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Metal-Organic-Framework Derived Co-Pd Catalyst is Preferred over Fe-Pd for Reductive Upgrading of Furfural to Tetrahydrofurfuryl alcohol

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ABSTRACT:

The function of palladium encapsulated nanohybrids with renewable platform molecules can be altered by bringing diversity in chemical compositions to step forward in bio-mass refining. In this respect we report PdCo₃O₄, PdFe₃O₄ nanoparticles encapsulated in a graphitic N-doped carbon matrix, to have a change in selectivity with superior catalytic activity for hydrogenation of biomass-derived molecule furfural (FA). Under the optimized reaction conditions, newly designed PdCo₃O₄@NC catalyst was exhibited highly efficient catalytic performance in the hydrogenation of furfural to THFAL (Tetrahydrofurfuryl alcohol) compared with PdFe₃O₄@NC, providing 100% conversion of furfural with an exclusive yield of 95% for THFAL and superior catalytic activity even up to four recycling tests. With the evidence of different characterization analysis data (XPS, H₂-TPR) of nanohybrid we can emphasise that the presence of PdCo-Nₓ active sites and the multiple synergistic effect between Co₃O₄ and Pd
(II), Co$_3$O$_4$ and Pd$^0$ as well as presence of N in the carbonaceous matrix is responsible for the superior catalytic activity and stability.

**INTRODUCTION:**

Currently, the modern world requires the sustainable production of biomass-derived chemicals such as fuels, fuel additives and value-added chemicals due to the diminishing of fossil feedstock reserves. Researchers have been focusing on finding sustainable ways to substitute fossil-derived feedstocks with residual biological matter such as crops, scrap wood, mill residuals, and other biomass resources.\(^1\) In our present study, Furfural used as raw material to produce tetrahydrofurfuryl alcohol (THFAL), which is one of the typical chemical products derived from furfural and furfuryl alcohol (FAL). THFAL completely miscible with water and used as green solvent in agricultural and industrial applications. It can also be converted into to various chemicals such as 1,5-pentanediol (1,5-PeD) an important monomer in the plastics industry, 1-pentanol (1-PeOH), tetrahydropyran (THP), tetrahydro-2-pyranone (THP-2-one), methyl tetrahydrofuran, 2-pentanol, tetrahydrofuran, 1-butanol (1-BuOH), 1,2-pentanediol\(^5\) and it is clearly pronouncing the importance of THFAL production. Salnikova et al. reported selective hydrogenation of furfural to FAL using Pd/Fe$_3$O$_4$/HPS as a catalyst, the conversion of furfural was > 95% with selectivity for furfuryl alcohol > 94%. Whereas these processes required high pressure about 6.0 MPa.\(^6\) Compared with Pd, Ru based catalysts show poor catalytic activity to hydrogenate C=C bonds in the aromatic ring of furfural.\(^7\)-\(^9\) Very recently, Rodríguez-Ramos et al. reported hydrogenation of furfural using a series of Ru-based catalysts under very mild conditions. Although conversion of furfural 93%, the selectivity toward total hydrogenation THFAL very poor.\(^8\) Nowadays, Metal-organic frameworks (MOFs) derived nanostructural materials have been received enormous attention as a novel class of porous carbon materials by providing wide-range of various structural materials, especially in heterogeneous catalysis. MOFs have also been utilized in various research fields, such as energy storage,\(^10\)-\(^12\) supercapacitors,\(^13\) gas separation,\(^14\) oxygen reduction reactions,\(^15\) CO$_2$ reduction,\(^16,17\) oxidation reactions,\(^18\) oxygen evolution reactions\(^19\) and so on. And their efficient catalytic activity is due to the modifiable particle, pore sizes, controllable shapes,\(^18\) and high specific surface areas with unique structures. Moreover, these materials are well known for developing N, P and S like hetero atom rich nanostructural carbon materials, and metal or metal oxide loaded porous carbons and N-doped porous carbons with novel
characteristics via pyrolysis process by acting as self-sacrificed template/precursor.\textsuperscript{12,20-22} Introduction of nitrogen like heteroatoms into carbon materials decreases the charge transfer resistance to improve catalytic performance by a synergistic effect\textsuperscript{20} between carbon and the heteroatom. 2-methylimidazole ligands of zeolitic imidazolate frameworks (ZIFs) are the unique source for developing carbon and nitrogen-rich (N-rich) MOFs derived porous nanostructural catalysts via direct carbonization.\textsuperscript{22,23} Pd-3d transition metal oxides@N-doped carbon type catalysts are efficient for selective and total hydrogenation of biomass-derived furfural. The selectivity of hydrogenation of furfural can be varied with 3d transition metal oxides. In the present study, Pd-Fe\textsubscript{3}O\textsubscript{4}@NC tends to hydrogenate C=O functional group over furan ring C=C bonds of furfural to produce furfuryl alcohol (FAL). FAL has been noticed as a valuable chemical compound with a wide range of applications such as foundry binders, precursors of resins.\textsuperscript{24} Additionally, FAL can be used in the production of THFAL.\textsuperscript{25} Interestingly, we noticed that the Pd-Co\textsubscript{3}O\textsubscript{4}@NC catalyst shown efficient catalytic activity towards hydrogenate furan aromatic ring C=C and C=O bonds of furfural with 100\% yield with excellent catalyst durability and much higher activity with upto 4\textsuperscript{th} catalytic run indicates the good recyclability. Overall, it is pronouncing that the Co\textsubscript{3}O\textsubscript{4} support is more effective for the total hydrogenation of furfural to produce THFAL over Fe\textsubscript{3}O\textsubscript{4} support. These Pd-Fe\textsubscript{3}O\textsubscript{4} and Pd-Co\textsubscript{3}O\textsubscript{4} decorated on porous nitrogen-doped carbon catalysts (Pd-Fe\textsubscript{3}O\textsubscript{4}@NC and Pd-Co\textsubscript{3}O\textsubscript{4}@NC) developed via direct thermal decomposition in H\textsubscript{2} flow of ZIF solid contain with an N-rich organic linker. The specific textural, chemical characteristics and atomic-level relationship between structure and catalysis of PdCo\textsubscript{3}O\textsubscript{4}@NC have been widely investigated by performing powder x-ray diffraction (P-XRD), high-resolution transmission electron microscopy (HR-TEM), scanning electron microscopy (SEM), temperature-programmed reduction (TPR), nitrogen adsorption-desorption, x-ray photoelectron spectroscopy (XPS) and Raman. On the basis of the detailed investigation with characteristic techniques, including H\textsubscript{2}TPR and XPS, the active catalytic performance and durability of Pd-Co\textsubscript{3}O\textsubscript{4}@NC towards the hydrogenation of furfural to THFAL with 95\% yield and good recyclability are can be attributed to the multipleintrinsic synergistic effect between Co\textsubscript{3}O\textsubscript{4} and Pd( I I), Co\textsubscript{3}O\textsubscript{4} and Pd\textsuperscript{0} as well as presence of N. In other words, PdCo-N\textsubscript{x} active sites in a carbonaceous matrix.

