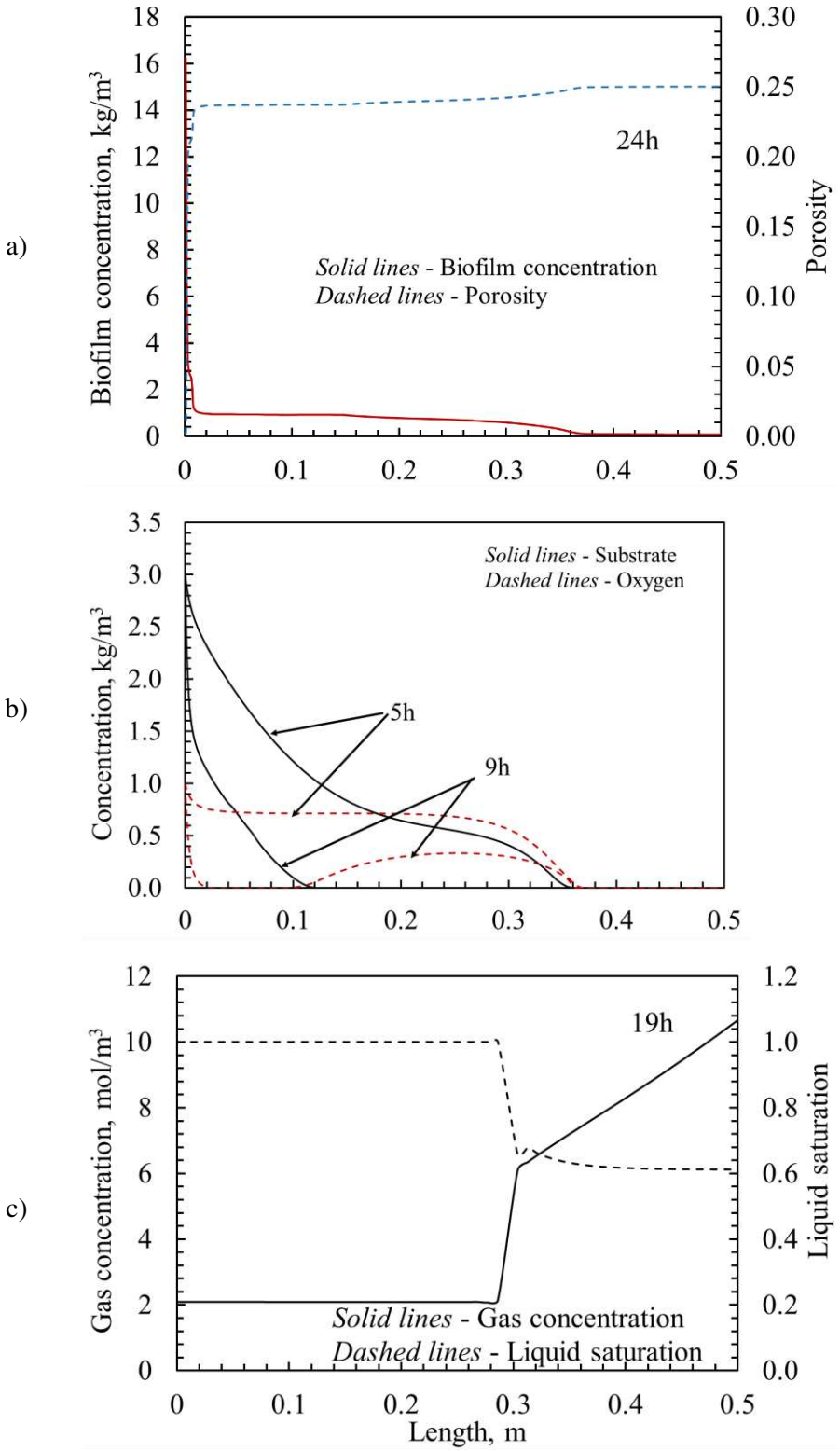

Figure 13 Profiles of a) biofilm and porosity, b) substrate and electron acceptor, c) gas concentration and liquid saturation along the length of the sandstone sample during microbial respiration under coupled flow.

