

1 Novel Ternary Metals-based Telluride Electrocatalyst with Synergistic Effects of High Valence
2 Non-3d Metal and Oxophilic Te for pH-Universal Hydrogen Evolution Reaction

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29 pH-universal hydrogen evolution reaction

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1 ABSTRACT

2 Electrocatalyst designs based on oxophilic foreign atoms are considered a promising
3 approach for developing efficient pH-universal hydrogen evolution reaction (HER)
4 electrocatalysts by overcoming the sluggish alkaline HER kinetics. Here, we design ternary
5 transition metals-based nickel telluride (MoW_{Ni}Te) catalysts consisting of high valence non-3d
6 Mo and W metals and oxophilic Te as a first demonstration of non-precious heterogeneous
7 electrocatalysts following the bifunctional mechanism. The MoW_{Ni}Te showed excellent HER
8 catalytic performance with overpotentials of 72, 125, and 182 mV to reach the current densities of
9 10, 100, and 1000 mA cm⁻², respectively, and the corresponding Tafel slope of 47, 52, and 58 mV
10 dec⁻¹ in alkaline media, which is much superior to commercial Pt/C. Additionally, the HER
11 performance of MoW_{Ni}Te is well maintained up to 3000 hours at the current density of 100 mA
12 cm⁻². It is further demonstrated that the MoW_{Ni}Te exhibits remarkable HER activities with an
13 overpotential of 45 mV (31 mV) and Tafel slope of 60 mV dec⁻¹ (34 mV dec⁻¹) at 10 mA cm⁻² in
14 neutral (acid) media. The superior HER performance of MoW_{Ni}Te is attributed to the electronic
15 structure modulation, inducing highly active low valence states by the incorporation of high
16 valence non-3d transition metals. It is also attributed to the oxophilic effect of Te, accelerating
17 water dissociation kinetics through a bifunctional catalytic mechanism in alkaline media. Density
18 functional theory calculations further reveal that such synergistic effects lead to reduced free
19 energy for an efficient water dissociation process, resulting in remarkable HER catalytic
20 performances within universal pH environments.

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1 **1. Introduction**

2 Hydrogen fuel (H₂) generated by electrochemical water splitting has been considered a
3 potential alternative to traditional fossil fuels, to address the energy crisis and global warming, due
4 to its outstanding energy density and eco-friendly manufacturability [1-3]. Considerable effort has
5 been focused on designing and realizing high-efficiency and enduring electrocatalysts for efficient
6 renewable energy conversion. However, for genuine practical applications, overcoming the energy
7 barrier associated with sluggish reaction kinetics for water dissociation remains challenging, which
8 requires a higher potential than the theoretical value [4-7]. In particular, the hydrogen evolution
9 reaction (HER) kinetics in alkaline media is much slower than that in its acidic counterpart. This
10 is attributed to its multi-step reaction pathway based on a combination of the Volmer and
11 Heyrovsky steps or the Volmer and Tafel steps where the overall kinetics is limited by the sluggish
12 Volmer step ($\text{H}_2\text{O} + \text{e}^- \rightarrow \text{H}_{\text{ad}} + \text{OH}^-$).

13 Recent studies have demonstrated that the incorporation of oxophilic metals into the
14 catalyst composition is crucial to enhancing the alkaline HER activity, leading to the contribution
15 of faster kinetics in the rate-determining Volmer step. Accordingly, modifying the catalytic surface
16 with foreign metals that have a higher oxophilicity is the most preferred approach to providing
17 bifunctional catalytic sites for efficient HER in non-acidic media, eventually for pH-universal HER
18 [8-14]. However, most of the studies that carried out the bifunctional theory based on the oxophilic
19 effect were limited to the high cost and reserve scarcity of noble Pt-based electrocatalysts [15,16].
20 Thus, it is highly desirable to consider the extension of the bifunctional effect to more economic
21 non-precious catalysts. In principle, from a viewpoint of surface modification of catalysts design,
22 the combination of earth-abundant active transition metals and foreign elements with low effective
23 nuclear charges and electronegativities can synergistically accelerate the alkaline HER kinetics
24 due to the introduction of oxophilicity. In this regard, earth-abundant transition metal
25 chalcogenides (TMCs) are one of the materials that can be used to enhance alkaline HER activity
26 through the modification of catalytic surface and the chemical environment through broad-range
27 phases with tunable composition [17-20]. Among the chalcogens, similar to metal cations with
28 oxophilic properties, tellurium (Te) would be a viable option for exploiting new TMCs materials
29 following the bifunctional theory. This is because Te is semi-metallic and possesses low
30 electronegativity and high electrical conductivity but has received little interest in the field of
31 oxophilic catalyst systems to date [21-24].

1 In this study, we designed and synthesized a ternary transition metals-based telluride
2 system (MoW₂NiTe) as a new class of electrocatalysts in which oxophilic Te acts as a bifunctional
3 catalytic site. We found that the combined incorporation of high valence non-3d two Mo and W
4 metals into heterogeneous catalyst systems enables an effective modulation of the electronic
5 structure, leading to electron-rich low valence states, and the synthesis of relatively small particles
6 with large catalytic surface area by reducing the overgrowth through sluggish atomic diffusion.
7 Moreover, it is found that Te also provides oxophilic properties, which can significantly improve
8 catalytic performance based on the bifunctional catalytic mechanism associated with the
9 accumulation ability of reactive OH* species on the catalytic surface in alkaline media. These
10 experimental results were further confirmed by density functional theory calculations showing that
11 the free energy associated with water dissociation can be decreased through a combination of high
12 valence non-3d metals and oxophilic Te.