**EXPERIMENTAL:**

**Catalyst Characterization:**
Powder X-ray diffraction (PXRD) patterns of the different samples were recorded with a Bruker D8 Advance X-ray diffractometer operated at a voltage of 40 kV and a current of 40 mA using Ni-filtered Cu Kα (λ=0.15406 nm) radiation. High-resolution transmission electron microscopy (HR-TEM) images were recorded from a JEOL JEM 2010 transmission electron microscope with an operating voltage of 200 kV equipped with a field emission gun. Field emission scanning electron microscopy images of the samples were obtained using a JEOL JEM 6700 field emission scanning electron microscope (FE-SEM). Raman spectra of the samples were recorded using a LabRAM HR800 confocal microscope Raman system (HoribaJobin Yvon) with an Ar ion laser operating at 632 nm. Nitrogen sorption isotherms were measured at 77 K with an autosorbiQ automated gas sorption analyser (Quantachrome Instruments, USA). Before the measurements, the samples were degassed under vacuum at 200°C for 8 h. The Brunauer–Emmett–Teller (BET) method was utilized to determine the specific surface area using adsorption data in a relative pressure (P/P₀) range of 0.05–0.30. The total pore volumes and pore size distribution curves were obtained from the adsorption branches using the nonlocal density functional theory (NLDFT) method. X-ray photoelectron spectroscopy (XPS) was performed on aKratos Axis Ultra system using monochromatic Al Kα radiation, with a photon energy of 1486.6 eV. High resolution spectra were collected using a 20 eV pass energy, whilst survey spectra were collected at 160 eV, with step sizes of 0.1 and 1 eV respectively. The H₂-TPR analysis was carried out in a quartz micro-reactor interfaced to a gas chromatograph (GC) equipped with a thermal conductivity detector (TCD) unit. Prior to TPR analysis, the catalyst was degassed at 300°C in helium gas for 30 min and then cooled to room temperature. The helium gas was switched to 4.97% H₂ in argon with a flow rate of 30 mL min⁻¹ and the temperature was increased to 900°C at a ramping rate of 5°C min⁻¹.

Catalyst Preparation:

Synthesis of stabilizedPd nanoparticles solution:

600 mg Polyvinylpyrrolidone (PVP) was dissolved in 180 mL methanol then Palladium acetate trimmer solution (80 mg Palladium acetate trimmer dissolved in 6.2 mL H₂O) was slowly added with continuous stirring at room temperature, after that this mixture was refluxed at 70°C in air for 3 h, resulting mixture was dried using rota evaporation, obtained black solid Pd stabilized nanoparticles material was dissolved in 50 mL H₂O.