609

610 *5.4 Microbial growth via fermentation and production of CO2 gas*

611 In this section, the model has been applied to predict microbial fermentation which occurs when
612 microbes metabolise substrates in absence of suitable electron acceptors in the medium. Microbial
613 fermentation of glucose substrate and the production of ethanol and CO2 gas as reaction by product is
614 considered. The overall chemical reaction:

$$C_6H_{12}O_6 \rightarrow 2C_2H_5OH + 2CO_2(g) \quad \text{(R2)}$$

615 The production of CO2 in the model is obtained from the reaction stoichiometry *i.e.* for one mole of
616 glucose metabolised two moles of CO2 gas is produced. The reaction has been modelled within the
617 COMPASS model. Therefore the geochemical model has not been used in this simulation. Since pH is
618 buffered in water-ethanol mixture and its changes are smaller, the effect of pH on microbial processes
619 has been ignored. The simulation has been carried out for 10 h.
620
621 *5.4.1 Initial and boundary conditions*

622 Initially the saturated sandstone sample contained 1.0 kg/m^3 of glucose substrate and 0.1 kg/m^3 of
623 biofilm and no gas.

624 At the left boundary, x = 0, substrate concentration is fixed at 3.0 kg/m^3. Fixed hydrostatic pressures of
625 1.0×10^3 and 2.0×10^2 Pa has been applied the left and right boundary, respectively. Boundaries are
626 considered impermeable, *i.e.* no-flow condition, for the gas.
627
628 *5.4.2 Parameters*

629 The parameters for the simulation are presented in Table 6. Henry's constant for CO2 in water at 298K
630 is 1600 atm or 3.4×10^{-2} mol/L/atm (Sander, 2015). However in water-ethanol mixture, at low ethanol
631 concentration (less than 0.1 mole fraction), Henry's constant is 2240 atm (Postigo and Katz, 1987),
632 which makes CO2 less soluble.
633
634 *5.4.3 Results*

635 The results of this simulation are presented in Figure 14 (evolution of variables at x = 0 and 0.45m) and
636 Figure 15 (profiles of varaibles). The results in Figure 14a and 15a show that biofilm concentration
637 varies from 1.44 kg/m^3 to 1.33 kg/m^3 and porosity from 0.229 to 0.231 between the two boundaries.
638 Biofilm concentration near the source of substrate is slightly higher than the opposite boundary (Figure
639 14a), which are due to the supply and availability of glucose substrate in the sample (Figure 14b). The
640 supply of substrate also influcences the concentration of CO2(g) and saturation level (Figure 14c and
641 Figure 15c). Within the vicinity of the source, elevated microbial metabolism results into little more
642 production of CO2(g) than the other end. The gas pressure continues to build up following the
643 fermentation reaction and de-saturation of the sample continues. The observed saturations (Figure 14c)
644 after 10 h at x = 0 and 0.50 m are 81.4% and 87.9%, respectively.

645

646 **Table 6** Simulation parameters for predicting microbial fermentation

Parameters	Values	Comments
Medium and fluid flow parameters:		
Porosity, n_0	0.25	
Intrinsic permeability, $K_{int,0}$	3.98×10^{-14} m^2	Mitchell et al. (2009)
Viscosity of water, μ_l	0.9×10^{-3} Pa s	Fredlund and Rahardjo (1993)
Viscosity of the gas, μ_g	1.5×10^{-5} Pa s	Mitchell et al. (2009)
Diffusion coefficient of the gas in air,	1.0×10^{-5} m^2/s	Fredlund and Rahardjo (1993)
Henry's constant, H_c	2.04×10^{-2} mol/L/atm	Calculated
Universal gas constant, R	8.3142 J/K/mol	
Absolute temperature, T	298 K	
Biofilm Parameters:		
Substrate utilisation rate, k_+	8.01×10^{-5} s^{-1}	Beyenal et al. (2003)
Yield coefficient, Y	0.628 kg/kg	Beyenal et al. (2003)
Monod half-saturation constant, K_s'	26.9×10^{-3} kg/m^3	Beyenal et al. (2003)
Endogenous death rate, k_-^e	3.18×10^{-7} s^{-1}	Taylor and Jaffe (1990)
Shear loss coefficient, b_s	2.97×10^{-6} s^{-1}	Rittmann (1982)
Biofilm density, ρ_b^s	65 kg/m^3	Peyton (1995)
Water retention parameters:	From Table 1	