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14 **2. Experimental**

15 2.1 Solution preparation

16 Nickel nitrate hexahydrate (Ni(NO₃)₂·6H₂O), tellurium dioxide (TeO₂), sodium molybdate
17 dihydrate (Na₂MoO₄·2H₂O), sodium tungstate dihydrate (Na₂WO₄·2H₂O), and ethanolamine
18 (C₂H₇NO) were purchased from Sigma Aldrich and were used without further purification. Four
19 different solutions were prepared for the electrochemical deposition process. 1 mM of
20 Ni(NO₃)₂·6H₂O and TeO₂ were dissolved in 28 mL of DI water, and then 2 mL of C₂H₇NO was
21 added (denoted as a NiTe solution). 1 mM of Ni(NO₃)₂·6H₂O, and Na₂MoO₄·2H₂O (or
22 Na₂WO₄·2H₂O) were dissolved in 28 mL of DI water, and then 2 mL of C₂H₇NO was added
23 (denoted as MoNi, and WNi solutions). 1 mM of Ni(NO₃)₂·6H₂O, Na₂MoO₄·2H₂O, and
24 Na₂WO₄·2H₂O were dissolved in 28 mL of DI water, and then 2 mL of C₂H₇NO was added
25 (denoted as a MoW₂Ni solution).

26 2.2 Electrochemical deposition

27 The electrochemical deposition was conducted at 40 °C using Autolab potentiostat PGSTAT302N.
28 A pair of nickel foams were used as the cathode and anode in a two-electrode system, and the
29 solutions were used as electrolytes [25]. The working electrode was subjected to current densities
30 of + 30 mA cm⁻² and - 30 mA cm⁻² for 5 minutes in turns using the NiTe solution as an electrolyte.

1 The resulting NiTe electrode was washed with DI water and directly used for secondary deposition.
2 To obtain MoW_{Ni}Te, a current density of - 30 mA cm⁻² was applied to the NiTe electrode for 10
3 minutes using the MoW_{Ni} solution as the electrolyte. Similarly, to obtain MoNiTe, and W_{Ni}Te, a
4 current density of - 30 mA cm⁻² was applied to the NiTe electrode for 10 minutes but using the
5 MoNi and W_{Ni} solution as electrolytes, respectively. Overgrown NiTe was prepared under the
6 same synthetic condition without solution change. All the electrodes were washed with DI water
7 after the electrochemical deposition process and dried at 60 °C overnight. To demonstrate the
8 catalytic role of Te in MoW_{Ni}Te, the dissolved amount of Te precursors in electrolyte solutions
9 for electrochemical deposition was controlled by varying molar concentrations of Te precursors
10 from 1, 0.75, 0.5, 0.25, and 0 mM, denoted as 100 % (MoW_{Ni}Te), 75 % (MoW_{Ni}Te_{0.75}), 50 %
11 (MoW_{Ni}Te_{0.50}), 25 % (MoW_{Ni}Te_{0.25}), and 0 % (MoW_{Ni}), respectively.

12 2.3 Material Characterization

13 Field emission scanning electron microscope (JSM-7800F Prime, JEOL Ltd, Japan), and spherical
14 aberration-corrected transmission electron microscope (JEM-ARM200F, JEOL Ltd, Japan) were
15 used to investigate morphologies and atomic arrangements of the samples. Energy-dispersive X-
16 ray spectroscopy (EDS) and Cs-TEM measurements were performed to identify the elemental
17 distribution of electrodeposited catalysts. The chemical structural properties of catalyst samples
18 were investigated by using X-ray photoelectron spectroscopy (ULVAC PHI 5000 VersaProbe II,
19 ThermoFisher Scientific, UK). All the binding energies were calibrated to C 1s (284.8 eV) to avoid
20 any misunderstanding originating from an instrumental error. The crystal structure of the samples
21 was examined by X-ray diffraction (Ultima IV, Rigaku, Japan) analysis. Zeta potentials were
22 measured using a zeta potential analyzer (ELSZ2000, OTSUKA, Japan). Inductively coupled
23 plasma atomic emission spectrometer (ICP-AES, OPTIMA 8300, Perkin-Elmer, USA) was used
24 to estimate the elemental composition of electrodeposited catalysts.

25 2.4 Electrochemical measurements

26 Before electrochemical measurements, all the samples were chemically activated by immersing in
27 a 6 M KOH solution purged with Ar gas at room temperature for 5 minutes. The activated samples
28 were washed with DI water and directly used as a working electrode. Electrochemical
29 measurements were performed in a three-electrode system composed of the working electrode, Pt
30 counter electrode, and reference electrode. Hg/HgO (20 % KOH, 0.098 V) was used as the

1 reference electrode in alkaline media, and Ag/AgCl (Saturated KCl, 0.197 V) as the reference
2 electrode in neutral and acidic media. Commercial Pt/C was prepared as a comparison for HER
3 applications. 10 mg of commercial Pt/C (Sigma Aldrich) was immersed in 950 μL of isopropanol
4 alcohol and then 50 μL of 5 wt% of nafion solution was added. 200 μL of the homogeneously
5 mixed solution was dropped poured on the nickel foam surface and dried at 60 $^{\circ}\text{C}$ overnight.

6 The reversible hydrogen electrode (RHE) was calculated using Equation 1.

$$7 \quad E_{RHE} = E_{ref} + 0.059 * pH + E^{\circ}_{ref} \quad (1)$$

8 All potential values were iR-corrected using solution resistance (R_s) values measured by
9 electrochemical impedance spectroscopy (EIS). The EIS was conducted at -0.1 V versus RHE
10 with a frequency range from 10 kHz to 10 mHz. Electrochemical active surface areas (ECSAs)
11 were calculated using Equation 2.

$$12 \quad ECSAs = C_{dl} / C_s \quad (2)$$

13 C_{dl} represents double-layer capacitance, and C_s represents the capacitance of an atomically smooth
14 surface area. The C_{dl} values were determined by the gradient of the graph of capacitive current
15 density against scan rates. The C_s value was adopted as 0.040 mF cm^{-2} in alkaline media and 0.035
16 mF cm^{-2} in acidic media [26]. Mass activities were calculated using Equation 3.

$$17 \quad \text{Mass activity} = j / \text{mass} \quad (3)$$

18 The j denotes the current during the measurements, mass was measured by subtracting from nickel
19 foam after electrochemical deposition to bare nickel foam. The amounts of electrodeposited
20 catalysts were found to be 0.82, 0.81, 0.78, 0.86, and 0.82 mg for MoW₂NiTe, MoNiTe, W₂NiTe,
21 NiTe, and Pt/C, respectively.