Metal-Organic-Framework derived synthesis of Pd-Fe₃O₄& Pd-Co₃O₄ nanoparticles on N-Doped Porous Carbon Sheets:
2-methylimidazole (1.312g) and PVP (0.08g) was dissolved in 100 mL methanol, then this solution was slowly added into metal nitrate solution (Co(NO$_3$)$_2$·6H$_2$O (4 mmol, 1.164g) dissolved in 100 mL methanol) with continuous stirring at room temperature, after that stabilised Pd nanoparticles solution (16 mL) was slowly dropwise added into previous solution and stirred for 45 minutes at room temperature, resulting mixture was supposed to age for 24 h, obtained solution was washed several times with methanol using centrifugation and dried in air, and then this solid material was heated at 120°C (10°C min$^{-1}$) for 1 h then 300°C (10°C min$^{-1}$) for 2 h in H$_2$ flow. The obtained solid component was assigned as Pd-Co$_3$O$_4$@NCsheets. Pd-Fe@NC was also prepared using the same synthesis process, the obtained component using Fe(NO$_3$)$_3$·9H$_2$O (Fe(NO$_3$)$_3$·9H$_2$O (4 mmol, 1.616g) dissolved in 100 mL methanol) as metal nitrate solution in the above procedure assigned as Pd-Fe$_3$O$_4$@NC.

Activity Test:

All the hydrogenation reactions of furfural were performed in a stainless-steel Parr autoclave inbuilt with a 190 pressure gauge setup lined with Teflon (50 mL), for a typical hydrogenation of furfural, 50 mL Parr autoclave was charged with a mixture of furfural (1 mmol), isopropanol (25 mL), 70 mg catalyst and the reactor was sealed with an overhead stirrer and purged four times with molecular hydrogen (H$_2$). Then the reactor was pressurized with H$_2$ (20 bar) and heated at 150°C with stirring at a speed of 700 rpm for 6 h. Then the reactor was stopped and the pressure in the autoclave was slowly released after the reactor cooled to room temperature. The solid catalyst was recovered from the reaction mixture by centrifugation and the isolated liquid reaction mixture was analyzed by chromatography (GC). GC (Shimadzu 2010) equipped contain with a flame ionization 200 detector (FID), no wax capillary column (length: 30 201 m diameter: 0.25 mm), and gas chromatography-mass spectrometry (GC-MS) (Shimadzu, 202 GCMS-QP2010S) were utilized for quantitative analysis and product detection in the presence of 1,4-dichlorobenzene as an internal standard. In the GC and GC-MS analysis, the initial column temperature of 50°C was held for 2 min, after that the temperature was programmed as 100°C with a ramp rate of 5°C m$^{-1}$ and held for 2 min, again the temperature was ramped at 10°C m$^{-1}$ until 250°C was reached and held for 2 min. in addition, the injector, detector temperatures were fixed to 250°C and 270°C, respectively.

Hot Filtration Test:

In order to confirm the heterogeneous and robust nature of our newly developed PdCo$_3$O$_4$@NC nanohybrid we have conducted a hot filtration test in a 50 mL Parr autoclave charged with a
mixture of furfural (1 mmol), isopropanol (25 mL), 70 mg catalyst and the reactor was sealed with an overhead stirrer and pressurized with H\(_2\) (20 bar) and heated at 150°C with stirring at a speed of 700 rpm for 2 h. After reaction proceeded for 2 h, the catalyst was isolated from the hot reaction mixture by centrifugation and sample prepared from filtrate for GC analysis, 100% furfural conversion with 75% yield was noticed over PdCo\(_3\)O\(_4\)@NC, then we have performed same catalytic reaction at identical reaction conditions with collected filtrate for an additional 6 h, and no considerable hydrogenation of filtrate was noticed by GC analysis indicating that there is no leaching of nanoparticles due to nanoparticles strongly anchored with N-doped carbon matrix pronouncing the robust nature of PdCo\(_3\)O\(_4\)@NC.

RESULTS AND DISCUSSION:

The successful development of robust hollow structured PdCo\(_3\)O\(_4\)@NC nanohybrid was achieved in a systematic and easy catalyst preparation strategy as illustrated in Scheme 1. Initially, PVP-Pd@ZIF-67 composite was developed by consuming 2-methylimidazole as a self-sacrificed template, Co(NO\(_3\))\(_2\).6H\(_2\)O and Palladium acetate trimer involved as a metal source at room temperature, in the overall synthesis process PVP served as a stabilizer in Pd nanoparticle synthesis and developing nanocomposite. The deep washing of prepared composite with methanol removes the molecules loosely adsorbed on PVP-Pd@ZIF-67 composite through electrostatic interactions. The characteristic FE-SEM of the solid nanocomposite of PVP-Pd@ZIF-67 shown in Figure S1 ESI. As final step solid PVP-Pd@ZIF-67 was pyrolyzed under the molecular hydrogen gas flow at pre-programed-temperature (120°C, 10°C min\(^{-1}\) than 300°C, 10°C min\(^{-1}\)) to obtain Pd-Co\(_3\)O\(_4\) encapsulate in graphitic N-doped carbon matrix denoted as PdCo\(_3\)O\(_4\)@NC. During the decomposition of nanocomposite, the organic ligands from the ZIF are condensed to form nitrogen doped porous carbon matrix, on other side the formation of Co\(_3\)O\(_4\) begins as raising temperature to 300°C from Co\(^{2+}\) which further interact with Pd to produce Pd-Co\(_3\)O\(_4\), which were in situ confined into N-doped carbon matrix, leading to homogeneous dispersion of the Pd-Co\(_3\)O\(_4\) on carbon matrix with controlled generation of highly catalytically PdCo-N\(_x\) active sites with an effective approach for graphitization of amorphous carbon by solid-state transformation method.
Scheme 1: Schematic illustration for metal-organic-framework mediated synthesis of Pd-Fe₃O₄ & Pd-Co₃O₄ nanoparticles on N-doped porous carbon sheets