647

a)

b)

c)

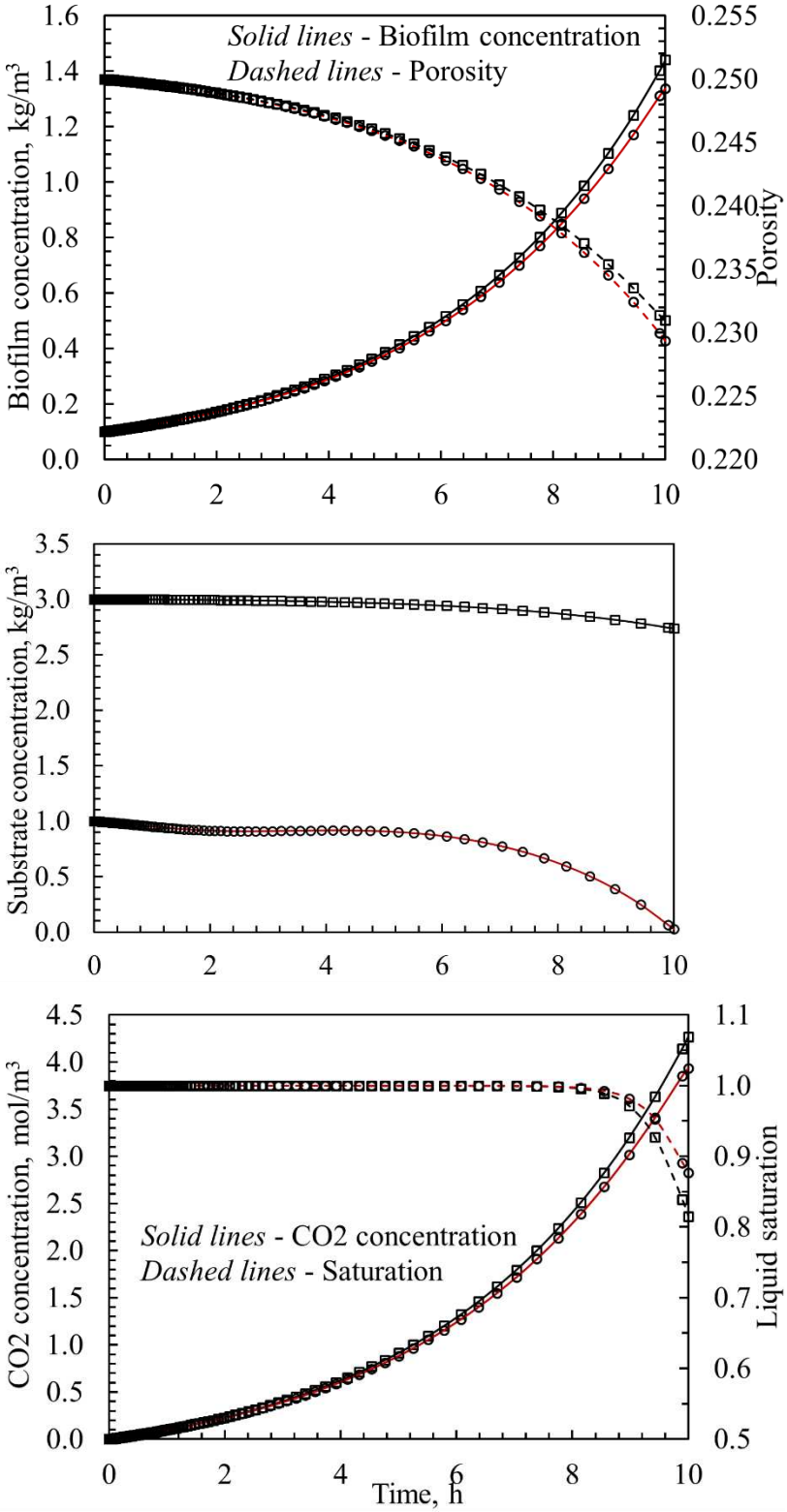

Figure 14 Evolution of a) biofilm and porosity, b) substrate, c) gas concentration and liquid saturation in the sandstone sample. The symbols (□) and (○) represent the results at x = 0 and 0.45m, respectively.

648

a)

b)

c)

