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Experimental and theoretical insights into  
borohydride-based reduction induced metal  
interdiffusion in Fe-oxide@NiCo<sub>2</sub>O<sub>4</sub>  
for enhanced oxygen evolution

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**KEYWORDS:** Bi-layered  $\text{Fe}_3\text{O}_4/\text{NiCo}_2\text{O}_4$ , chemical reduction, metal-interdiffusion, electrocatalytic water-splitting, oxygen evolution reaction (OER)

**ABSTRACT:** Oxygen evolution reaction (OER) plays a key role in determining the performance of overall water-splitting, while a core technological consideration is the development of cost-effective, efficient, and durable catalysts. Here, we demonstrate a robust reduced Fe-oxide@ $\text{NiCo}_2\text{O}_4$  bi-layered non-precious metal oxide composite as a highly efficient OER catalyst in an alkaline medium. A bi-layered oxide composite film with an interconnected nanoflake morphology ( $\text{Fe}_2\text{O}_3@\text{NiCo}_2\text{O}_4$ ) is reduced in an aqueous  $\text{NaBH}_4$  solution, which results in a moss-like  $\text{Fe}_3\text{O}_4@\text{NiCo}_2\text{O}_4$  (reduced Fe-oxide@ $\text{NiCo}_2\text{O}_4$ ; rFNCO) nanostructured film with an enhanced electrochemical surface area. The rFNCO film demonstrates an outstanding OER activity with an extraordinary low overpotential of 189 mV at  $10 \text{ mA cm}^{-2}$  (246 mV at  $100 \text{ mA cm}^{-2}$ ) and a remarkably small Tafel slope of  $32 \text{ mV dec}^{-1}$ . The film also has an excellent durability for more than 50 hours of continuous operation, even at  $100 \text{ mA cm}^{-2}$ . Furthermore, density functional theory calculations suggest that the unintentionally *in-situ* doped Ni during the reduction reaction possibly improves the OER performance of the rFNCO catalyst shifting *d*-band centers of both Fe and Ni active sites.

## 1. Introduction

To fulfil the ever-increasing global energy demand while simultaneously considering the environmental impact and the limited availability of natural resources, a wide variety of efficient and cost-effective energy conversion and storage devices have been devised and tested.<sup>1-3</sup> Of these devices, hydrogen generation from electrochemical water-splitting is particularly promising because of its unique advantages, including resource abundance, a  $\text{CO}_2$ -free process, and the potential for using renewable energy technologies as a sustainable power source. Two types of reactions occur in the electrolysis of water: the oxygen evolution reaction

(OER) at the anode and the hydrogen evolution reaction (HER) at the cathode.<sup>4</sup> Because the generation of oxygen kinetically requires the transfer of four electrons, a higher overpotential is needed for the OER.<sup>5</sup> Therefore, to produce highly efficient water-splitting electrolyzers, the design of low-overpotential-demanding OER catalysts is crucial. Toward this endeavor, iridium oxide (IrO<sub>2</sub>), ruthenium oxide (RuO<sub>2</sub>), and platinum (Pt) have been widely used as highly efficient electro-catalytic water splitting electrodes.<sup>6,7</sup> However, despite their high catalytic performance, the scarcity and high cost of the raw materials have limited their commercial application in water electrolysis. As a result, significant efforts have been made to replace these noble metal-based electrocatalysts with cost-effective and non-precious metal-based electrodes.

Over the past few years, metal hydroxides/oxides have been investigated as cost-effective and efficient OER and HER catalysts.<sup>8-15</sup> To achieve high electrocatalytic performance, it is important to design an electrode material with a large surface area having a high number of electrochemically active sites and high electrical conductivity.<sup>6,13</sup> Bulk materials (in powder form) are structurally unstable and suffer from poor electrochemical performance due to their limited surface area, circumscribing the number of active reaction sites.<sup>10,16,17</sup> Therefore, a general strategy for producing suitable electrodes is the growth of binder-free nanostructured active materials, such as nanotubes, nanosheets, hollow structures, and nanowires on mesoporous substrates.<sup>18-27</sup> The use of these materials can increase the electrochemically active surface area (ECSA) and electrical conductivity compared to their bulk counterpart, thus enhancing their electrocatalytic and electrochemical properties.

In this work, we demonstrate the direct growth of a non-precious metal-based oxide composite by reducing bi-layered oxide nanosheets of Fe<sub>3</sub>O<sub>4</sub> and NiCo<sub>2</sub>O<sub>4</sub> (*viz.* reduced Fe-oxide@NiCo<sub>2</sub>O<sub>4</sub> denoted as rFNCO). The rFNCO composite electrode was prepared on Ni foam via electrodeposition, followed by annealing and a reduction reaction. A well-defined

mesoporous rFNCO electrode with a moss-like nanostructured surface was achieved, exhibiting outstanding water-splitting performance in an aqueous alkaline electrolyte. It exhibits an ultra-low OER overpotential of 189 mV at 10 mA cm<sup>-2</sup> (246 mV at 100 mA cm<sup>-2</sup>) with a very small Tafel slope of 32 mV dec<sup>-1</sup>. Also, the electrode shows excellent long-term electrochemical stability even at a high current density of 100 mA cm<sup>-2</sup>. Moreover, density functional theory (DFT) calculations were performed to further understand the improved OER performance. This catalytic material is particularly advantageous due to its structural integrity, high aspect ratio, easy accessibility, and rich active sites.

## **2. Experimental**

### *2.1. Material Synthesis*

Moss-like rFNCO electrodes were fabricated on a Ni foam substrate sequentially using the following synthesis process: (i) electrodeposition of the NiCo<sub>2</sub>O<sub>4</sub> (NCO) bottom layer on the Ni foam substrate, (ii) electrodeposition of the top Fe<sub>2</sub>O<sub>3</sub> layer on the NCO layer followed by thermal annealing, and finally (iii) chemical reduction to produce rFNCO (Fig. 1). For electrodeposition of the bi-layered metal oxide composite film, Ni foam was used as the working electrode (WE) while a Pt wire served as the counter electrode (CE) and a saturated calomel electrode (SCE) was employed as the reference electrode (RE). Before electrodeposition, the Ni foam substrate, with an area of 1×5 cm<sup>2</sup>, was consecutively cleaned via sonication with 3 M HCl, acetone, ethanol, and deionized water to remove the native oxide layer and surface impurities.

Thin bi-layered metal oxide composite films were potentiostatically electrodeposited in an aqueous bath containing different molar concentrations of FeCl<sub>2</sub>·4H<sub>2</sub>O and different molar ratios of Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O and Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O precursors. NCO was first electrodeposited under a constant potential of -1.0 V (vs SCE). Four molar concentration ratios of Ni(NO<sub>3</sub>)<sub>2</sub>:Co(NO<sub>3</sub>)<sub>2</sub>

(1:2, 1:1, 2:1, and 4:1) were examined, and a ratio of 2:1 was found to be the optimal selection, with the lowest overpotential and Tafel slope (Fig. S1). The top Fe<sub>2</sub>O<sub>3</sub> layer was then fabricated in a bath containing a FeCl<sub>2</sub>·4H<sub>2</sub>O precursor under a constant potential of -1.0 V (vs SCE). The top Fe<sub>2</sub>O<sub>3</sub> layer was also optimized by varying the FeCl<sub>2</sub> molar concentration (5, 15, 30, 45, and 60 mM), and the molar concentration of 45 mM exhibited the best performance. The bi-layered Fe<sub>2</sub>O<sub>3</sub>/NiCo<sub>2</sub>O<sub>4</sub> (FNCO) film was then rinsed with ethanol and deionized water and dried at 60 °C for 12 hours and annealed at 200 °C for 2 hours with a ramping rate of 1 °C/min. Finally, to enhance the electrochemical activity, the FNCO film was soaked in a 0.1 M aqueous NaBH<sub>4</sub> solution, for 30 minutes, to induce a reduction reaction and obtain the final rFNCO film.