22 Turnover frequencies (TOFs) were calculated using Equation 4

$$23 \quad TOFs = j / 2 \cdot F \cdot n \quad (4)$$

24 The coefficient 1/2 is originated from the number of electrons required to evolve one H_2 gas, F
25 represents the Faradaic constant ($96,485 \text{ C mol}^{-1}$), and n is the number of active sites (mol). The
26 measured loading masses of catalysts were considered active sites and the number of active sites
27 was calculated as follows:

$$28 \quad \text{MoW}_2\text{NiTe} = 0.00082 / (95.95 + 183.84 + 58.69 + 127.60) = 1.76e^{-6} \quad (5)$$

1 $MoNiTe = 0.00081 / (95.95 + 58.69 + 127.60) = 2.86e^{-6}$ (6)

2 $WNiTe = 0.00078 / (183.84 + 58.69 + 127.60) = 2.10e^{-6}$ (7)

3 $NiTe = 0.00086 / (58.69 + 127.60) = 4.61e^{-6}$ (8)

4 $Pt/C = 0.00082 / 195.08 = 4.20e^{-6}$ (9)

5 2.5 Density functional theory calculations

6 All density functional theory (DFT) calculation here was performed using Quantum Espresso and
7 Perdew-Burke-Ernzerhof (PBE) exchange-correlation functional pseudopotentials were used
8 [27,28]. And meanwhile, Semiempirical Grimme's DFT-D3 dispersion correction was utilized to
9 correct the van der Waals (vdW) interactions [29]. All structures were relaxed with the following
10 sequence: first, vc-relax option was employed to fully relax the whole cell parameters and the
11 positions of atoms. And then, relax option was used to further find the optimized position of each
12 atom with high convergence criteria of force and energy. The cut-off energy here was chosen as
13 800 Ry which is larger enough to gain the desired result and the Brillouin zone was sampled by a
14 $4 \times 4 \times 1$ Gamma-centered k-points grid. Another point that should be mentioned was that four
15 layers configuration was modeled and a vacuum layer with a thickness of 15 Å was added along
16 the out-of-plane direction. While the pure NiTe slab model contains four layers, stacking by Ni
17 and Ti elements orderly, the initial cell is expanded into a 2×2 supercell which contains 16 atoms.
18 It is worth mentioning that initial bulk NiTe possesses a hexagonal structure, and its lattice belongs
19 to the space group P63/mmc. Our computed lattice parameter for this structure after optimization
20 was $a = 4.042$ Å. For the model of MoW₂NiTe, considering periodicity, centrally located atoms are
21 more likely to be replaced. Therefore, we chose the central position and the position adjacent to it
22 as the substitution sites, doped with Mo and W respectively.

23

24 3. Results and discussion

25 3.1. Material preparation and Characterization

26 Fig. 1a shows the conceptual schematic of the formation reaction of ternary transition
27 metals-based nickel telluride (MoW₂NiTe) catalysts as a heterogeneous catalyst system using a
28 simple and facile electrodeposition technique. Generally, as the deposition time increases, the
29 electrodeposition follows the Stranski-Krastanov (SK) growth, leading to a transition from the 2-
30 dimensional (2D) layer growth to the 3D island growth at a critical film thickness [30,31]. This

1 results in the formation of a 3D island structure, which provides a large surface area useful for
2 electrocatalysis applications. However, as shown in Fig. 1a, the excessive growth of particles can
3 occur through the relatively fast atomic diffusion in the simple component system such as NiTe
4 [32], resulting in an overgrown NiTe with a large particle size. In contrast, in the heterogeneous
5 multi-component system, the atomic diffusion can be more sluggish due to the chemical potential
6 difference between multi-component elements inducing high migration barriers [32-34]. Thus, it
7 is expected that by introducing high valence non-3d metal (single Mo, W, and binary MoW) into
8 the NiTe (as described in the Experimental section), heterogeneous multi-component catalysts,
9 such as MoNiTe or WNiTe and MoWNiTe, can be synthesized and smaller with increasing the
10 number of foreign non-3d metal elements.

11 As expected, field emission scanning electron microscope (FE-SEM) results showed that
12 the particle size of electrodeposited samples strongly depends on the number of components under
13 the same deposition time (Fig. 1b). It was found that MoWNiTe (~300 nm) has a smaller particle
14 size than MoNiTe (~450 nm), WNiTe (~450 nm), and overgrown NiTe (~5600 nm) (Fig. S1-4).
15 Moreover, Fig. 1c shows X-ray diffraction (XRD) patterns of all the telluride samples prepared by
16 electrodeposition. As shown in Fig. 1c, the broad peak around $2\theta = 31.75^\circ$, which is assigned to
17 the (101) plane of NiTe (ICSD ID 51732), gradually disappeared as more foreign atoms were
18 introduced to the NiTe. This finding suggests that the sluggish atomic diffusion in the multi-
19 component system retards grain growth, leading to a small particle size [32]. Furthermore,
20 aberration-corrected transmission electron microscope (Cs-TEM) examinations were performed
21 to characterize the element composition and microstructure of the electrodeposited samples (Fig.
22 1d). On the right side of Fig. 1d is the random atomic structure in amorphous MoWNiTe. MoNiTe
23 (Fig. S2) and WNiTe (Fig. S3) show the mixed feature of the ordered and disordered structure,
24 whereas overgrown NiTe (Fig. S4) shows a crystalline feature. These results are well consistent
25 with XRD results showing that heterogeneous catalysts are more amorphized with an increasing
26 number of foreign elements. In addition, it was further confirmed by the energy-dispersive X-ray
27 spectroscopy (EDS) measurements that all the samples show uniform elemental distributions in
28 MoWNiTe (Fig. 1e and Fig. S1), MoNiTe (Fig. S2), WNiTe (Fig. S3), and overgrown NiTe (Fig.
29 S4), respectively. The elemental composition of electrodeposited catalysts determined by
30 inductively coupled plasma atomic emission spectrometer (ICP-AES) is summarized in Table S1.