The formation of Co₃O₄ and Fe₃O₄ confirmed by the X-ray diffraction analysis of the prepared samples, the X-ray diffractograms were scanned between wide angles of 5-80° (2θ). Pd-Fe₃O₄@NC sample exhibited six peaks, the absence of other phases of iron oxide, characteristic for the magnetic cubic structure of Fe₃O₄ (Figure 1) phase at 2θ values of 30.3°, 35.7°, 43.3°, 54.1°, 57.4° and 62.9° (JCPDS 19-0629) with the corresponding diffraction planes of (220), (311), (400), (422), (511) and (440). There is no noticeable Pd (0) diffraction peak for both Pd-Fe₃O₄@NC and Pd-Co₃O₄@NC indicative of finely dispersed Pd (0) and its existence confirmed by XPS analysis (figure 4) and H₂-TPR (figure 3). Pd-Co₃O₄@NC exhibited characteristic peaks of Co₃O₄ phase at 2θ values of 36.6° and 44.5° (JCPDS-ICDD 9-418) with the corresponding to the (311) and (400) diffraction planes indicating the successful formation of high crystalline quality metal oxide (Co₃O₄) (Figure 2). Surface properties of catalysts could be determined using Nitrogen adsorption-desorption isotherm. The obtained isotherm of both PdFe₃O₄@NC and PdCo₃O₄@NC catalysts are corresponding to a type (II) with H3 hysteresis in the Brunauer classification confirms the existence of inter-particle void spaces, and it does not show any limiting adsorption at high relative pressures (P/P₀). The Brunauer-Emmett-Teller surface area (S_BET) for Pd-Fe₃O₄@NC and Pd-Co₃O₄@NC was found to be 60.96m²/g and 109.07m²/g, respectively. The pore size distribution of PdCo₃O₄@NC was measured to be 1.70nm, which further confirms its microporous nanostructure. Interestingly, a comparable pore size distribution centered at 1.70 for PdFe₃O₄@NC due to similar dense
nanoparticles serves as templates to generate microporous N-doped carbon nanostructure in both catalysts, and the additional pores, which are formed from uncontrolled aggregated nanoparticles of Fe-ZIFs thermal treatment in H₂ flow, were noticed from PdFe₃O₄@NC as well. (Figures S2, S3, ESI).

Figure 1: Wide angle power XRD patterns (a) and (b), N₂ adsorption/desorption isotherms (c) and (d), of Pd-Co₃O₄@NC and Pd-Fe₃O₄@NC, respectively.

Nanostructures, Particle size and morphology of Pd-Fe₃O₄@NC and Pd-Co₃O₄@NC composites evidently studied by high-resolution transmission electron microscopy (HR-TEM), transmission electron microscopy (TEM) and scanning electron microscopy (SEM) analytical techniques. The morphology of Pd-Fe₃O₄@NC and Pd-Co₃O₄@NC is clearly categorized by the FE-SEM images (Figure S5 ESI). As presented in Figure S5b ESI, The closely packed Pd-Fe₃O₄ nanoparticles decorated on N-doped carbon flake type sheets, which could also be clearly seen from TEM images that well-defined and homogenous spherical shape of nanoparticles. But in the case of the Pd-Co₃O₄@NC compound consistency of closely packed spherical shape of particles very clearly noticed from SEM images (Figure S5a ESI). Actually, Pd-Fe₃O₄ nanoparticles tend to form aggregates due to high surface energy, and high surface interaction.
between the nanoparticles and large specific surface area. In the TEM images (Figure 2), uniformly distributed darker spots of spherical metal oxides nanoparticles surrounded by lighter regions of n-doped carbon matrix in Pd-Fe₃O₄@NC and Pd-Co₃O₄@NC are developed by aggregation process of metal oxides nanoparticles with an average size range of 11.9-21.8 (Fe₃O₄) and 20-40 nm (Co₃O₄). As shown in Figure 2b & 2d, HR-TEM images along with the corresponding Elemental mapping data are clearly representing the hollow metal oxide (Co₃O₄, Fe₃O₄) polycrystals, the distinguished crystalline lattice spacing about 0.30nm attributed to (220) diffraction planes omitted from crystallographic planes of the inverse spinel Fe₃O₄ nanoparticles. Parallel fringes having d-spacing of ~0.204 and 0.248nm, respectively are corresponding to the (400) and (311) diffraction planes of the normal spinel Co₃O₄ nanoparticles which is similar to powder XRD crystalline reflections. Moreover, the corresponding high angle annular dark field scanning transmission electron microscopy Elemental mapping data of nanohybrids further confirmed the homogeneous distribution of elements O, C, Pd and Co of Pd-Co₃O₄@NC, and O, N, C, Pd and Fe of Pd-Fe₃O₄@NC on the catalyst surface, respectively.