## *2.2. Characterization methods*

The morphologies and chemical compositions of the electrode films produced at each synthesis step were investigated using field emission scanning electron microscopy (FE-SEM) coupled with energy-dispersive X-ray spectroscopy (EDS) and an image-mapping accessory. The crystal structure and composition of the films were determined using high-resolution transmission electron microscopy (HR-TEM), high-angle annular dark (HAADF) scanning transmission electron microscope (STEM), selected area electron diffraction (SEAD), and HAADF-STEM EDS elemental mapping. Binding states were investigated via X-ray photoelectron spectroscopy (XPS).

## *2.3. Electrochemical measurements and analysis*

The electrocatalytic OER performance of the electrodes was evaluated using linear sweep voltammetry (LSV), electrochemical impedance spectroscopy (EIS) and cyclic voltammetry (CV). Electrochemical measurements were performed in a conventional three-electrode cell,

where a platinum wire served as the CE, the proposed moss-like rFNCO electrode was used as the WE, and an SCE was employed as the RE. An aqueous 1 M KOH solution was used as the electrolyte.

### **3. Results and discussion**

#### *3.1. The structural and morphological properties of the catalyst films*

Figures 2a-d show top-view FE-SEM images of the Ni foam substrate, NCO, FNCO, and rFNCO, respectively. The substrate was fully covered by the electrochemically active materials after each deposition and reduction step (Figs. 2b-d). While the NCO and FNCO electrodes consisted of similarly shaped interconnected nanosheets, the rFNCO electrode demonstrated moss-like aggregates of nanoparticles. The dramatic morphological change from nanosheets to aggregated nanoparticles is related to the hydroxyl species that are produced by hydrolysis of  $\text{NaBH}_4$  solution used in the chemical reduction of FNCO.<sup>24</sup> This is more discussed in a following section with the XPS results. Moss-like aggregates began to form on the edges of the nanosheet, eventually covering surface of the nanosheet (Fig. S2). Moreover, not only on the surface, but their presence all over the film and NCO base-nanosheets structures beneath them are confirmed via FIB cross-section TEM and EDS (Figs. S3 and S4). Based on the EDS analysis, the atomic Co:Ni ratio in NCO, FNCO, and rFNCO were determined to be 1:11.73; 1:10.50, and 1:24, respectively (Table S1). However, due to the thin-film deposits, penetration of the X-ray probe could have reached the NF substrate. Thus, the measured Ni content for the samples may be higher than the actual values.

The formation of a nanoscale morphology was revealed by electron microscopy. Figures 3a-c present TEM images of the NCO, FNCO, and rFNCO samples, respectively. Interestingly, Fig. 3a shows that the nanosheets are made up of numerous interconnected nanoparticles with a slightly crumpled surface at the edge of the sheet (marked with an arrow), which can also be

observed in the FE-SEM image for the NCO sample (Fig. 2b). Even after the addition of  $\text{Fe}_2\text{O}_3$ , the nanosheet morphology was maintained, but the crumpled edges of these nanosheets became wider in the FNCO sample (Fig. 3b, marked with arrows). Also, the TEM image of the rFNCO sample (Fig. 3c) shows aggregated nanoparticles, which is consistent with the aggregated nanoparticles observed in the FE-SEM image (Fig. 2d). Moreover, HAADF-STEM elemental mapping results confirm uniform distributions of the constituents (Fig. S4). After the reduction of  $\text{NaBH}_4$ , a small amount of boron is clearly detected in the EDX and XPS spectra of the rFNCO electrode.

### *3.2. Crystal phase and chemical composition analysis*

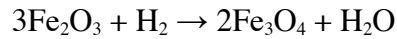
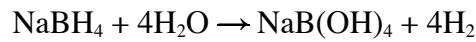
Crystallinity and microstructure of the as-prepared samples were studied via comprehensive electron microscopy characterizations, as shown in Figs. 3d-g. The NCO sample (Fig. 3d) exhibits lattice fringe distances ( $d$ ) of 0.15 and 0.21 nm, which are associated with the (511) and (400) planes of  $\text{NiCo}_2\text{O}_4$  (JCPDS 73-1702), respectively. The FNCO sample (Fig. 3e) has a  $d$  of 0.30 (indicated by the white box) and 0.27 nm (blue box), corresponding to the (220) plane of  $\text{NiCo}_2\text{O}_4$  (JCPDS 20-0781) and the (104) plane of  $\text{Fe}_2\text{O}_3$  (JCPDS 89-0599), respectively. Finally, the HRTEM image of the rFNCO sample presented in Fig. 3f reveals  $d$  of 0.26 nm, corresponding to the (311) plane of  $\text{Fe}_3\text{O}_4$  (JCPDS 89-0951). The transformation from  $\text{Fe}_2\text{O}_3$  to  $\text{Fe}_3\text{O}_4$  phase is likely due to the chemical reduction of  $\text{Fe}^{3+}$  in  $\text{Fe}_2\text{O}_3$  by  $\text{NaBH}_4$ . As a result, the  $\text{Fe}_3\text{O}_4$  phase was detected on the rFNCO surface instead of  $\text{Fe}_2\text{O}_3$ . However, no  $\text{NiCo}_2\text{O}_4$  phase is resolved in the HR-TEM image of rFNCO, possibly due to the poor crystallinity of the as-deposited NCO layer and the amorphous phase generated during the reduction process. Diffused SEAD ring patterns and dot patterns can be observed in Fig. 3g, which indicates the coexistence of polycrystalline and amorphous phases in NCO.<sup>28</sup> Figure 3h presents the concentric SEAD ring patterns for the FNCO sample, which can be attributed to



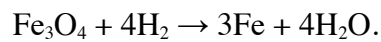
the coexistence of  $\text{NiCo}_2\text{O}_4$  (JCPDS 20-0781) and  $\text{Fe}_2\text{O}_3$  (JCPDS 89-0599) phases. This is in good agreement with the HR-TEM image of FNCO, as displayed in Fig. 3e. Overall, these microscopy results suggest that the  $\text{NiCo}_2\text{O}_4$  flakes are covered by the  $\text{Fe}_2\text{O}_3$  nanostructures. In addition, no significant lattice expansion can be resolved, implying that the Fe-based compound is not intercalated with the  $\text{NiCo}_2\text{O}_4$ . Moreover, based on the TEM, HR-TEM and SEAD analyses, we could conclude that the as-prepared NCO film is polycrystalline in nature before the  $\text{Fe}_2\text{O}_3$  coating but transformed into the amorphous phase during the chemical reduction process. Also, it is worth noting from Figs. S3b and S4c that Ni-species from the underlying nanosheets can be doped into  $\text{Fe}_3\text{O}_4$  during the reduction reaction. DFT calculations reveal that this presumption of Ni-doping can explain the remarkably improved OER performance after the reduction, and the point will be discussed in detail in a subsequent section.