31 We investigated the chemical structures and electronic interactions of the electrodeposited

1 samples using X-ray photoelectron spectroscopy (XPS). Fig. 1f shows high-resolution XPS spectra
2 of Ni 2p, Te 3d, Mo 3d, and W 4f peak regions with the fitted peak components. It can be seen that
3 the ratio of Ni²⁺ and Ni³⁺ states, which are deconvoluted from Ni 2p_{3/2} spectra, was found to be
4 1.21, 1.38, 1.52, and 3.05, for NiTe, MoNiTe, WNiTe, and MoWNiTe, respectively [21-24]. These
5 results indicate that the modification of the electronic structure of MoWNiTe catalysts by the
6 combination of foreign Mo and W metals induces more electron-rich Ni states [35,36], which are
7 more favorable for HER [37,38], compared to MoNiTe or WNiTe modulated by single foreign
8 metal solely and overgrown NiTe catalysts. Furthermore, it was observed that there exist high
9 valence oxidation (Te⁴⁺ at 575.4 and 585.8 eV and Te⁶⁺ at 577.3 and 587.3 eV) states, indicating
10 that Te provides a strong oxophilic effect [21-24]. It was also found that in the Mo 3d region, after
11 the incorporation of W into MoNiTe, high valence non-3d transition metal states (Mo⁵⁺ and Mo⁶⁺)
12 increase while Mo⁴⁺ (229.0 and 232.6 eV) and Mo⁰ states (227.6 and 231 eV) decrease [10,35,39].
13 W 4f_{7/2} (34.9 eV), and W 4f_{5/2} (37.0 eV) peaks show a similar trend as the evolution of Mo 3d
14 peaks after the incorporation of Mo into WNiTe [9,35]. These results further confirm that the
15 incorporation of high valence non-3d transition metals play an important role as electron donors
16 in promoting the activation process towards HER by modulating the electronic structure of
17 MoWNiTe [35-38].

18 3.2. Electrochemical measurements

19 HER performances were evaluated with three-electrode configurations consisting of the
20 working electrode, Hg/HgO reference electrode, and Pt counter electrode in 1 M KOH.
21 Polarization curves were obtained at a scan rate of 1 mV s⁻¹ and calibrated to the reversible
22 hydrogen electrode (RHE) scale (Fig. 2a). As expected, MoWNiTe showed excellent
23 overpotentials of 72 and 125 mV to reach the current density of 10 and 100 mA cm⁻², respectively.
24 MoWNiTe exhibits a remarkable HER catalytic activity with an overpotential of 182 mV at a high
25 current density of 1000 mA cm⁻², which is much lower than the commercial Pt/C (222 mV).
26 Additionally, the catalytic activity of MoWNiTe is superior to the corresponding MoNiTe, WNiTe,
27 and NiTe, which attained overpotentials of 143, 223, and 247, respectively, to reach the current
28 density of 10 mA cm⁻². The HER performance of MoWNiTe catalysts is also estimated using
29 carbon paper and graphite rod as a working electrode and a counter electrode, respectively, and
30 demonstrated excellent activity regardless of electrodes (Fig. S5a).

31 To investigate HER kinetics and the mechanism of the catalysts, Tafel plots were obtained

1 from polarization curves around the current density of 100 mA cm^{-2} (Fig. 2b). The Tafel slope of
2 MoW₂NiTe was determined to be 52 mV dec^{-1} , which is smaller than those of MoNiTe (67 mV dec^{-1}),
3 W₂NiTe (54 mV dec^{-1}), and NiTe (98 mV dec^{-1}), indicating the transition of the rate-determining
4 kinetics away from the Volmer reaction mechanism. Moreover, MoW₂NiTe showed negligible
5 difference ($\Delta 7 \text{ mV dec}^{-1}$) in values of the Tafel slope obtained from around 10 to 100 mA cm^{-2}
6 current density, while the commercial Pt/C had a significant increase in the Tafel slope of 95 mV
7 dec^{-1} (Fig. S5b). It should be noted that the increase in the Tafel slope with overpotential is
8 associated with the sluggish Volmer kinetics in alkaline HER [40]. Thus, we believe that the
9 MoW₂NiTe follows the Heyrovsky mechanism even at the high current density.

10 To further evaluate and understand the catalytic activities of the electrodeposited catalysts,
11 electrochemical active surface areas (ECSAs), turnover frequencies (TOFs), and specific activities
12 were calculated. MoW₂NiTe needs a low overpotential of 170 mV to achieve a TOF value of 0.01
13 $\text{H}_2 \text{ s}^{-1}$ while MoNiTe, W₂NiTe, and NiTe require higher overpotentials of 283, 315, and 355 mV,
14 respectively, as shown in Fig. 2c. Fig. 2d shows specific activities of electrocatalysts normalized
15 by ECSAs, which are obtained from double-layer capacitance (C_{dl}) (Fig. S6). To reach the specific
16 current density of 10 mA cm^{-2} , MoW₂NiTe needs a much lower overpotential of 134 mV compared
17 to MoNiTe (282 mV), W₂NiTe (322 mV), and NiTe (356 mV). Geometrical current densities, TOFs,
18 and mass activities at -0.15 V versus RHE are summarized in bar plots, showing that the
19 MoW₂NiTe has superior extrinsic and intrinsic activities to the other prepared catalysts (Fig. 2e and
20 Fig. S7). Additionally, we compared the performance of MoW₂NiTe to the recently studied alkaline
21 HER electrocatalysts based on the value of overpotential and Tafel slope at the current density of
22 10 mA cm^{-2} , as summarized in Table S2, showing comparable or superior performance.