**Figure 2:** HR-TEM images (a & b) of Pd-Co₃O₄@NC, (c & d) of Pd-Fe₃O₄@NC, respectively with corresponding Elemental mapping data.
As shown in Figure 3, the H$_2$-TPR of Pd-Fe$_3$O$_4$@NC and Pd-Co$_3$O$_4$@NC is indicating the successful loading of palladium, and the formation of Fe$_3$O$_4$ and Co$_3$O$_4$, respectively. The H$_2$-TPR of Pd-Fe$_3$O$_4$@NC exhibited a peak about 120-207 cm$^{-1}$ corresponding to the reduction of Pd-O to Pd, and a broad peak appeared at 470-840 cm$^{-1}$ is due to overlapping of Fe$_3$O$_4$ to FeO peak at 420-660 cm$^{-1}$ and FeO to Fe peak at 660-850 cm$^{-1}$ revealing the consistency of Fe$_3$O$_4$ phase.$^{[28]}$ Usually, the discrepancy in chemical states of Pd nanoparticles directs to deferent redox properties. The Pd-Co$_3$O$_4$@NC exhibited a broad reduction peak of Pd(II) to Pd at 104-315 cm$^{-1}$ with slow uptake by consuming H$_2$ continuously is due to inhibition of in-situ formation of PdO via lowering the reduction temperature of Pd-O to Pd by Co$_3$O$_4$. Interestingly, Pd(II) reduction temperature shifted towards higher temperature indicating the stabilization of Pd(II) due to the formation of Pd-O-Co bond between Pd(II) and Co$_3$O$_4$.$^{[29]}$ and it is pronouncing that the existence of electronic interaction between Pd and Co. The broad peak and a small peak at 299-600 cm$^{-1}$ is due to two-step reduction process of Co$_3$O$_4$, the first peak is due to Co$_3$O$_4$ to CoO reduction and the second peak is due to the subsequent reduction of CoO to Co.

![Figure 3: H$_2$-TPR profiles of Pd-Co$_3$O$_4$@NC & Pd-Fe$_3$O$_4$@NC, respectively.](image)

The electronic structure and chemical state of Pd nanoparticles in Pd-Co$_3$O$_4$@NC and Pd-Fe$_3$O$_4$@NC catalysts, and surface electronic property and elemental compositions were evidently identified by XPS investigation of Pd-3d, Co-2p, Fe-2p and N1s of Pd-Co$_3$O$_4$@NC.
and Pd-Fe$_3$O$_4$@NC (Figure 4) at their corresponding binding energies. The N-1s XPS spectrum of Pd-Co$_3$O$_4$@NC exhibited a broad peak which could be resolved in to two components attributed to pyridinic N at 399.1 eV and graphitic N at 400.4 eV. The pyridinic N peak resulted from Pd-Co$_3$O$_4$@NC shifted towards the high binding energy about \(\sim 0.3\) eV compared with Pd-Fe$_3$O$_4$@NC revealing that the pyridinic N (Lewis base) strong interactions with Co$_3$O$_4$ confirming the successful formation of the N-doped carbon matrix and it is well known that the synergistic effect between Pd and N play additional role in enhancing the catalytic activity$^{[30,31]}$ whereas, in Pd-Fe$_3$O$_4$@NC the N-1s binding energy of pyridinic N located at 398.8 eV (Figure 4d). As shown in Figure 4a, the Pd-3d XPS spectra of PdCo$_3$O$_4$@NC exhibited a sharp doublet with the 3d$_{5/2}$ peak centred at 335.3 eV w corresponding to Pd$^0$ (Figure 4a). Interactions between Pd$^0$ and Co$_3$O$_4$ can be attributed to intrinsic synergistic effect developed by charge transfer of electrons between Pd and Co$^{30}$ and shown enhanced activity in the hydrogenation of furfural, and one more doublet with a Pd5/2 peak at 338.0 eV corresponding to Pd(II) which connected with Co$_3$O$_4$.$^{[32]}$ Moreover, we also identified that the electronic structural properties of Co$_3$O$_4$ in PdCo$_3$O$_4$@NC nanohybrid is quite similar to those investigated by Xihong Lu et al. The investigation of Co-2p XPS spectra at binding energy of 779.6 eV revealing (Figure 4c) that as lattice oxygen atoms containing Co$_3$O$_4$ (O 1s, Figure S4 ESI) interacting with Pd(II) nanoparticles the Lewis acidic nature of Co$_3$O$_4$ enhances due to synergistic effect between Co$_3$O$_4$ and Pd(II) by electron transport from Co$_3$O$_4$ to Pd(II), and it pay a key role in favoring the interactions between carbonyl group of furfural with Co$_3$O$_4$ to succeed coordination bond as well in hydrogenation process in presence of Pd$^0$ via hydrogen dissociation and spillover on Co oxide encapsulated in graphitic N-doped carbon matrix.$^{[33,34]}$ In the case of the Pd-Fe$_3$O$_4$@NC catalyst Pd-3d XPS spectra exhibited metallic Pd as indicated by the 3d5/2 signal at, 334.9 eV this bulk like value suggests that either the particles are bigger, exhibiting more bulk like properties, or there is little considerable interactions between Pd and Fe$_3$O$_4$ lowers the charge transport between the Pd and Fe$_3$O$_4$ which can be suppress the capability of ring hydrogenation of furfural and the second one at lower binding energies compare with Pd-Co$_3$O$_4$, binding energy of 337.2eV indicating the existence of Pd(II). The Fe 2p XPS spectra indicates no other iron oxides are present, with the Fe2p$_{3/2}$ peak at 710 (Fe 2p3/2), along with satellite peaks can attributed to the magnetite (Fe$_3$O$_4$) (Figure 4b).$^{[35]}$
**XPS: Figure 4:** Fitted Pd-3d (a), Fe-2p (b), Co-2p (c), N-1s (d), XP spectra of Pd-Fe$_3$O$_4$@NC & Pd-Co$_3$O$_4$@NC, respectively.