The elemental composition and oxidation states of the as-prepared FNCO and the rFNCO electrodes were confirmed by XPS analysis. As shown in Fig. 4a, the FNCO electrode has three Fe  $2p^{3/2}$  peaks at 719.2, 714.2, and 711.4 eV, which corresponded to the satellite,  $\text{Fe}^{3+}$  and  $\text{Fe}^{2+}$  oxidation states, respectively.<sup>29-31</sup> On the other hand, the rFNCO electrode displays shifted peaks at 717.4, 713.9, and 711.0 eV. An additional peak at 707.1 eV (marked with the thick arrow) corresponds to the metallic binding state of  $\text{Fe}^0$ . After the reduction process, the intensity of the binding peaks also decreased. The observation of negatively shifted peaks and the metallic binding state for the rFNCO electrode indicates that the film had been successfully reduced and would likely become conductive after the chemical reduction reaction. This would electronically bridge the rFNCO and the corresponding catalytically active M-OOH formed, as a result of the anodic bias during the OER, with the NF substrate. Consequently, the charge transfer resistance between the electrode and the electrolyte is reduced, resulting in enhanced OER catalytic activity.

The NaBH<sub>4</sub>-based reduction is a result of the spontaneous release of H<sub>2</sub> from the exothermic reaction between NaBH<sub>4</sub> and H<sub>2</sub>O:<sup>32,33</sup>



Further, because the intermediate wüstite oxide, Fe<sub>1-x</sub>O is not stable below 570 °C, Fe<sub>3</sub>O<sub>4</sub> can be reduced partially as metallic iron (Fe), which can be described as follows:<sup>33</sup>



The reduction of Fe<sub>2</sub>O<sub>3</sub> was also confirmed by the O 1s spectra (Fig. 4b). For the FNCO sample, the spectrum was deconvoluted into three binding peaks at 532.7, 531.5, and 530.2 eV which correspond to carbon-related or surface-absorbed water molecules (O1), lattice FeOH or absorbed hydroxyl (O2), and oxygen atoms bound to metals (O3), respectively.<sup>34</sup> After the reduction process, the metal-binding peak O3 decreased significantly, whereas the other two peaks at higher energies increased, especially O2. This finding is consistent with the presence of the metallic binding state Fe<sup>0</sup> observed for the rFNCO. In addition, in line with the above hydrolysis reaction of NaBH<sub>4</sub>, the stronger hydroxyl species-related peak (O2) in the rFNCO sample is possibly due to the residual NaB(OH)<sub>4</sub> that formed during the hydrolysis of NaBH<sub>4</sub>, suggesting that hydroxyl species are produced during the reduction process. Xu et al. demonstrated that the hydroxyl ions in a reaction solution regulate Fe<sub>3</sub>O<sub>4</sub> morphology.<sup>24</sup> Based on the first principle, they calculated the adsorption energies of OH<sup>-</sup> on different crystal planes of Fe<sub>3</sub>O<sub>4</sub> and showed that, when the influence of OH<sup>-</sup> adsorption on specific crystal planes is low, isotropic spherical Fe<sub>3</sub>O<sub>4</sub> forms. In the present study, the hydrolysis of NaBH<sub>4</sub> that occurs during the chemical reduction of FNCO produces a weak NaB(OH)<sub>4</sub> base, resulting in the low concentration of OH<sup>-</sup> species. Under this low OH<sup>-</sup> concentration, a similar morphological evolution occurs, leading to the formation of moss-like aggregates of nanoparticles.

### 3.3. Evaluation of the electrocatalytic activity and stability

The electrocatalytic OER activity of the electrodes, including bare nickel foam (NF), were evaluated using LSV at a scan rate of  $10 \text{ mV s}^{-1}$  (Fig. 5a). The bare NF electrode exhibits the weakest catalytic activity, requiring a high overpotential of 318 mV at  $10 \text{ mA cm}^{-2}$ . The electrocatalytic water-splitting performance of the other samples is compared in terms of their overpotential in delivering benchmark current densities of 10, 50, and  $100 \text{ mA cm}^{-2}$  (Fig. 5 b). During the LSV measurements, the Fe-oxide and FNCO electrodes produced a current density of  $10 \text{ mA cm}^{-2}$  at an overpotential of 243 mV and 219 mV, respectively. Notably, the rFNCO electrode shows that a remarkably low overpotential of only 189 mV is required to deliver a current density of  $10 \text{ mA cm}^{-2}$ . The rFNCO electrode also exhibits a very low overpotential of 246 mV even at a very high current density of  $100 \text{ mA cm}^{-2}$ . It is worth noting that the catalytic OER activity achieved by the rFNCO electrode is comparable or even superior to that of the recently reported state-of-the-art non-precious metal oxide-based electrocatalysts (Fig. 5c).<sup>35-44</sup> Furthermore, the intrinsic activity of the samples was assessed by normalizing the geometrical current density using the corresponding ECSA,<sup>26</sup> as shown in ECSA-based LSV curves (Fig. S7). The normalized LSV curves revealed that the intrinsic OER catalytic activity of the samples followed the same order of rFNCO > FNCO > NCO, as observed in the geometrical area-based voltammograms.

Tafel slopes were obtained from the LSV plots of the catalysts to assess the OER kinetics (Fig. 5d). The Tafel slope of the rFNCO electrode is  $32 \text{ mV dec}^{-1}$ , which is smaller than those of the NF ( $71 \text{ mV dec}^{-1}$ ), NCO ( $45 \text{ mV dec}^{-1}$ ), Fe-oxide ( $36 \text{ mV dec}^{-1}$ ), and FNCO ( $43 \text{ mV dec}^{-1}$ ) electrodes. The Tafel slope is superior compared to those of the state-of-the-art commercial  $\text{RuO}_2$  ( $72 \text{ mV dec}^{-1}$ ) and MOF-based ( $42 \text{ mV dec}^{-1}$ ) electrodes.<sup>7,36</sup> The very small Tafel slope of the rFNCO/NF electrode indicates rapid electron/mass transfer between the electrode and the electrolyte during the OER, confirming its superior OER kinetics.

Interestingly, the Tafel slopes of the rFNCO and Fe-oxide electrodes remained steep even at high currents. This is because the morphology of rFNCO and Fe-oxide allows for the effective release of bubbles from the electrodes during O<sub>2</sub> evolution.