23 Electrochemical stability tests were carried out with the best-performed MoW₂NiTe
24 catalyst at the current density of 100 mA cm^{-2} for a long term of 3000 hours in 1 M KOH using
25 chronopotentiometry (CP) (Fig. 2f). MoW₂NiTe showed no significant change in its performance
26 during the long-term stability test and its polarization curves (inset of Fig. 2f) showed a negligible
27 degradation of $\Delta 1 \text{ mV}$ after stability tests. Moreover, after a long-term HER stability test, it was
28 confirmed from FE-SEM and Cs-TEM measurements that the surface structure and elemental
29 distribution of MoW₂NiTe were retained, supporting excellent electrochemical stability (Fig. S8).
30 Ex-situ XPS examination results also showed that low valence Te^{2-} and high valence Te^{6+} states,
31 indicating $\text{Te}(\text{OH})_6$ species, were simultaneously increased in the Te 3d region (Fig. S9) after a

1 stability test. Thus, the superior HER catalytic behavior of the optimized MoW₂NiTe can be
2 explained with the following synergistic benefits: (1) the incorporation of high valence non-3d
3 transition metals (Mo and W), which enhance the surface area with small particle size by sluggish
4 atomic diffusion and the intrinsic catalytic activity by modulating the electronic structure, leading
5 to electron-rich low valence states [37,38]; (2) the oxophilicity of Te as a dominant OH⁻ adsorption
6 site (OH⁻ ↔ OH_{ad} + e⁻), which leads to accumulation of reactive OH* species on the catalyst
7 surface to promote water dissociation through a bifunctional catalytic mechanism in alkaline media.

8 In order to further address whether Te with a high oxophilicity can provide bifunctional
9 catalytic sites associated with the in-situ formation of reactive OH* for efficient HER, we
10 evaluated HER activity of MoW₂NiTe as a function of Te contents (0 – 100 %). As shown in Fig.
11 3a, HER activity is sensitively dependent on the amount of Te in MoW₂NiTe_{1-x} (x = 0 ~ 1). HER
12 performance gradually improves as the amount of Te increases from 0 (MoW₂Ni) to 100 %
13 (MoW₂NiTe). Tafel slopes decrease from 140 to 52 mV dec⁻¹ around the current density of 100 mA
14 cm⁻², and zeta potential increases from 7.14 to 14.85 mV as the Te content increases from 0 to 100 %
15 (Fig. 3b and Fig. S10). Moreover, from cyclic voltammetry (CV) analysis (Fig. 3c), the Te anodic
16 peak increases as the amount of Te in MoW₂NiTe increases while the Ni anodic peak decreases,
17 confirming that Te acts as a dominant OH adsorption site (OH⁻ → OH_{ad} + e⁻) [41]. These findings
18 suggest that introducing the oxophilic Te makes the catalytic surface more positively charged with
19 increasing Te contents. This accelerates the catalytic interaction with OH⁻, leading to a transition
20 of the rate-determining step from the Volmer to Heyrovski step (Fig. 3d). Furthermore, density
21 functional theory calculations were conducted to identify the free energy for the water dissociation
22 process in alkaline media as shown in Fig. 3e and Fig. S11. It can be clearly seen that the MoW₂NiTe
23 exhibits a significantly reduced free energy of 0.536 eV for water dissociation compared with that
24 of the NiTe (0.965 eV). These calculation results suggest that the superior HER performance of M
25 oW₂NiTe is attributed to synergistic effects associated with the electronic structure modulation thr
26 ough the incorporation of high valence non-3d transition metals and the oxophilicity of Te leadin
27 g to the accumulation of reactive OH* species on the catalyst surface to accelerate water
28 dissociation through a bifunctional catalytic mechanism.

29 To demonstrate the high HER catalytic activity of MoW₂NiTe following the bifunctional
30 mechanism within universal pH conditions, HER measurements of MoW₂NiTe were further carried
31 out in non-alkaline media. 1 M phosphate-buffered saline (PBS) (pH ~ 7.4) and 0.5 M H₂SO₄ (pH

1 ~ 0.3) electrolytes were used with the same electrochemical setup with Ag/AgCl as the reference
2 electrode. In 1 M PBS, the MoW₂NiTe exhibited the best HER electrocatalytic performance with a
3 superior overpotential of 45 mV and Tafel slope of 60 mV dec⁻¹ at the current densities of 10 mA
4 cm⁻², respectively, which are lower than commercial Pt/C and the other electrocatalysts (Fig. 4a,c)
5 as well as previously reported HER electrocatalysts (Table S3). MoW₂NiTe also showed
6 remarkable overpotentials of 31 and 54 mV and Tafel slope of 34 and 70 mV dec⁻¹ at the current
7 densities of 10 and 100 mA cm⁻², respectively, (Fig. 4b,d), which are much smaller than those of
8 recently studied non-alkaline HER electrocatalysts and comparable to commercial Pt/C (Table S4).
9 Furthermore, MoW₂NiTe exhibited the lowest charge transfer resistance among the prepared
10 catalysts in universal pH environments, which is comparable to commercial Pt/C (Fig. S12).

11 The electrochemical stability of MoW₂NiTe was also evaluated in both the 1 M PBS and
12 0.5 M H₂SO₄ electrolytes. CP curves are well retained in both the neutral and acidic media for a
13 long-term of 1000 hours at the current density of 100 mA cm⁻² (Fig. 4e). Besides, only 4 and 1 mV
14 of overpotential increments were observed at the 100 mA cm⁻² in 1 M PBS and 0.5 M H₂SO₄,
15 respectively, (Fig. 4f), showing the excellent stability of MoW₂NiTe. Thus, it is considered that the
16 excellent electrochemical behavior of MoW₂NiTe within the universal pH range is attributed to
17 synergistic effects of incorporated high valence Mo and W, increasing intrinsic catalytic activity,
18 as well as oxophilic Te, leading to the accumulation of reactive OH* species in high pH
19 environments, which facilitate HER activity through the bifunctional mechanism associated with
20 efficient water dissociation.