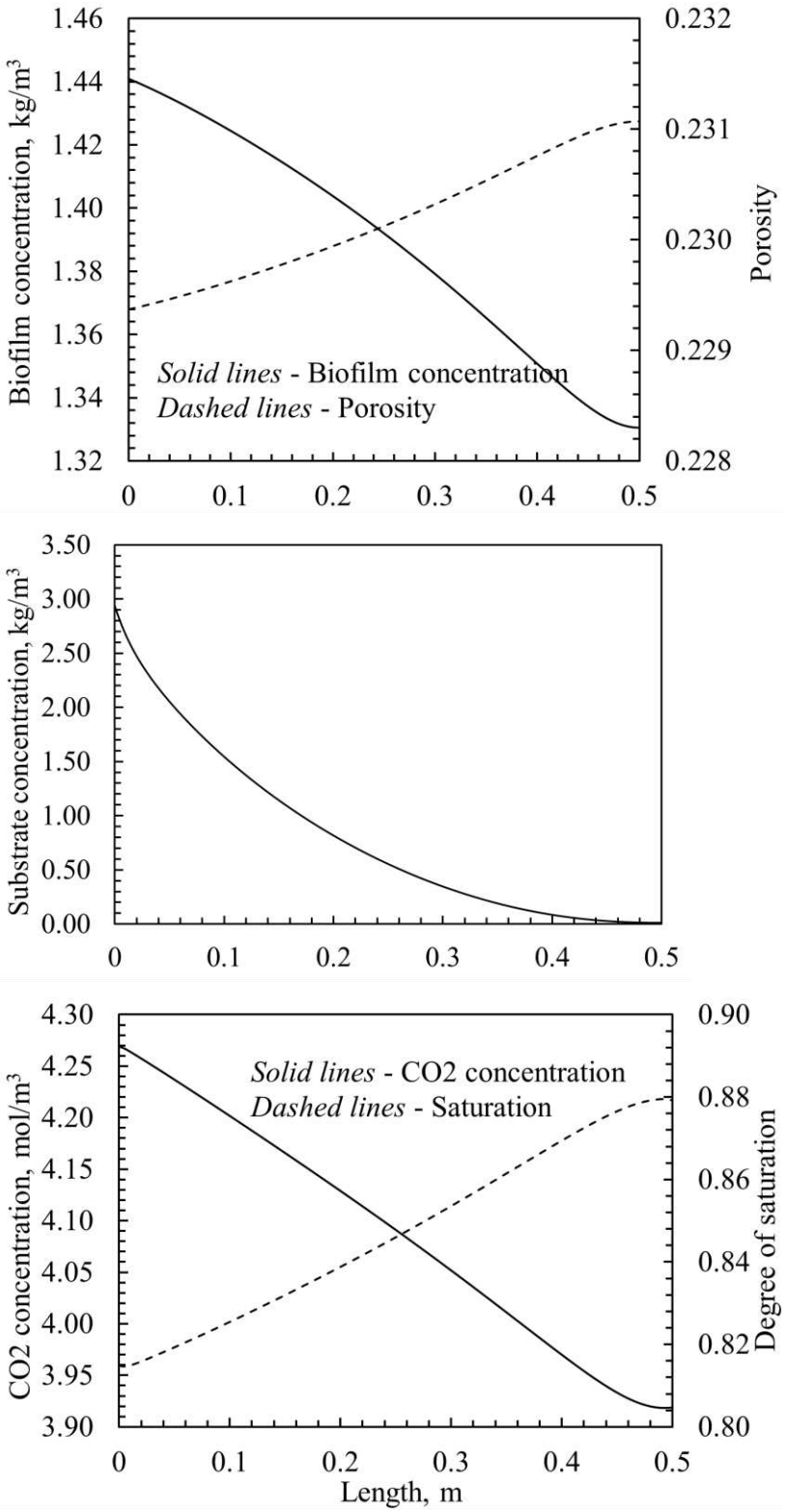

Figure 15 Profiles of a) biofilm and porosity, b) substrate, c) gas concentration and liquid saturation along the length of the sandstone sample during microbial fermentation. The profiles have been plotted after end of the simulation.

649

650 **6. Discussion and Conclusions**

In this paper, a new microbial model has been presented. Biomass transport, growth and decay processes have been included within a coupled THCM framework. The THCM model, COMPASS, solves the governing transport equations: suspended microbes in liquid phase, biofilms in solid phase, multicomponent chemicals in liquid phase, multicomponent gas phase, liquid phase, heat and mechanical deformation. The geochemical model, PHREEQC, estimates equilibrium and kinetic reactions as well as redox behavior, changes in pH etc. The linked modelling platform enables a greater range of applications involving fluids, chemicals, microbes and heat flow together with geochemical/ bio-geochemical reactions and deformation processes to be studied. In addition the multicomponent feature of the model allows inter-community and intra-community microbial interactions to be investigated.

Verification exercises demonstrated accurate implementations of the microbial processes in the model. The model has been tested against the results of a laboratory experiment obtained from the literatures. It is evident from the results that the model can predict qualitatively and quantitatively the effects of microbial activities (*i.e.* net biofilm accumulation) on porous media properties (*i.e.* porosity, permeability). Please note that the model is only partially evaluated at this stage. For full validation/ evaluation, relevant and comprehensive experimental data of microbial processes under multiphase flow and reaction conditions are essential. However such information is scarcely available in the literature.