EIS measurements were carried out to further elucidate the kinetics of the electrocatalytic OER reaction at an AC excitation potential of 10 mV and frequencies ranging from 0.1 Hz to 10 kHz. The EIS spectra of the electrodes are presented in Fig. 5e. The obtained Nyquist plots were fitted using a simple equivalent circuit (see the inset of Fig. 5e), which is denoted by the solid lines. Details of the impedance parameters extracted from the fitting of the Nyquist plots are provided in Table S2. The  $R_s$  represents a combination of the bulk electrolyte resistance, the internal resistance of the substrate, including contact with the current collector, and other contact resistances.<sup>45-47</sup> The semi-circle is attributed to the charge transfer resistance ( $R_{ct}$ ) whereas the straight line is assigned to Warburg impedance ( $W$ ) which is representative of the diffusion behaviour of an electrode material for electroactive species.<sup>48</sup> The NCO electrode has  $R_s$  and  $R_{ct}$  of 0.93  $\Omega$  and 0.17  $\Omega$ , respectively. The FNCO electrode has lower values of 0.84  $\Omega$  and 0.16  $\Omega$ , respectively, suggesting that the intrinsic and charge transfer resistance of the electrode is reduced after FeO deposition. After the reduction process, it was found that the electron/ion transport became more efficient, with a further reduction in  $R_{ct}$  to 0.11  $\Omega$  for the rFNCO electrode. Thus, the  $R_{ct}$  for the rFNCO electrode is improved by more than 30% compared with that of the NCO and FNCO electrodes. This is associated with the synergistic effects of extensive contact with the electrolyte and the shorter ion-diffusion pathways resulting from the moss-like aggregated nanoparticle surface of the rFNCO containing Fe<sup>0</sup>. Also, the slope of the Warburg element in low-frequency region increased dramatically after the reduction process (NCO < FNCO < rFNCO). The rapid and efficient electron/ion transport at the electrode/electrolyte interface is the direct result of many oxygen vacancies produced by the reduction process and the moss-like morphology of the rFNCO. These factors facilitate the

transport of the electrons and OER active species such as  $\text{OH}^-$ , promote their interaction with the catalytically active sites and remove bubbles on the surface effectively, thus enhancing OER reaction kinetics.<sup>9,47</sup>

To confirm the reproducibility of the observed OER performance, several rFNCO electrode films were fabricated under the same conditions and their OER properties were assessed. The average overpotential for these films was 198 mV at a current density of  $10 \text{ mA cm}^{-2}$ , with an acceptable standard deviation of  $\pm 8 \text{ mV}$ . Similarly, the average Tafel slope was  $37 \text{ mV dec}^{-1} \pm 4 \text{ mV dec}^{-1}$  (Fig. S5).

To comprehensively understand the effect of the electrode kinetics, as indicated by the Tafel slopes and EIS spectra on the electrochemical reaction at the electrolyte/electrode interface, the ECSA of each electrode was evaluated by determining its electrochemical double-layer capacitance (EDLC;  $C_{dl}$ ).<sup>49</sup> (Fig S6) As shown in Fig. 6a, the estimated ECSA for the NCO, FNCO, and rFNCO electrodes was 365.0, 537.5, and  $1222.5 \text{ cm}^2$ , respectively, showing that the rFNCO electrode was significantly more electrochemically active than the other electrodes. This suggests that the reduction process resulted in a high density of electrochemically active sites on the FNCO electrode. Consequently, the kinetic activity of the rFNCO electrocatalyst was much higher than those of the other electrodes.

Figure 7a shows the results of stability for the rFNCO electrode based on a chronopotentiometry test. Constant current densities of 10, 50, and  $100 \text{ mA cm}^{-2}$  were applied for 20 hours each and the corresponding overpotential was measured. The rFNCO electrode shows excellent stability with very little fluctuation ( $< 4 \text{ mV}$ ,  $\sim 1 \%$ ) even at high current densities. Figure 7b presents the LSV curves of the rFNCO electrode before and after stability testing. The measured LSV curves are almost identical, thus confirming its electrochemical stability. The measured electrochemical stability of the FNCO electrode at various current

densities is presented in Fig. S8 (Supplementary Information), revealing a relatively poor stability particularly at a high current bias.

The SEM images of rFNCO both before and after the stability test are shown in Fig. 7c and Fig. S9. After a long-term stability test, bulky submicron-sized agglomerates formed on the surface. To identify the origin of these agglomerates, the chemical composition of the electrode after the stability test was investigated using SEM-EDS. As shown in the elemental mapping images, the main elemental components of the agglomerates are potassium (K) and oxygen (O), which originate from the KOH electrolyte. In addition, after the long-term stability test, the metallic Fe<sup>0</sup> peak disappears from the Fe 2p spectrum but the O3 peak (associated with Fe-O binding) in the O 1s spectrum increases, indicating that the metallic Fe was oxidized (Fig. S10 in the Supplementary Information). Although electrolyte-associated agglomerates were detected during the stability test, the rFNCO electrode still exhibited remarkable electrochemical stability, suggesting that the agglomerates cover only a small portion of the electrode and there is a negligible phase transition. The unique moss-like morphology of the rFNCO is also considered as a critical factor contributing to the excellent stability because the generated gas bubbles can be effectively released from the electrode, thus maintaining the initially existing high number of electrochemically active sites. The measured stability of various catalysts including our sample is presented in Table S3 in the Supplementary Information.

### *3.4. Computational calculations*

Furthermore, we also performed DFT calculations to gain further insights into the origin of the OER electrocatalytic activity on the Ni-doped Fe<sub>3</sub>O<sub>4</sub> structure. For the investigation of the Ni incorporation effect on the improved OER performance, we preferentially designed reasonable Ni doped Fe<sub>3</sub>O<sub>4</sub> bulk and surface structures (Figs S11, designed structures are

described in the Supplementary Information) based on the experimental TEM-EDS results on the surface of the rFNCO composite (Fig S3b). Given the well-established pure and doped structure, we systematically investigated OER activities by overpotential ( $\eta^{\text{OER}}$ ), using a general free energy diagram (FED) approach (Figs. 12b, S15b, and S16 b) for all possible active sites (Figs. S11c and S12 c,d).<sup>50-52</sup> The calculated FEDs reveal that the FN<sub>0.25</sub>O structure has a significantly low OER overpotential of 0.41 V outperforming that of FN<sub>0.375</sub>O (0.61 V) and pure Fe<sub>3</sub>O<sub>4</sub> (0.66 V), and it theoretically represents competitive catalytic activity for conventional RuO<sub>2</sub> (0.43 V). Here, the most active FED in Fe<sub>3</sub>O<sub>4</sub> clearly shows that the second step of OER ( $\Delta G_2^{\text{OER}}$ ) associated with OH\* and O\* intermediates is a significant uphill reaction (Fig S15b). Therefore, we intensively explored the changes of reaction free energies for all possible Fe sites under the ideal potential to emphasize the importance of  $\Delta G_2^{\text{OER}}$  values (Fig. S16a) and found that the OER overpotentials undoubtedly come from strong OH\* and weak O\*, which show the linear scaling relationship (Fig. S16b). From these results, one can deduce that the  $\Delta G_2^{\text{OER}}$  plays an important role in determining the OER activity as the potential determining step (PDS). Hence, we systematically investigated  $\Delta G_2^{\text{OER}}$  variations induced by the Ni incorporation (FN<sub>0.25</sub>O and FN<sub>0.375</sub>O), and identified that the binding strengths of OH\* (O\*) in the FN<sub>0.25</sub>O are remarkably lower (higher) than those for a pure system, respectively (Figs. 12a and b). Based on these changed free energies, the results in Fig. S18 also reveal that the difference on  $\Delta G_2^{\text{OER}}$  values under the ideal potential explains the OER activity variations well, which show the improved scaling relationship. This theoretical evaluation implies that the suitable binding of intermediates can make the  $\Delta G_2^{\text{OER}}$  value closer to the ideal potential of 0.402 V in an alkaline media, which leads to the enhanced OER catalytic performance.