21

22 **4. Conclusion**

23 In this study, we designed and demonstrated a ternary transition metals-based nickel
24 telluride system with high valence non-3d metals (Mo and W) and oxophilic Te as efficient
25 heterogeneous HER electrocatalysts following the bifunctional mechanism. The incorporation of
26 high valence non-3d two hetero-transition metals effectively induced electron-rich low valence
27 states of Ni and Te, leading to the enhanced hydrogen reduction reaction. Furthermore, introducing
28 Te made the catalytic surface more oxophilic, enabling accelerated catalytic interaction with OH-,
29 resulting in a transition of the rate-determining step from the Volmer to the Heyrovski step. As a
30 result, the optimized MoW₂NiTe showed excellent pH-universal HER performances with
31 overpotentials of 72, 45, and 31 mV at the current density of 10 mA cm⁻² in alkaline, neutral, and

1 acid media, respectively, which are much superior or comparable to previously reported
2 electrocatalysts and commercial Pt/C within universal pH environments. In addition, superior
3 long-term catalytic stability of MoW₂NiTe was also demonstrated without a negligible degradation
4 of overpotential increment up to 3000 hours in alkaline and 1000 hours in non-alkaline media at
5 the current density of 100 mA cm⁻². These experimental results are consistent with density
6 functional theory calculations, demonstrating that the enhanced HER performance was due to the
7 reduced free energy for water dissociation. We believe that our findings provide insight into the
8 design of highly efficient and stable HER electrocatalysts in universal pH and new prospects for a
9 bifunctional mechanism.
10

1 **Declaration of Competing Interest**

2 The authors declare no competing financial interest.

3

4 **Acknowledgments**

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6 the Ministry of Science and ICT (2022M3H4A1A04096478). The authors appreciate the support
7 from the Supercomputing Center of Wuhan University.

8

9 **Appendix A. Supporting Information**

10 FE-SEM and Cs-TEM images, Table for elemental composition of the prepared catalysts,
11 Polarization curves of MoW₂NiTe with different electrochemical setups, Tafel plots at the current
12 density from 10 to 100 mA cm⁻², CV curves in the non-Faradaic region, Table for HER activity in
13 1 M KOH compared to recently studied electrocatalysts, XPS spectra after long-term stability test,
14 FE-SEM and Cs-TEM images after a long-term stability test, Tafel plots of MoW₂NiTe with
15 different Te contents, Table for HER activity in 1 M PBS and 0.5 M H₂SO₄ compared to recently
16 studied electrocatalysts, EIS data of the prepared catalysts in universal pH environments.

