



## 2. Methodology

For the numerical simulation, the Impinging Jet flame model of Cantera 2.6.0 [15] was employed. The curve and slope were set to 0.014 and 0.028 to ensure all simulations have ~800 grid points. Diffusion transport was calculated by a multi-component model with the Soret effect enabled. The  $\text{NH}_3/\text{CH}_4$  fuel mixture was defined by an ammonia heat ratio,  $E_{\text{NH}_3}$ , given by Eq. (1):

$$E_{\text{NH}_3} = \frac{X_{\text{NH}_3} \cdot LHV_{\text{NH}_3}}{X_{\text{NH}_3} \cdot LHV_{\text{NH}_3} + X_{\text{CH}_4} \cdot LHV_{\text{CH}_4}} \quad (1)$$

Where  $LHV$  is the lower heating value of the fuels ( $LHV_{\text{CH}_4} = 802.30$  kJ/mol,  $LHV_{\text{NH}_3} = 316.84$  kJ/mol).

Figures 2, 5 and 6 show the variation of the integral value of the reaction R. Here, the value of  $I_R$  (in kmol/m<sup>2</sup>/s) was calculated using Eq. (2), where  $L$  is the distance between the burner nozzle outlet and the stagnation plate, set to 20 mm:

$$I_R = \int_0^L \dot{\omega}_R dx \quad (2)$$

For modelling the experimental data, mechanisms with variation in the detail of hydrocarbon-nitrogen subsets were used. The CEU- $\text{NH}_3$  model by Wang et al. [16] with detailed hydrocarbon-nitrogen reaction subsets were selected and utilized for the analysis. Meanwhile, GRI-3.0 [17] and Okafor [5] mechanisms were selected as intermediate sized mechanisms and finally, UCSD (San Diego) [18] was selected as a mechanism with no significant hydrocarbon-nitrogen chemistry subsets.

## 3. Results and Discussion

Figure 1 shows the comparison between experimental and numerical NO prediction. As can be seen, with the exception of GRI-3.0 and UCSD, the mechanisms are generally able to predict NO emissions in the lean region, however they all underpredict the empirical NO emissions at rich conditions, with the POLIMI and Wang mechanisms offering best agreement. Whether this is due to their detailed nitrogen-hydrocarbon chemistry, relevant to NO<sub>x</sub> formation in the rich region is investigated further.

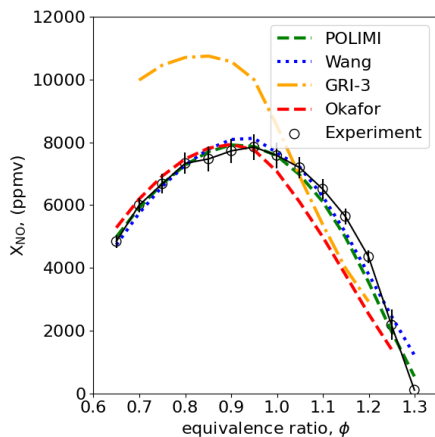


Fig. 1 NO product gas trends with change in equivalence ratio for  $E_{\text{NH}_3} = 0.2$ . Experimental values are from Ref [1].

Figure 2 shows a reaction pathway analysis for the rich region under the same conditions, with hydrocarbon species marked in red, and nitrogen-bound species marked in blue, and cyanide/isocyanides marked in green. Here, the thickness of the arrows is determined by  $I_R$ , from Eq. 2. The pathway shows segregation between the  $\text{NH}_3$  and  $\text{CH}_4$  chemistry routes, but with some interaction between the pathways through the formation of  $\text{H}_2\text{CN}$  and subsequent

decomposition of NCO. However, NO-reburn pathways to cyanide and isocyanide species formation and direct amine-hydrocarbon interactions to form methylamines are not considered significant.