To demonstrate the capabilities of the model, four sets of application are presented. These are; i) biofilm growth at various gas injection rates, ii) effect of pH on microbial growth, iii) microbial respiration under two-phase flow and iv) microbial fermentation and production of a gas phase. The results show that in unsaturated conditions the extent of biofilm growth largely depends on the hydraulic properties of the medium, if the growth is not limited by substrates or electron acceptors. If gas pressure is relatively large and desaturates the medium then growth is restricted to the residual water volume. Sufficient amount of liquid phase is essential for nutrient transport and biofilm development. Usage of biofilms to enhance the barrier performances of a subsurface reservoir (*i.e.* carbon storage facility) or caprocks might be less effective in such circumstances. To avoid that, media with higher water holding capacity or lower gas injection (from injection-wells) and release (of sequestrated gas from storage formations) rates; together with faster growing biofilms could be preferred. The influence of geochemical condition on biofilm growth has been modelled by varying the porewater pH (*i.e.* dissolving CO2 gas in the sandstone porewater). The results indicate that the growth is favoured by higher pH values and is significantly retarded at lower pH. The capabilities of the model to simulate microbial respiration under a coupled multiphase flow and microbial fermentation have been demonstrated. The results suggest that respiration in two-phase flow is not only influenced by substrate and oxidizer concentration but also by the gas concentration in the system. The simulated results of