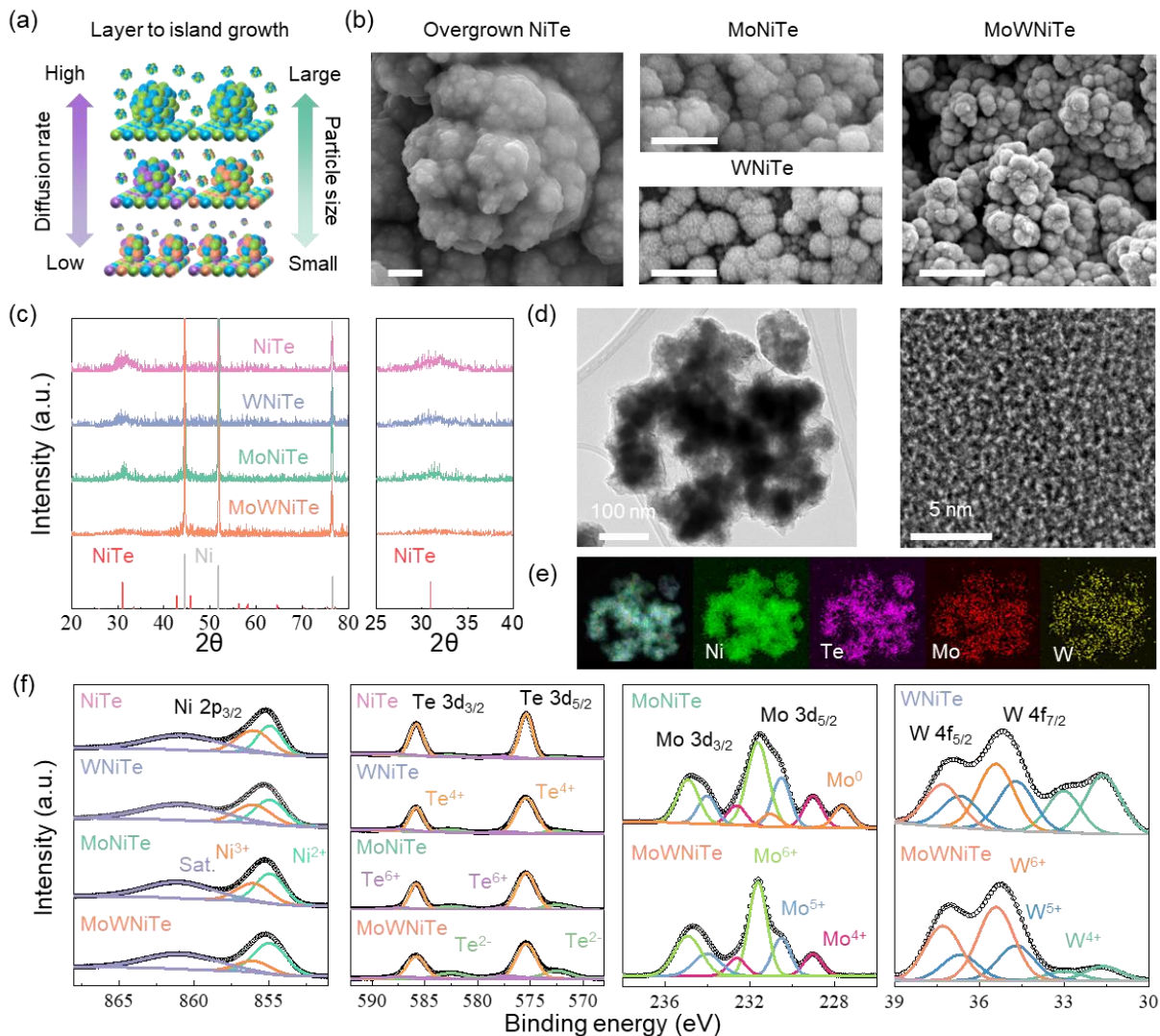
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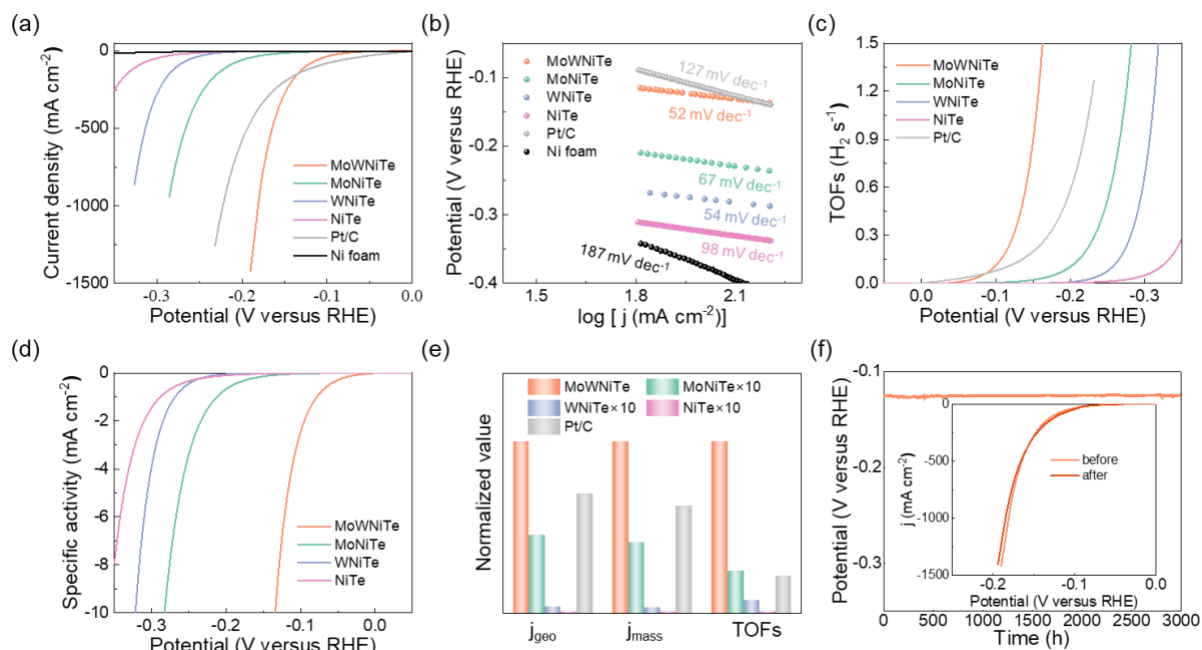
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2 **Fig. 1.** Characterization of electrodeposited catalysts. (a) Schematic illustration of the formation
3 reaction of the electrocatalyst during electrodeposition. Yellow, blue, purple, and grey particle
4 represent Ni, Te, Mo, and W, respectively. (b) Field emission scanning electron microscope (FE-
5 SEM) images of the electrocatalysts samples (All scale bars, 1 μm). (c) X-ray diffraction (XRD)
6 patterns of the prepared electrocatalysts. (d) Spherical aberration-corrected transmission electron
7 microscope (Cs-TEM), and (e) energy-dispersive X-ray spectroscopy (EDS) images of MoWNIte.
8 (f) X-ray photoelectron spectroscopy (XPS) spectra of the electrocatalysts samples in Ni 2p, Te
9 3d, Mo 3d, and W 4f peak regions.