The binding strength of intermediates at PDS is strongly correlated with the tendency of valence orbitals of active sites that judge the electron filling of the anti-bonding state near the Fermi level.<sup>53-55</sup> Interestingly, the binding configuration of the OH\* is the on-top on the Fe site,

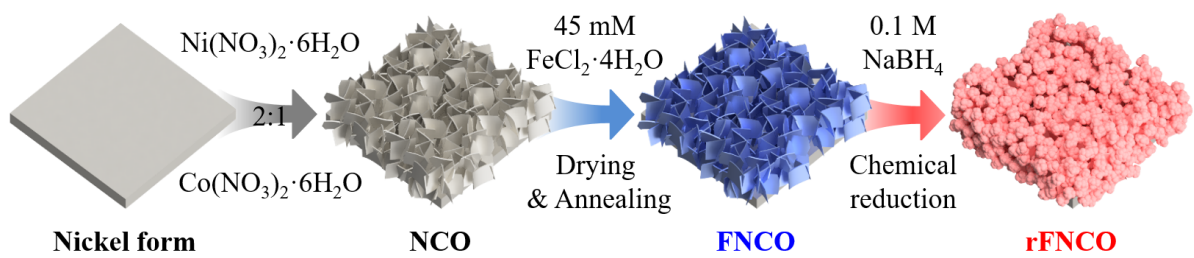
and that of the O\* is the bridge on the Fe and Ni sites. Therefore, we focused on the position of the *d*-band center with all-metal sites of the designed pure and doped structures. The partial density of states (PDOS) in Fig. 8c shows that the *d*-band center of Fe (Ni) active sites in the FN<sub>0.25</sub>O is shifted to a lower (higher) position compared to Fe sites of Fe<sub>3</sub>O<sub>4</sub>. This theoretical viewpoint implies that the Fe active sites of FN<sub>0.25</sub>O can have decreased OH\* binding strength, whereas the Ni active sites can have increased O\* binding strength. Furthermore, the additional electronic results in Fig. S19 reveal that the Fe<sub>3</sub>O<sub>4</sub> and FN<sub>0.25</sub>O structures have metallic properties, which can enhance the catalytic activity, and have the particularly large contribution of metals to frontier energy states around the Fermi level consistent with the active site preference. Consequently, it is worth noticing that the characteristic electronic feature of FN<sub>0.25</sub>O leads to improving OER catalytic performance by desirably shifting the *d*-band centers of both Fe and Ni active site.

#### 4. Conclusions

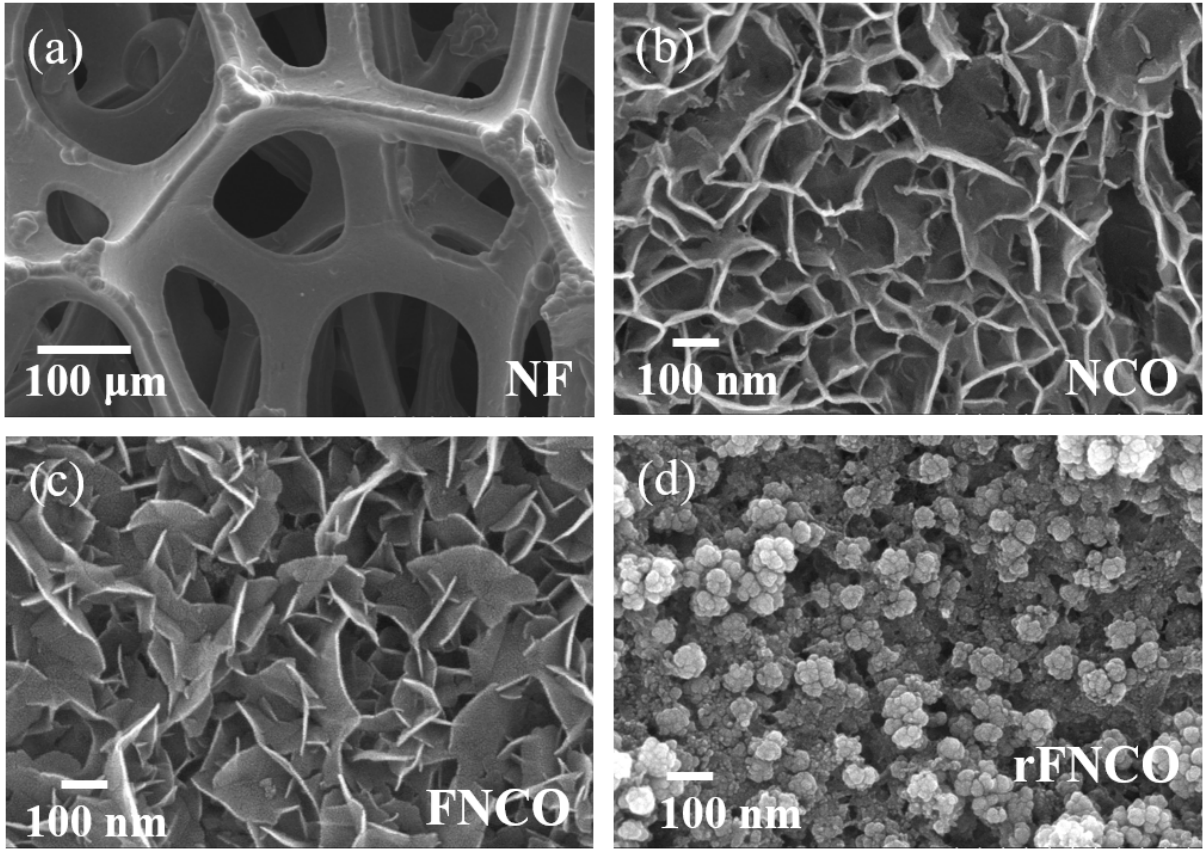
The present study demonstrated a simple and scalable electrodeposition process combined with a reduction reaction for the fabrication of NCO, FNCO, and reduced rFNCO electrodes on Ni foam. The NaBH<sub>4</sub> reduction reaction reduced Fe<sub>2</sub>O<sub>3</sub> and transformed the surface of the FNCO nanosheets into moss-like aggregates of nanoparticles doped with Ni, leading to a significant increase in the ECSA, reducing the number of bubbles on the surface, enhancing conductivity, and subsequently improving the electrochemical OER performance. The DFT calculations showed that the unintentionally *in-situ* doped Ni on Fe<sub>3</sub>O<sub>4</sub> can lower the overpotential, improving the OER performance by reducing the required energy in PDS. Experimentally, the optimal rFNCO electrode exhibited a very low overpotential of 189 mV at 10 mA cm<sup>-2</sup> with an ultra-small Tafel slope of 32 mV dec<sup>-1</sup>. The rFNCO electrode also exhibited excellent electrochemical stability, with a chronopotentiometric variation of only 4