688 microbial fermentation show that formation of a gas phase or change in gas phase composition can
689 affect the coupled fluid flow processes in the system.
690
691 Parameters, such as, biofilm density, attachment and detachment rates, coefficient of shear loss, bio-
692 geochemical rate parameters are (bacterial) species dependent and not widely available. In that regard,
693 laboratory experiments should be carried out to obtain appropriate model parameters as well as relevant
694 model information. For example, initial biofilm concentration is a key information for transient analysis.
695 The onset of experimental studies and numerical models of biofilm growth is usually considered after
696 the period of cell settlement and biofilm formation. The processes that take place during the settlement
697 period are of significant importance, since they dictate the initial biofilm concentration in the medium.
698 Further works will be carried out to address these issues.
699
700 Within the scope of this article, advanced capabilities of the model to study complex subsurface
701 microbial processes have been demonstrated. However, the full extent of the model could not be utilised
702 due to information limitations and/ essential simplifications. More complex and comprehensive
703 scenarios of microbial processes and chemical reactions (*i.e.* equilibrium reactions, mineral
704 precipitation/ dissolution kinetics etc.) involving wider extent of the geochemical model will be
705 presented in future publications.
706
707 **Appendix A**
708 **Table A** Nomenclature

Symbol	Definition	Units
$A, \boldsymbol{B}, \boldsymbol{C}$	Coefficient matrices	
D_b^*,D_d^*,	Hydrodynamic dispersion coefficient of suspended cells and dissolved chemicals in liquid phase	m^2/s, m^2/s
D_g^i,D_g^0	Effective, free flow diffusion coefficient of i^{th} gas species	m^2/s, m^2/s
D_d^0,D_d^i, D_d^h	Free flow chemical diffusion, effective chemical diffusion coefficient, mechanical dispersion in liquid	m^2/s, m^2/s, m^2/s
$[H^+]$	Concentration of hydrogen ion in liquid solution	mol/L
K_s',K_e'	Substrate, electron acceptor half-saturation constant	kg/m^3, kg/m^3
K_{int}, $K_{int,0}$	in-situ, original intrinsic permeability	m^2, m^2
N_g, N_d	Total number of gas, dissolved chemical components	
N_b^l, N_b^s	Total number of suspended cell, biofilm species	
P	Strain matrix	
R	Universal gas constant	J/K/mol
R_Ω	Residual error over the domain Ω	
S_l, S_g, S_r	Degree of liquid, gas, residual liquid saturation	[-],[-],[-]
S_s	Sink/source for liquid phase	kg/m^3
S_e	Effective saturation	[-]
T	Absolute temperature	°K
Y, F	Yield coefficient of substrate, electron acceptor	kg/kg, kg/kg
b_s	Detachment rate due to liquid shear stress	s^{-1}

c_b^l	Suspended cell concentration *i.e.* the amount of suspended cell in the liquid phase	kg/m^3
c_b^s	Biofilm concentration *i.e.* the amount of attached biomass/ biofilm in the whole porous media (soil)	kg/m^3
c_d^i	Concertation of the i^{th} chemical species in liquid	kg/m^3
c_d^s,c_d^e	Substrate, electron acceptor concentration in the liquid phase	kg/m^3, kg/m^3
c_g^i	Concentration of the i^{th} species in the gas phase or air	mol/m^3
c_c, c_-^b,	Biocide decay parameters	[-], s^{-1}
k_+	Substrate utilisation rate	s^{-1}
k_-, k_-^e, k_-^b	Combined, endogenous, biocide decay rate	s^{-1}, s^{-1}, s^{-1}
k_{pH}	pH dependent growth rate	s^{-1}
k_0^p, K_1^p	specific growth rate, ionisation constant	s^{-1}, mol/m^3
k_a, k_d	Rate constants for attachment, detachment of cells to, from biofilm	s^{-1}, s^{-1}
k_{rl}, k_{rg}	Liquid, gas phase relative permeability	[-],[-]
k_τ	Specific shear loss coefficient	Pa^{-1}s^{-1}
n_0, n	Initial unaffected, active porosity	[-],[-]
s_b^l	Sink/source for a suspended cell in liquid	kg/m^3
s_b^s	Sink/source for a biofilm in soil	kg/m^3
s_d^i	Sink/source for the i^{th} chemical in liquid	kg/m^3
s_g^i	Sink/source for the i^{th} gas component	mol/m^3
s, h	Suction, suction head	Pa,m
t	Time	s
u_l, u_g	Porewater, total poregas pressure	Pa, Pa
u	Displacement	m
v_l, v_g	Velocity of liquid, gas phase	m/s, m/s
α_L	Longitudinal dispersion coefficient	m
α, m, β	Curve fitting parameters of van Genuchten model	m^{-1}, [-],[-]
θ_l, θ_g, θ_b	Volumetric liquid, gas, biofilm content	m^3/m^3,m^3/m^3,m^3/m^3
μ_l, μ_g	Viscosity of liquid, gas	Pa s, Pa s
ρ_b^s	Biofilm mass density *i.e.* the amount of dry biomass per unit wet volume of the biofilm	kg/m^3
ρ_l,γ_l	Liquid density, unit weight of water	kg/m^3, N/m^3
τ	Shear stress	Pa
τ_l, τ_g	Liquid phase, gas phase tortuosity factor	[-],[-]
φ	Vector of primary/independent model variables	
∇	Gradient operator	m^{-1}