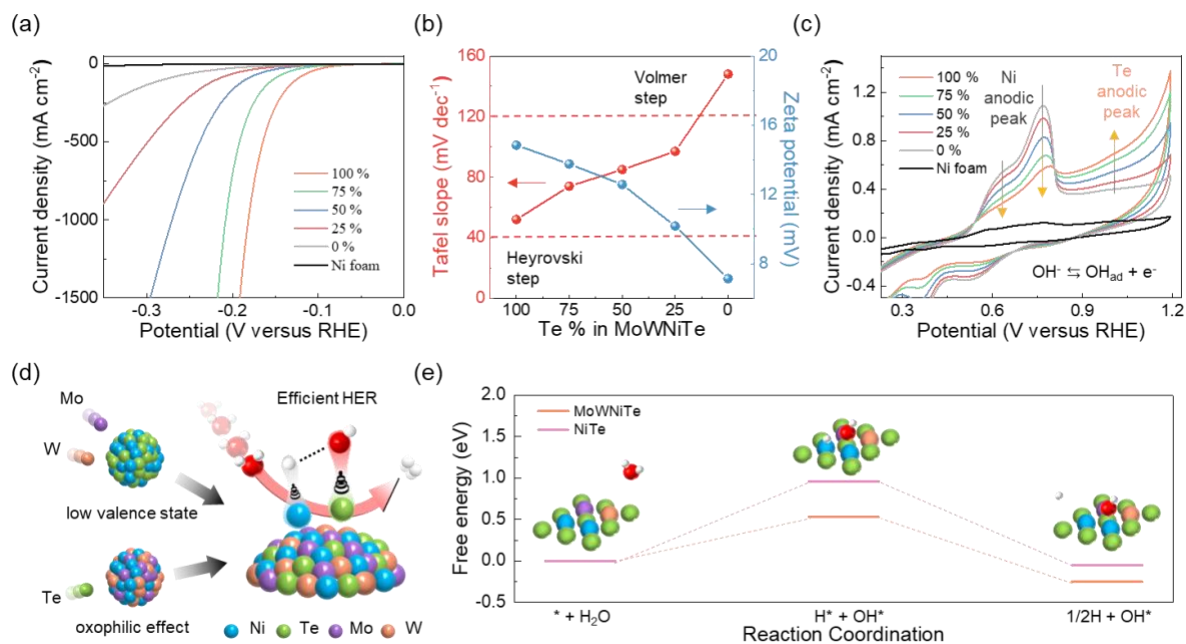
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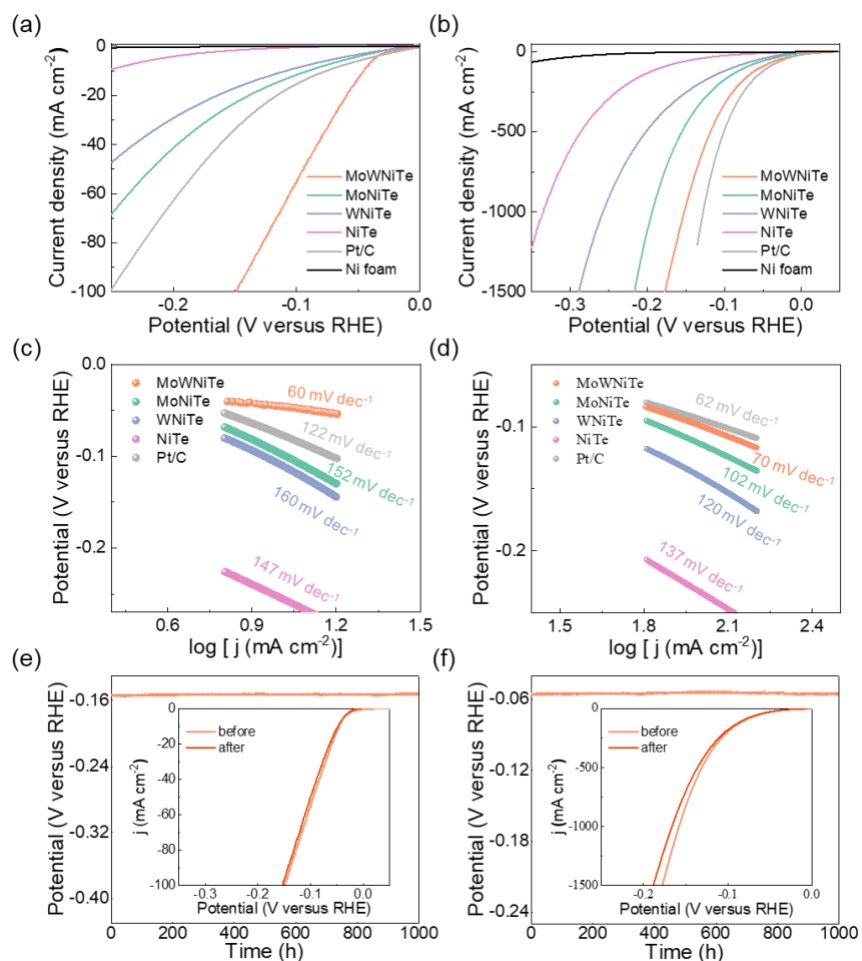
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2 **Fig. 2.** Electrochemical measurements in 1 M KOH. (a) Polarization curves of the electrodeposited
3 catalysts. (b) Tafel plots of the electrocatalysts around the current density of 100 mA cm^{-2} . (c)
4 Turnover frequencies (TOFs) and (d) specific activity of the prepared electrocatalysts. (e) Bar plots
5 of the electrocatalysts samples summarized with respect to geometrical current densities, mass
6 activities, and TOFs at -0.15 V versus RHE. The values of MoNIte, WNIte, and NiTe were 10
7 times (denoted as $\times 10$) their original values. (f) Chronopotentiometry (CP) curves of MoWNIte
8 at the current density of 100 mA cm^{-2} . Inset shows polarization curves of MoWNIte before and
9 after the stability test.

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2 **Fig. 3.** Catalytic activity of MoWNIte based on Te contents in 1 M KOH. (a) Polarization curves
3 of MoWNIte with different Te contents. (b) Tafel slope and zeta potential with respect to Te
4 contents in MoWNIte. (c) Cyclic voltammetry (CV) curves of MoWNIte with different Te
5 contents with a scan rate of 10 mV s⁻¹. Downward and upward arrows indicate Ni and Te oxidation
6 peaks, respectively. (d) Schematic illustration of water dissociation process on the surface of
7 MoWNIte in alkaline media. (e) Free energy diagram of HER reactions in alkaline media.

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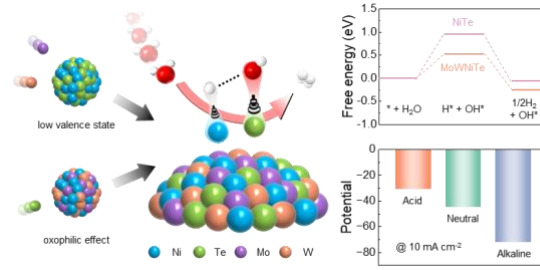


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 2 **Fig. 4.** Electrochemical measurements in 1 M PBS and 0.5 M H₂SO₄. Polarization curves in (a) 1
 3 M PBS, and (b) 0.5 M H₂SO₄. Tafel plots derived from polarization curves in (c) 1 M PBS, and (d)
 4 0.5 M H₂SO₄. Chronopotentiometry curves of MoWNIte at the current density of 100 mA cm⁻² in
 5 (e) 1 M PBS and (f) 0.5 M H₂SO₄. Insets show polarization curves of MoWNIte before and after
 6 the stability test.

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Graphical abstract



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Synergistic effect of high valence Mo and W metals and oxophilic Te in MoW/NiTe on accelerating water dissociation for efficient hydrogen evolution reaction in universal pH environments.