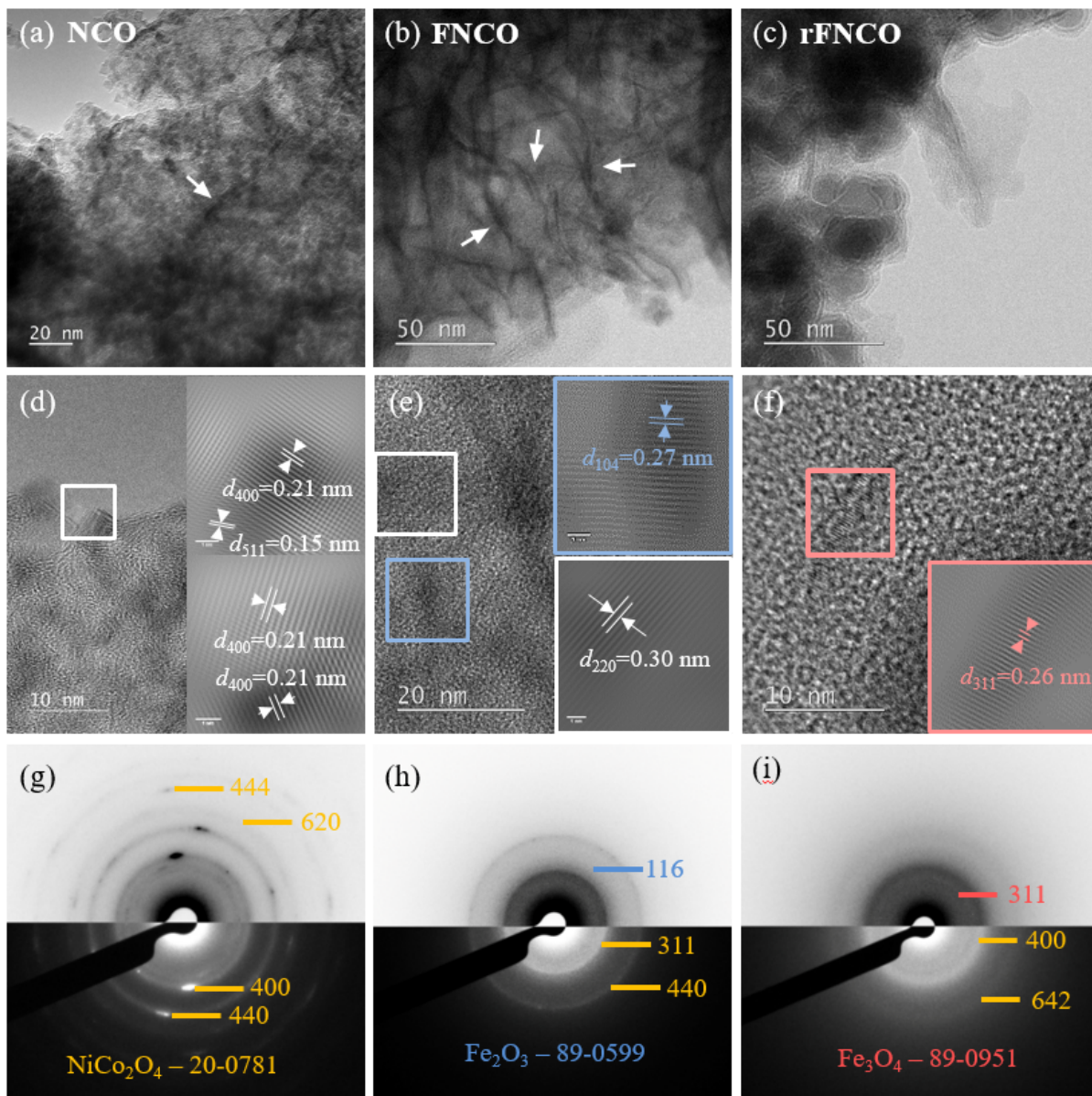
mV even at a very high current density of  $100 \text{ mA cm}^{-2}$  for 50 h. Given the present work, key perspectives, such as further development of rFNCO-based nanostructures and the application of other iron compounds for eco-friendly electrochemical water splitting, can be envisioned.



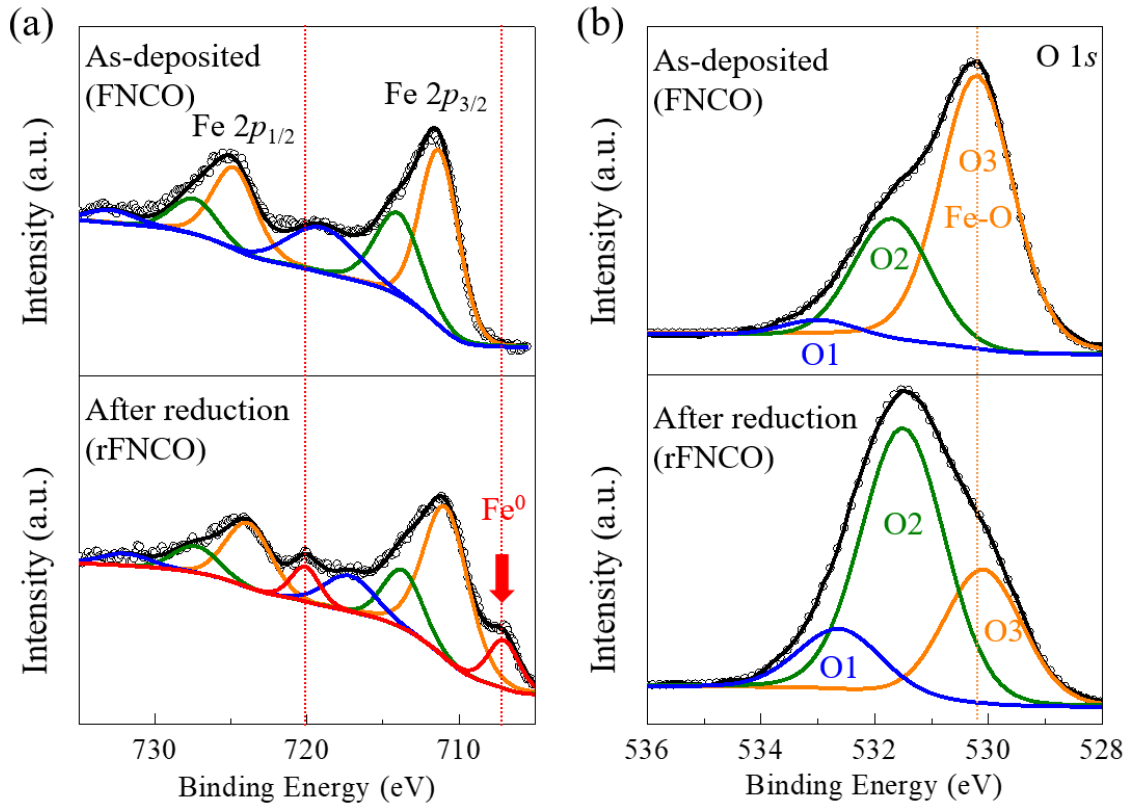
**Figure 1.** Schematic illustration of the fabrication process for the growth of an rFNCO electrode on Ni foam. The NCO and FNCO films are deposited using a three-electrode system, and a tube furnace is used for annealing.