In addition to powder XRD the formation of Co$_3$O$_4$ and Fe$_3$O$_4$ phases is confirmed by the Raman spectroscopy analysis of untainted Pd-Fe$_3$O$_4$@NC and Pd-Co$_3$O$_4$@NC catalysts. The Raman spectra of Pd-Fe$_3$O$_4$@NC exhibited one broadband around 660 cm$^{-1}$ corresponding to A$_{1g}$ mode and two broadbands around 1359 and 1583 cm$^{-1}$ are attributed to the vibration modes of Fe$_3$O$_4$ phase and hematite, respectively.\textsuperscript{[36,37]} As space group theory predicts $\Gamma$=A$_{1g}$ + E$_g$ +
3F2g vibration modes are Raman active modes as “Fd3m” symmetry for the Co3O4 normal spinel configuration, the Pd- Co3O4@NC nanoparticles exhibited five characteristic bands around 197, 484, 524, 621 and 690 cm⁻¹ can be attributed to Raman active F2g, Eg, 2F2g and A1g vibration modes of normal spinel Co3O4 phase, respectively (Figure 5). Out of five Raman active vibrational modes, the F2g (197 cm⁻¹) vibration mode corresponding to CoO6 scissoring vibration mode, whereas Eg (484 cm⁻¹), 2F2g (524, 621 cm⁻¹) and A1g (690 cm⁻¹) are exhibit Co-O symmetric stretching vibration.[38-40]

![Raman spectra](image)

**Figure 5:** Raman spectra of Pd-Co3O4@NC (a) & Pd-Fe3O4@NC (b), respectively.

**Catalytic activity for reductive upgrading of bio-mass derived furfural:**

To evaluate the catalytic activity of the as-synthesized PdCo3O4@NC we have conducted Hydrogenation of furfural. During the course of the reaction, we have noticed the formation of the verity of products from furfural over the PdFe3O4@NC and PdCo3O4@NC catalyst (Scheme S1 ESI). The formation of THFAL from furfural involves two subsequent steps. hydrogenating furan aromatic ring C=C is hard compared with C=O bonds of furfural as presented in plausible mechanism Scheme S1 ESI, in the first step furfural interact with a catalyst to produce furfuryl alcohol (FAL), subsequently, second step initiate to hydrogenate furon ring of furfuryl alcohol to yield desired THFAL. Further THFAL interaction with metal involves in hydrogenolysis process to yield MeTHF which is a by-product of furfural hydrogenation using PdFe3O4@NC and PdCo3O4@NC as a catalyst. Our catalytic study experiments evidently proved the plausible mechanism. The beginning of catalytic activity study is the comparison, and the effect of reaction time, temperature and pressure on the catalytic activity of PdFe3O4@NCand PdCo3O4@NC (Figure 6). As shown in Figure 6b in
presence of PdFe₃O₄@NC, at initial 1 h time period the product yield of THFAL, FAL noticed as 28% and 71%, respectively along with the formation of side products (MeTHF, 2-Methylfuron) with 100% conversion. Herein we noticed that the THFAL yield further enhanced to 70% by hydrogenating FAL to THFAL as expanded the time period to 8 h at identical 20 bar H₂, 150°C. Interestingly, the PdCo₃O₄@NC nanohybrid was exhibited complete conversion of furfural with the 60% yield of THFAL and 33% yield of FAL at reaction time period for 1 h. As increasing the reaction time period 1 h to 8 h during the optimization of reaction time at fixed H₂ pressure (25 bar) and temperature (150°C) gradual increase in the product yield of THFAL with the maximum of 95% up to 6 h noticed which indicating that the active sites are initially engaged in interacting with furfural carbonyl group Pd(II) in presence of Pd⁰ to yield FAL which subsequently undergoes to produce THFAL due to the total hydrogenation of furfural to THFAL proceeds via hydrogenating C=O and furan aromatic ring C=C bonds of furfural, respectively, the C=O bond is less stable and easy to hydrogenate than furan aromatic ring C=C bonds (Scheme S2 ESI)⁴¹,⁴² and the further extension of time period to 8 h declined the THFAL yield to 88% which can be ascribed to the hydrodeoxygenation of THFAL into undesired side product methyl tetrahydrofuran (MeTHF) in presence of PdCo₃O₄@NC with the complete conversion as well (Figure 6a).
Figure 6: Evolution of reactant and product distributions as a function of time over (a) PdCo$_3$O$_4$@NC, (b) PdFe$_3$O$_4$@NC. Reaction conditions: furfural (1 mmol), isopropanol (25 mL), 70 mg catalyst, H$_2$ (20 bar), 150°C.