Appendix B

The mathematical relationship to define the effect of pH on microbial growth is presented in Equation (12). In Figure B, the growth rate, k_{pH} is plotted against pH for a different combination of the equation parameter (k_0^p, K_1^p) values (Table B). The parameter values in A, B, C and D are chosen arbitrarily but within the published range available in literatures.

Table B Parameter values

	k_0^p	K_1^p

A	1.0×10^{-5}	1.0×10^{-7}
B	5.0×10^{-5}	1.0×10^{-7}
C	1.0×10^{-5}	5.0×10^{-7}
D	1.0×10^{-4}	1.0×10^{-6}

The graphs show that the rate is mostly sensitive to the specific growth rate, k_0^p for the selected parameter values.

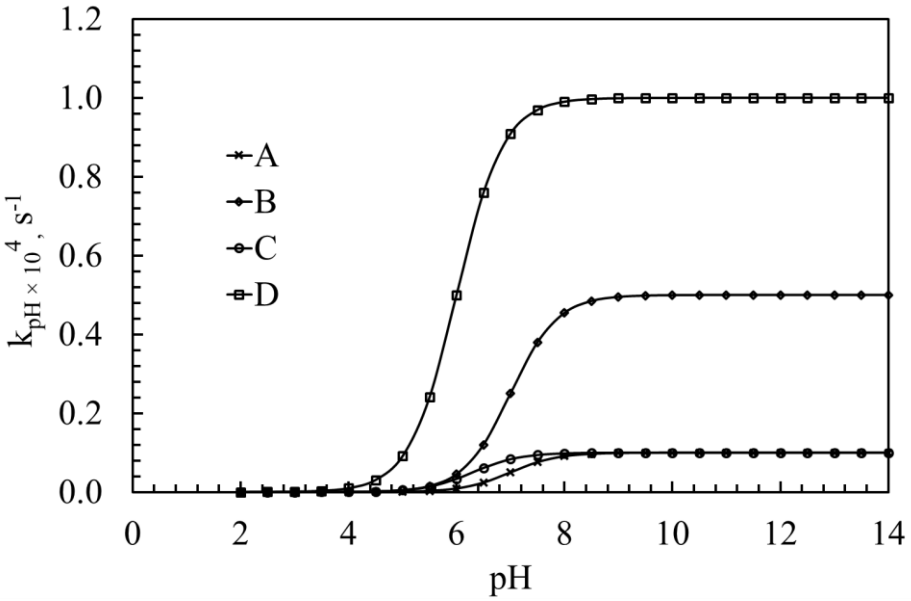

Figure B Sensitivity of the parameters on pH-dependent growth rate (k_{pH}) for various pH values.

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