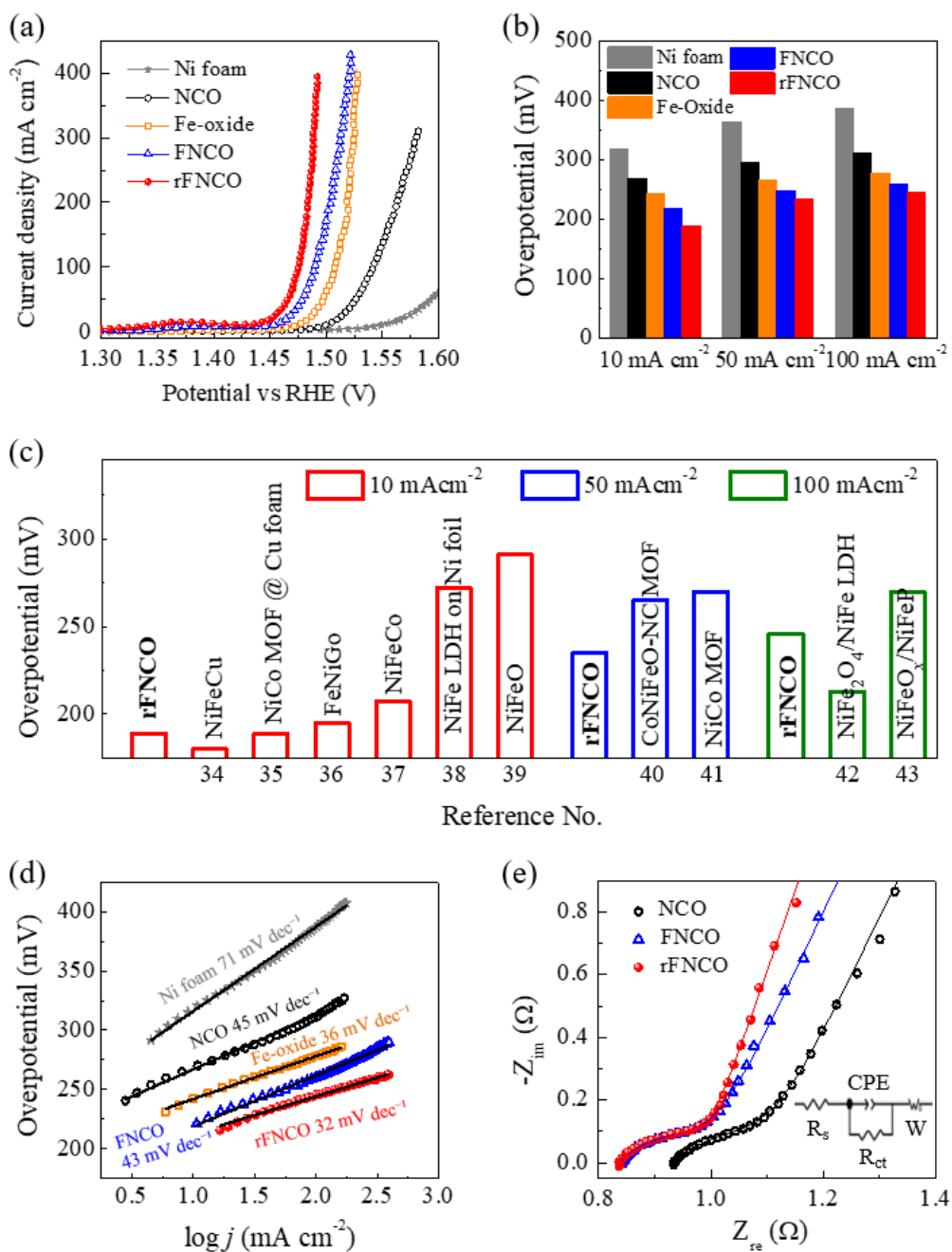
**Figure 2.** Top FE-SEM views of (a) Ni foam, (b) NCO, (c) FNCO, and (d) rFNCO on a Ni foam substrate. Dramatic morphology transform is observed between FNCO and rFNCO.



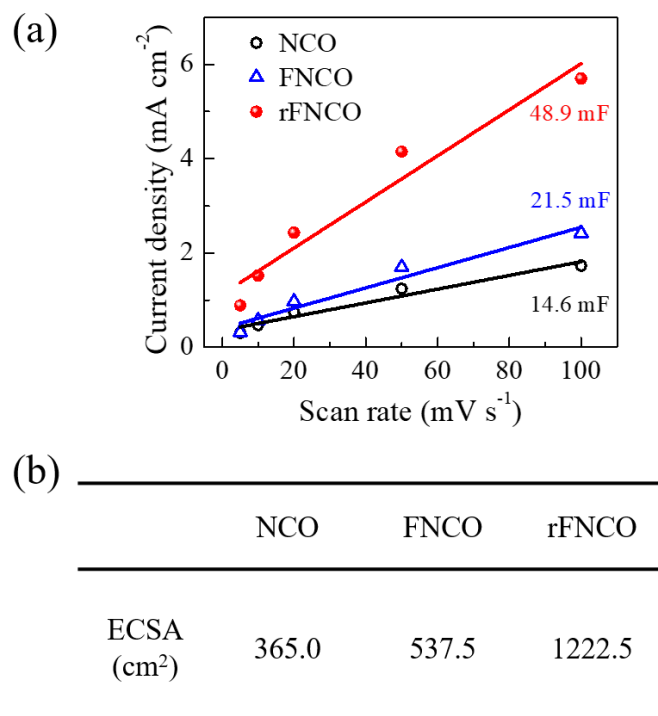
**Figure 3.** (a-c) Bright-field TEM images, (d-f) HR-TEM images of NCO, FNCO, and rFNCO samples, respectively. White arrows in the bright-field TEM images indicate a crumpled surface at the edges for NCO and FNCO. (g-i) SEAD patterns of NCO, FNCO, and rFNCO samples. White (or orange), Blue, red colours in HR-TEM and SEAD pattern images are associated with NCO, FNCO, and rFNCO, respectively.