A similar scenario has been identified while investigating temperature and pressure influence on the catalytic activity of both catalysts, the desired product yield of THFAL and the side products yield affected as well. As the temperature increase 90 to 200°C at the fixed H$_2$ pressure of 20 bar, the maximum product yield of THFAL with 95% achieved at 150°C for PdCo$_3$O$_4$@NC and quite dissimilar from PdFe$_3$O$_4$@NC further increase of temperature from this point the continuous decline in product yield of THFAL observed on another side MeTHF percentage of yield gradually increased to 41% via hydrodeoxygenation process at high temperature (220°C) (Figure 7c). High product yield (88%) of FAL has been noticed in presence of PdFe$_3$O$_4$@NC at lower temperatures (90°C), and as raising the temperature from lower to higher (200°C) the yield of THFAL reached 65%, further involved in the
hydrogenolysis process to yield MeTHF at 220°C (Figure 7d). Eventually, after an investigation of temperature effect on the catalytic activity of catalysts, the pressure influence of H₂ pressure ranging from 15-30 bar has been examined. With increasing the H₂ pressure from 15-25 bar, the required abundance of dissolved H₂ in the reaction mixture was achieved at 25 bar and obtained the huge yield of THFAL with 95% at 150°C and 6 h reaction time period for PdCo₃O₄@NC (Figure 7a). In presence of PdFe₃O₄@NC furfural converted into FAL with 71% product yield at an initial H₂ pressure of 15 bar and the maximum yield of THFAL noticed at 30 bar due to further hydrogenation of FAL at high pressure (H₂ 30 bar) (Figure 7b).

![Graphs showing influence of H₂ pressure and temperature on PdCo₃O₄@NC & PdFe₃O₄@NC](image)

**Figure 7:** Influence of H₂ pressure (a & b) & temperature (c & d) on PdCo₃O₄@NC & PdFe₃O₄@NC, respectively. Reaction conditions: furfural (1 mmol), isopropanol (25 mL), 70 mg catalyst, H₂ (20 bar), 6 h.

In order to evaluate the superior catalytic activity of PdCo₃O₄@NC towards the hydrogenation of furfural to THFAL, we have compared reported Pd-Based Catalysts catalytic activity for conversion of furfural to THFAL (Table S1 ESI), additionally, we have developed a series of catalysts including CuFe@NC, CuCo@NC, Co@NC and Fe@NC by following a similar
synthesis procedure involved in the development of PdCo$_3$O$_4$@NC nanohybrid. From the comparison study as depicted in Figure 8 we have achieved 100%, 100%, 38%, 23% furfural conversion from CuFe@NC, CuCo@NC, Co@NC and Fe@NC, respectively, at optimized reaction conditions. Especially the yields of THFAL from furfural for corresponding catalysts are noticed as very low compared with PdCo$_3$O$_4$@NC. Fe@NC, Co@NC provided much lower yields of THFAL 3% and 12%, respectively. CuFe@NC and CuCo@NC catalysts exhibited improved catalytic activity and the yields of THFA are 27% and 42%, respectively, with complete conversion of furfural Which conclude that the Cu promoted Co/Fe and Co/Fe are less active in N-doped carbon matrix to achieve desired product THFAL suggesting the importance of enhanced Lewis acidic nature of Co$_3$O$_4$ by synergistic effect between Co$_3$O$_4$ and Pd(II) in PdCo-N, active sites to achieve the interactions between carbonyl group of furfural with metal oxide in hydrogenation process of furfural. But in the case of PdFe$_3$O$_4$@NC exhibited considerably good yields at first reaction run (45%, 6 h) although which is unstable indicating the impact of Pd$^0$ in achieving enhanced THFAL yields. As a final step in the comparison study, we have conducted the hydrogenation reaction of furfural in inert conditions too for PdCo$_3$O$_4$@NC and PdFe$_3$O$_4$@NC, and the resulted yields of THFA are 35% and 45%, respectively (Figure 8). However, from comparison investigation conclude that the PdCo$_3$O$_4$@NC nanohybrid exhibited superior catalytic activity with exclusive yields of THFA (95%) (Figure 6a).