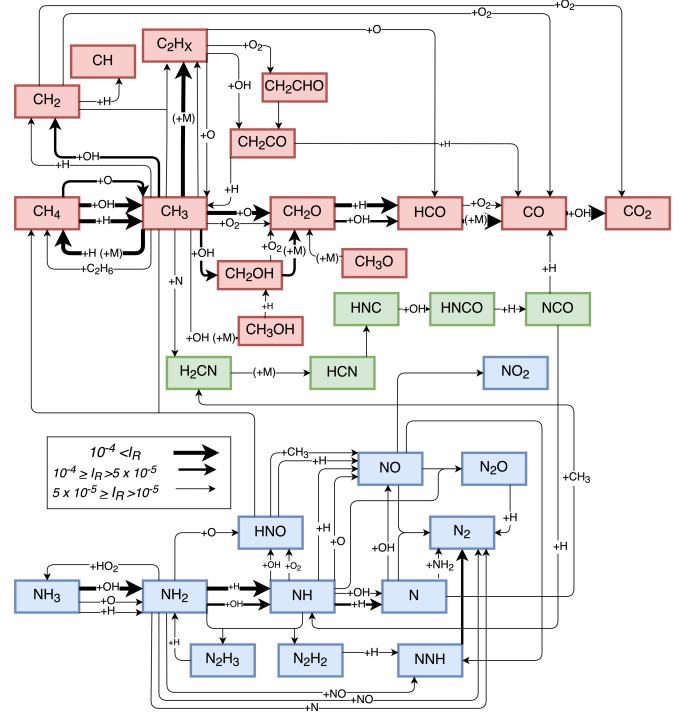


Fig. 2 Integrated ROP pathway analysis for  $E_{\text{NH}_3} = 0.2$ ,  $\phi = 1.30$  using the Wang mechanism.

Since the key interaction points  $\text{H}_2\text{CN}$  and NCO are rarely measured in combustion [19, 20] with the latter being a short-lived radical, other cyanide and isocyanide species can be used as an indicator of interactions between  $\text{NH}_3$  and  $\text{CH}_4$  chemistry. Figures 3 and 4 provide experimental evidence that the significance of these routes, and especially the role of HCN becomes more significant for  $E_{\text{NH}_3} = 0.2$  at  $\phi > 1.25$ . The data shows that all mechanisms are able to capture the increase in HCN in the rich region with varying accuracy, with only the Wang mechanism able to capture the increasing HNCO emissions in the rich region. However, further work is needed to measure this species with less uncertainty. It can be deduced from the Wang mechanism predicted emissions and reaction pathway analysis, that similar magnitudes of HNCO are formed as HCN at  $\phi = 1.30$ . However, according to experimental data, significant HCN emissions are measured at  $\phi = 1.30$ , which suggests that further work is needed to understand HCN formation in ammonia/methane flames.

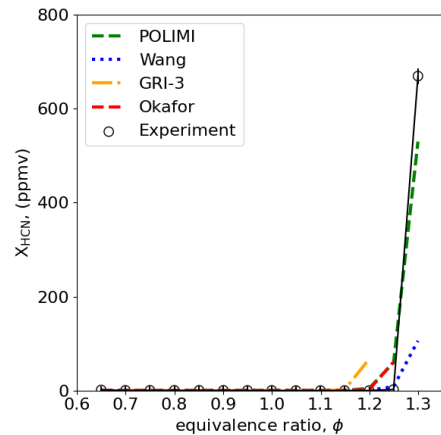


Fig. 3 HCN product gas trends with change in equivalence ratio for  $E_{\text{NH}_3} = 0.2$ . Experimental values are from Ref [1].



#### 4. Conclusion

A review of some popular NH<sub>3</sub>/CH<sub>4</sub> mechanisms suggests that many do not contain the full hydrocarbon-nitrogen chemistry subsets. The present study found that POLIMI and Wang mechanisms, containing the most complete hydrocarbon-nitrogen chemistry had almost perfect prediction of NO emissions at  $E_{NH_3} = 0.2$ . A few nitrogen-hydrocarbon reactions, especially  $CH_3 + HNO \rightleftharpoons CH_4 + NO$  contribute significantly to the formation of NO, though they are neglected from most popular NH<sub>3</sub>/CH<sub>4</sub> mechanisms. However, these reactions were not sensitive to the value of NO at the outlet, with reactions either containing NO or controlling the O, OH, H radical pool having the highest sensitivity. This suggests that the superior performance of the detailed mechanisms comes from better fitting reaction constants for key NO, O, H, OH reactions, rather than the inclusion of hydrocarbon-nitrogen chemistry interactions.

Meanwhile NO-reburn reactions contribute to around 10% of the NO consumption, in rich, high methane content blends. However, experimental data shows that the mechanisms tested in the present study were not able to accurately capture trends of HCNO and HCN emissions, which are also the species involved in NO-reburn reactions. Therefore, further experimental data of cyanide and isocyanide species may be necessary to fully understand the role of these species in ammonia/methane chemistry.

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