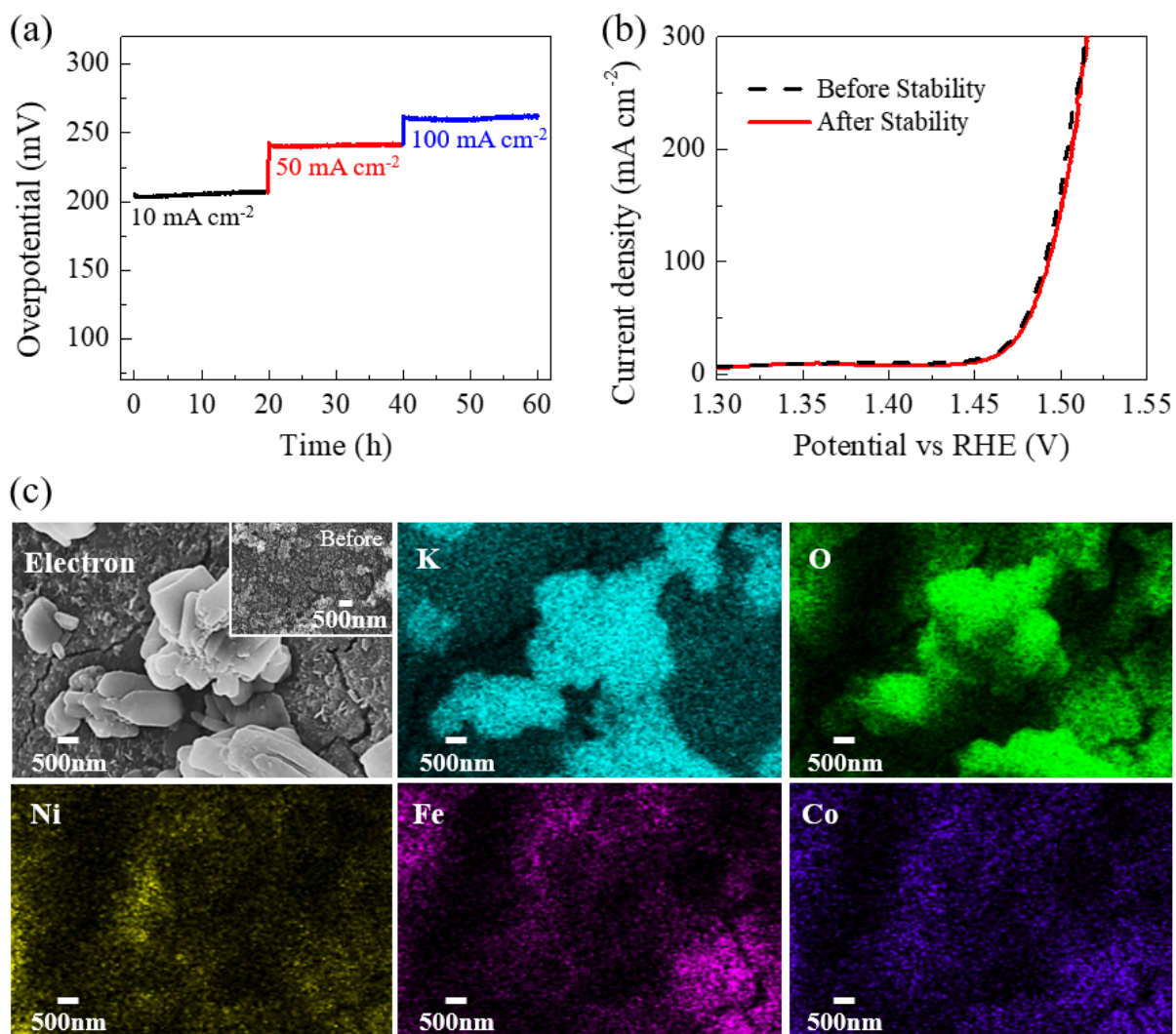
**Figure 4.** XPS measurements. Core level (a) Fe 2p and (b) O 1s spectra of the FNCO and rFNCO. The complex XPS spectra are deconvoluted in to several components using the Gaussian-Lorentz curve fitting.



**Figure 5.** OER catalytic activity of the Ni foam (substrate), Fe-oxide, FNCO, and rFNCO. (a) LSV curves at  $10 \text{ mV s}^{-1}$ , (b) comparison of the obtained overpotentials at different current densities, (c) comparative electrocatalytic OER performance of our rFNCO catalyst and recently reported state-of-the-art catalysts at various driving current densities, (d) Tafel plots, and (e) Nyquist plots.

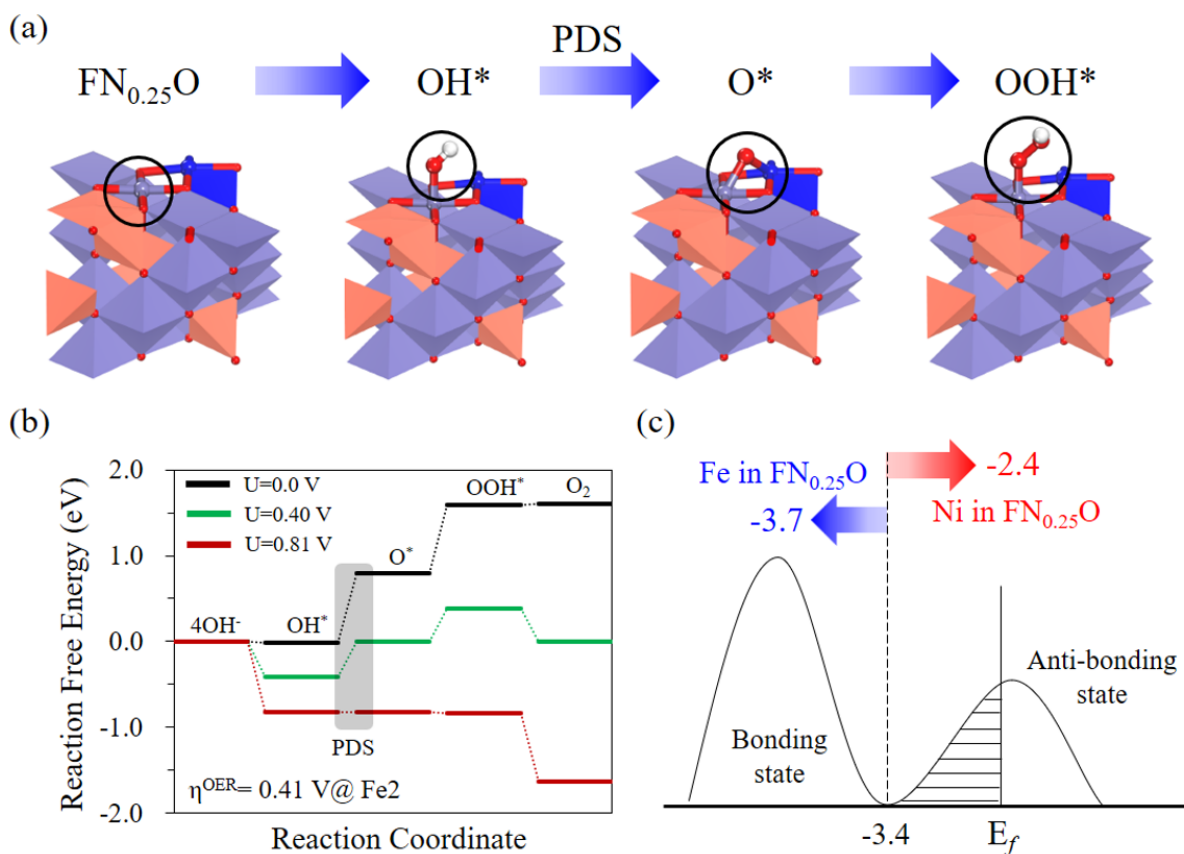


**Figure 6.** (a) Non-faradaic current density obtained from CV curves at 0.22 V as a function of scan rate ( $\text{mV s}^{-1}$ ), and (b) a comparison of the ECSA.



**Figure 7.** (a) Electrochemical stability of the rFNCO electrode at various current densities, (b) LSV curves for the rFNCO electrode before and after stability testing, and (c) EDS elemental mapping images for the rFNCO electrode after stability testing.





**Figure 8.** (a) Most active OER mechanistic on the  $\text{FN}_{0.25}\text{O}$  structure and its potential-determining step (PDS). (b) Free energy diagrams on the most active Fe2 active site of  $\text{FN}_{0.25}\text{O}$  for the OER in an alkaline environment. All possible active sites are shown in Fig. S11c. (c) Schemes of  $d$ -band center variation and anti-bonding state occupation in partial density of states (PDOS) of metal sites in  $\text{Fe}_3\text{O}_4$  and  $\text{FN}_{0.25}\text{O}$ . The black dashed line indicates the standard  $d$ -band center value of Fe sites in the  $\text{Fe}_3\text{O}_4$  structure.

## ASSOCIATED CONTENT

### **Supporting Information**

Detailed optimization of samples, physical characterizations, electrochemical measurements, and theoretical calculation details and results (PDF). This material is available free of charge via the Internet at <http://pubs.acs.org>.

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Y.J. and S.C. equally contributed to this work as co-first authors. The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

## Notes

The authors declare no competing financial interest.

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