Figure 8: Reaction conditions: furfural (1 mmol), isopropanol (25 mL), 70 mg catalyst, H$_2$ (20 bar), 6 h for CuFe@NC, CuCo@NC, Co@NC and Fe@NC, furfural (1 mmol), isopropanol (25 mL), 70 mg catalyst, inert atmosphere, 6 h for PdCo@NC and PdFe@NC.
In order to affirm the stability of catalyst, we have done XPS analysis at 3d-Pd region of used catalysts along with reusability test as well. Interestingly, we noticed that the PdCo$_3$O$_4$@NC nanohybrid exhibited a sharp doublet with high intensity similar with fresh catalyst at the binding energy of ~340.5 and ~335.4 eV corresponding to the Pd$^0$ interacted with Co$_3$O$_4$ further confirming the negligible leaching of Pd and the robust nature of Pd-Co$_3$O$_4$@NC nanohybrid, additionally, these results well consistent with the hot filtration test. Whereas Pd-3d XPS spectra of PdFe$_3$O$_4$@NC (Figure 10a) very clearly indicating the huge amount of leaching of Pd from the catalyst due to the existence of Pd in the form of bulk Pd(0) (3d$_{3/2}$ = 40.2 eV; 3d$_{5/2}$ = 334.9 eV) which is loosely binded on Fe$_3$O$_4$@NC surface with less interactions between Pd and Fe$_3$O$_4$ diminishes the stability of catalyst. The Fe 2p XPS spectra peaks of used catalyst noticed at the binding energies about 710.3 (Fe 2p3/2), 724.152 (Fe 2p1/2) along with satellite peaks (Figure S6 ESI), and identical with fresh catalyst Fe 2p XPS spectra. Moreover, the elemental surface composition of carbon noticed as 55.36 and 59.02 mol % for used PdCo$_3$O$_4$@NC and PdFe$_3$O$_4$@NC catalysts, respectively, indicating that there is more amount of carbon deposited on the surface of the used PdFe$_3$O$_4$@NC catalyst compared to the used PdCo$_3$O$_4$@NC catalyst, and very poor signal detection noticed from used PdFe$_3$O$_4$@NC catalyst. The obtained result from XPS analysis of fresh and used catalysts suggested that the stability of active PdCo$_3$O$_4$@NC nanohybrid improved which could be ascribed to the strong synergistic effect between Pd and Co$_3$O$_4$ compared with Pd and Fe$_3$O$_4$. Moreover, we have noticed good results from reusability test up to fourth reaction run (Figure 10b) which furtherly confirmed the robust nature of PdCo$_3$O$_4$@NC nanohybrid. After isolation of PdCo$_3$O$_4$@NC nanohybrid by centrifugation followed by washed with the methanol and oven dried at 80ºC from the first run reaction mixture we have conducted four more reaction runs at optimized reaction conditions and the yields of THFAL from furfural obtained as 94, 92, 89 and 85% for second, third, fourth and fifth run, respectively, with complete conversion, and this negligible decline in the yield of THFAL can be attributed to minimal carbon deposition on the surface of the active sites which may furtherly lead to the minimized porosity of nanohybrid. [43,44]
CONCLUSIONS:

In summary, present study describes the facile strategy to development of PdCo$_3$O$_4$ nanoparticles encapsulated in graphitic N-doped carbon matrix (PdCo$_3$O$_4$@NC), via stabilized Pd nanoparticle (PVP-Pd) deposited on the ZIFs metal-organic framework (PVP-Pd@ZIF-67) subsequently pyrolyzed in molecular hydrogen gas, for deep insight into investigation and comparison with PdFe$_3$O$_4$@NC synergetic effects on catalytic activity. In particular, PdCo$_3$O$_4$@NC nanohybrid with a composition of PdFe$_3$O$_4$@NC exhibited superior catalytic activity toward the conversion of furfural 100% with an exclusive yield 95% for hydrogenation product THFAL (Tetrahydrofurfuryl alcohol). The characterization techniques including XPS (fresh and used catalysts), H$_2$-TPR studies experimentally evidenced that the presence of PdCo-N$_x$ active sites and the multiple synergistic effects are responsible for the superior catalytic activity and stability of PdCo$_3$O$_4$@NC nanohybrid.

ASSOCIATED CONTENT

†Electronic supplementary information (ESI) available: Characterization techniques, Pore-size distribution, FE-SEM images & O-1s XPS spectra of PdCo$_3$O$_4$@NC and PdFe$_3$O$_4$@NC, FE-SEM images of PVP-Pd@ZIF-67 and Proposed mechanistic pathway for catalytic hydrogenation of furfural to THFAL.
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Notes

The authors declare no competing financial interest

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Graphical Abstract:

**Metal-Orga**n-Framework Derived Co-Pd Catalyst is Preferred over Fe-Pd for Reductive Upgrading of Furfural to Tetrahydrofurfuryl alcohol

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